Rhodes, Greece, 31 August to 2 September 2017

## Syngas Production via Ethanol Dry Reforming: Effect of Promoter Type on Al<sub>2</sub>O<sub>3</sub>-supported Co Catalysts

Fahim Fayaz<sup>1</sup>, Mahadi B. Bahari<sup>1</sup>, Huy Nguyen-Phu<sup>2</sup>, Chinh Nguyen-Huy<sup>3</sup>, Bawadi Abdullah<sup>4</sup> and Dai-Viet N. Vo<sup>1,5,\*</sup>

<sup>1</sup>Faculty of Chemical & Natural Resources Engineering, Universiti Malaysia Pahang, Lebuhraya Tun Razak, 26300 Gambang, Kuantan, Pahang, Malaysia

<sup>2</sup>School of Chemical Engineering, University of Ulsan, 93 Daehak-ro, Nam-gu, Ulsan 44610, South Korea

<sup>3</sup>School of Energy & Chemical Engineering, Ulsan National Institute of Science and Technology (UNIST), 50 UNIST-gil, Eonyang-eup, Ulju-gun, Ulsan 689-798, Republic of Korea

<sup>4</sup>Chemical Engineering Department, Universiti Teknologi PETRONAS, Malaysia

<sup>5</sup>Centre of Excellence for Advanced Research in Fluid Flow, Universiti Malaysia Pahang, 26300 Gambang, Kuantan, Pahang, Malaysia

\*corresponding author: e-mail: vietvo@ump.edu.my (D.-V.N. Vo)

Abstract. Lanthanide-promoted (ceria and lanthana) and unpromoted 10%Co/Al<sub>2</sub>O<sub>3</sub> catalysts were synthesized via co-impregnation technique and evaluated for ethanol dry reforming in a quartz fixedbed reactor at  $P_{CO2} = P_{C2H5OH} = 20$  kPa and reaction temperature of 973 K under atmospheric pressure. Both Co<sub>3</sub>O<sub>4</sub> and CoAl<sub>2</sub>O<sub>4</sub> phases were formed on the surface of promoted and unpromoted catalysts. The reduction of Co<sub>3</sub>O<sub>4</sub> to CoO phase was facilitated by CeO<sub>2</sub> or La<sub>2</sub>O<sub>3</sub> addition. C<sub>2</sub>H<sub>5</sub>OH conversion improved significantly up to about 1.2 and 1.9 times with the addition of CeO<sub>2</sub> and La<sub>2</sub>O<sub>3</sub> promoters, respectively. La-promoted catalyst appeared to be the best catalyst in terms of H<sub>2</sub> and CO yields as well as C<sub>2</sub>H<sub>5</sub>OH conversion followed by Ce-promoted and unpromoted catalysts.

**Keywords:** Ethanol dry reforming, Co-based catalysts, Hydrogen, Syngas

## 1. Introduction

The growing concerns about the depletion of fossil fuels and increasing greenhouse gas emissions have resulted in the urgent exploration of alternative and green energy sources which can contribute to reduce the significant dependence on conventional fuels and utilize efficiently the undesirable greenhouse gasses. Syngas (referring to CO and H<sub>2</sub> mixture) has been considered as a potential source for the production of environmentally friendly synthetic fuels. Conventionally, syngas is produced via partial oxidation, steam or dry reforming of methane (Usman et al., 2015). However, methane is also a nonrenewable fossil fuel diminishing in the near future. Thus, there is a requirement for a sustainable and green process for generating syngas. Ethanol dry reforming (EDR) seems to be a promising method for syngas production and receives significant attention from both academic and industrial research since this process not only use a renewable reactant, *viz.*, ethanol to generate syngas employed as feedstock for downstream methanol production and Fischer-Tropsch synthesis, FTS (Vo and Adesina, 2012) but also mitigate undesirable  $CO_2$  greenhouse gas. Additionally, ethanol, which is rich of hydrogen content, readily available, and easily stored, can be simply produced via fermentation of biomass such as lignocellulose, sugar cane or starch-rich materials (Ni *et al.*, 2007; Vicente *et al.*, 2014).

Like other catalytic reforming processes of methane, EDR reaction is commonly carried out using Nibased catalysts in order to aid the cleavage of C-C and C-O bonds in ethanol (Hu and Lu, 2009; Bellido et al., 2009). However, Ni-based catalysts were easily deactivated during EDR process due to carbon formation through the Boudouard, methane cracking and ethylene polymerization reactions (Zawadzki et al., 2014; Bellido et al., 2009). Lanthanide metals (including  $La_2O_3$  and  $CeO_2$ ) have been recently employed as dopants or supports for Ni-based catalysts to improve carbon resilience during EDR reaction owing to their strong basic properties, high CO<sub>2</sub> adsorption capacity, great oxygen storage capacity and hence excellent coke resistance (Srisiriwat et al., 2009; Mazumder and de Lasa, 2014). In fact, Zawadzki et al. (2014) investigated the influence of different types of supports (such as CeO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, ZrO<sub>2</sub> and MgO) on Ni-based catalysts