

HYDROGEN AND METHANE
PRODUCTION FROM PALM OIL MILL
EFFLUENT THROUGH TWO-STAGE DARK
FERMENTATION

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Doctor of Philosophy

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Thesis submitted in fulfillment of the requirements
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DEDICATION

Specially dedicated to my beloved parents, lovable brothers, and sister who constantly encouraged and supported me all the way since the beginning of the studies.

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LIST OF SYMBOLS/UNITS

Q_F	Feed flow rate
V_{up}	Up-flow velocity
$H(t)$	Cumulative hydrogen production (mL)
P	Hydrogen production potential (mL)
R_m	Maximum hydrogen production rate (mL/h)
l	Lag phase time (h)
t	Cultivation time (h)
$H_{(Ac)}$	Acetic acid
$H_{(Bu)}$	Butyric acid
$H_{(Pr)}$	Propionic acid
$H_{(Va)}$	Valeric acid
EtoH	Ethanol
°C	Degree Celsius
$FeCl_2$	Ferric chloride
$MgSO_4$	Magnesium sulphate
NaOH	Sodium hydroxide
w/v	Weight to volume
m^3	Meter cube
min	Minute
g/L or gL^{-1}	Gram per litre
%	Percentage
Mol	Moles
nm	Nanometre
mg/L	Milligram per litre
$L H_2 L^{-1} d^{-1}$	Litre hydrogen per litre per day
$L CH_4 L^{-1} d^{-1}$	Litre methane per litre per day
ml	Millilitre
L	Litre
C:N	Carbon to nitrogen
C:P	Carbon to phosphate
Na^+	Sodium ions
K^+	Potassium ions
Na_2HPO_4	Disodium mono hydrogen phosphate
$CaCO_3$	Calcium carbonate
d	Days
h	Hours
Kg/m^3	Kilograms per cubic meter
KJ	Kilojoule
MJ	Mega joule
L/d	Litre per day
m/h	Meter per hour
$L H_2 kgCOD^{-1}$	Litre hydrogen per kilograms of chemical oxygen demand
$L CH_4 kgCOD^{-1}$	Litre methane per kilograms of chemical oxygen demand
$L H_2/L-POME$	Litre hydrogen per litre of palm oil mill effluent
$L CH_4/L-POME$	Litre methane per litre of palm oil mill effluent
$Kg/m^3 \cdot d$	Kilograms per meter cube per day

LIST OF ABBREVIATIONS

POME	Palm oil mill effluent
UASB	Up-flow anaerobic sludge blanket reactor
CSTR	Continuous stirred tank reactor
H ₂	Hydrogen
CH ₄	Methane
HPR	Hydrogen production rate
MPR	Methane production rate
HY	Hydrogen yield
MY	Methane yield
N ₂	Nitrogen
CO ₂	Carbon dioxide
POME	Palm oil mill effluent
HPP	Hydrogen production potential
MPP	Methane production potential
OLR	Organic loading rate
HRT	Hydraulic retention time
CCD	Central composite design
RSM	Response surface methodology
COD	Chemical oxygen demand
BOD	Biological oxygen demand
VSS	Volatile suspended solids
VS	Volatile solids
TSS	Total suspended solids
TS	Total solids
MLVSS	Mixed liquor volatile suspended solids
VFA	Volatile fatty acids
SHPR	Specific hydrogen production rate
SMPR	Specific methane production rate
DGGE	Denatured gradient gel electrophoresis
PCR	Polymerase chain reaction
Fe	Iron
DOE	Department of Environment
EIA	Energy information administration
EC	European commission
MPOB	Malaysian palm oil board
TN	Total nitrogen
CPO	Crude palm oil
TAN or NH ₄ ⁺ -N	Total ammonia nitrogen
TKN	Total kjeldahl nitrogen
BLAST	Basic local alignment search tool
HPG	Hydrogen producing granules
SRT	Solid retention time
F/M	Food to microbe ratio
DO	Dissolved oxygen

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ABSTRAK

Dua peringkat penapaian gelap adalah teknologi hijau yang melambangkan satu peluang yang hebat untuk pertukaran tenaga yang tinggi dan kawalan pencemaran kedua-duanya. Objektif utama kajian ini adalah untuk menyiasat dua proses peringkat gelap penapaian anaerobik untuk hidrogen (H_2) berturutan dan penghasilan metana (CH_4) menggunakan cecair buangan dari kilang minyak sawit sebagai (POME) aliran atas selimut anaerobik enapcemar-reaktor tangki teraduk berterusan (UASB-CSTR). Semasa eksperimen, H_2 telah dihasilkan dalam reaktor UASB dalam keadaan termofilik ($55^\circ C$) pada peringkat pertama, manakala CH_4 dihasilkan daripada buangan dari reaktor UASB dalam CSTR dalam keadaan mesofilik ($37^\circ C$) pada peringkat kedua. Haba terawat dan tidak terawat enapcemar anaerobik digunakan masing-masing sebagai inokulum untuk reaktor UASB dan CSTR. Pada yang pertama, ujian kumpulan telah dijalankan untuk mengetahui H_2 dan CH_4 yang berpotensi bagi pengeluaran POME. Mengikuti, reaktor UASB yang dikendalikan secara berterusan pada keadaan termofilik dengan masa tahanan hidraulik (HRT) selama 2 hari dan kadar muatan organik (OLR) sebanyak $75 \text{ kgCODm}^{-3}\cdot\text{d}^{-1}$ sehari untuk penghasilan H_2 . Buangan dari reaktor UASB yang selalunya mengandungi asetat dan butyrate telah dimasukkan terus ke dalam CSTR untuk penghasilan CH_4 pada suhu mesofilik dalam masa 5 hari HRT. Kadar maksimum penghasilan H_2 dan CH_4 telah dicapai masing-masing pada $1.92 \text{ L } H_2 \text{ L}^{-1}$ dan $3.2 \text{ L } H_2 \text{ L}^{-1}$ sehari. Hasil terkumpul H_2 dan CH_4 adalah masing-masing $215 \text{ L } H_2/\text{kgCOD}^{-1}$ dan $320 \text{ L } CH_4/\text{kgCOD}^{-1}$ dengan jumlah kecekapan penyingkiran COD sebanyak 94%. Granul enapcemar dari kedua-dua reaktor UASB dan CSTR dianalisis dengan menggunakan mikroskop elektron pengimbas dan komuniti mikrob dianalisis menggunakan PCR denaturasi elektroforesis gel kecerunan (PCR-DGGE). Keputusan menunjukkan kehadiran spesies *Thermoanaerobacterium* dalam UASB dan *Methanobrevibacter* spesies, dan *Methanosarcina* spesies dalam CSTR. Kajian kedua menunjukkan kesan edaran semula buangan CH_4 ke dalam reaktor UASB bagi penghasilan secara berterusan untuk H_2 dan CH_4 . HPP dari POME yang bercampur dengan buangan metanogen pada kadar edaran semula 50%, 40%, 35%, 30%, 20% dan 10% dikaji. Kedua-dua hasil dan kadar penghasilan H_2 meningkat dalam sistem edaran semula buangan metanogen. Edaran semula buangan metanogen pada kadar edaran semula 35% dapat mengimbangi kealkalian yang dikehendaki oleh reaktor UASB. Hasil H_2 dan CH_4 pula masing-masing $178 \text{ mL } H_2/\text{gCOD}$ and $412 \text{ mL } CH_4/\text{gCOD}$. Pengaruh kadar loading organik (OLR) juga dikaji. Pelbagai OLR seperti 25, 50, 75, 100, 125 kgCOD/m^3 sehari telah dianalisis bagi meningkatkan kadar penghasilan dan hasil H_2 dan CH_4 . Hasil yang lebih baik telah dicapai apabila OLR berada dalam lingkungan $75 \text{ kg-COD} / \text{m}^3$ sehari. Kadar maksimum penghasilan H_2 adalah $175.15 \text{ mL } H_2/\text{g MLVSS}$ sehari, manakala kandungan H_2 tertinggi dan hasil H_2 adalah masing-masing 35% and $49.22 \text{ mL } H_2/\text{g } COD_{\text{applied}}$. Kandungan dan hasil maksimum CH_4 , dan SMPR adalah 68%, $155.87 \text{ mL } CH_4/\text{g } COD_{\text{applied}}$ dan $325.13 \text{ mL } CH_4/\text{g MLVSS}$ sehari. Kajian terhadap pengaruh kadar aliran (Q_F) dan halaju aliran atas (VUP) diantara ($1.7\text{-}10.2 \text{ L/}$ sehari) dan ($0.5\text{-}3.0 \text{ m/jam}$) untuk penghasilan H_2 menggunakan kaedah gerak balas permukaan (RSM) menunjukkan bahawa hasil H_2 adalah $0.32 \text{ L } H_2 \text{ g}^{-1} \text{ COD}$ pada Q_F dan V_{up} of 1.7 L sehari and 0.5 m sejam. Julat optimum untuk penghasilan penapaian H_2 POME ialah $Q_F = 2.1\text{-}3.7 \text{ L}$ sehari and $V_{\text{up}} = 1.5\text{-}2.3 \text{ m}$ sejam. Keputusan eksperimen bersetuju sangat dengan ramalan model.

ABSTRACT

Two-stage dark fermentation is a green technology, presents an outstanding opportunity for both high energy conversion and pollution control. The main objective of this research is to investigate two-stage dark fermentation processes for sequential hydrogen (H₂) and methane (CH₄) production using palm oil mill effluent (POME) in up-flow anaerobic sludge blanket–continuous stirred tank reactor (UASB-CSTR). During the experiment, H₂ was produced in UASB reactor at thermophilic condition (55°C) in the first stage, while CH₄ was produced from the effluents of UASB reactor in the CSTR at mesophilic condition (37°C) in the second stage. The heat treated and non-heat treated anaerobic sludge was used as inoculum for UASB and CSTR reactor, respectively. In the first study, batch test was conducted to find out the hydrogen production potential (HPP) and methane production potential (MPP) of POME. Following, the UASB reactor operated continuously at thermophilic conditions with the hydraulic retention time (HRT) of 2 days and organic loading rate (OLR) 75 kgCOD m³·d⁻¹ for H₂ production. The effluents from UASB reactor were directly fed into CSTR for CH₄ production at mesophilic temperature with the HRT of 5 days. The maximum H₂ and CH₄ production rate achieved was 1.92 L H₂ L⁻¹·d⁻¹ and 3.2 L CH₄ L⁻¹ d⁻¹, respectively. The cumulative H₂ and CH₄ yields were 215 L H₂/kgCOD⁻¹ and 320 L CH₄/kgCOD⁻¹, respectively with the total COD removal efficiency of 94%. The sludge granules from both UASB and CSTR reactor were analyzed using scanning electron microscopy and the microbial community was analyzed using polymerase chain reaction denaturing gradient gel electrophoresis (PCR-DGGE). Results revealed that sludge granules were nearly round shaped with multiple cracks on the surface and UASB and CSTR reactor was enriched with *Thermoanaerobacterium* species and *Methanobrevibacter* species, *Methanosarcina* species, respectively. The second study addressed the effect of recirculation of methane effluent into UASB reactor for the continuous H₂ and CH₄ production. HPP from POME mixed with methanogenic effluent at recirculation rate of 50%, 40%, 35%, 30%, 20% and 10% was investigated. The recirculation of methanogenic effluent at 35% recirculation rate could compensate for alkalinity required by UASB reactor. The maximum H₂ and CH₄ yield were 178 mL H₂/gCOD and 412 mL CH₄/gCOD, respectively. Two-stage process with methanogenic effluent recirculation flavoured the UASB reactor and efficiently for energy recovery from POME. In the third study, influence of different organic loading rates (OLR) such as 25, 50, 75, 100, 125 kg-COD/m³·d was analyzed for the improvement of hydrogen and methane production rate and yield. The better yield was achieved when the OLR was in the range of 75 kg-COD/m³·d. The maximum H₂ production rate was 175.15 mL H₂/g MLVSS·d, while the highest H₂ content and yield were 35% and 49.22 mL H₂/g COD_{applied}, respectively. The maximum CH₄ content, CH₄ yield, and specific methane production rate (SMPR) were 68%, 155.87 mL CH₄/g COD_{applied} and 325.13 mL CH₄/g MLVSS·d, respectively. The results indicated that OLR affected H₂-CH₄ production and substrate removal efficiency. Finally, the studies on the influence of flow rate (Q_F) and up-flow velocity (V_{up}) ranging (1.7-10.2 L/d) and (0.5-3.0 m/h), respectively on hydrogen production using response surface methodology (RSM) showed that H₂ yield was 0.32 L H₂ g⁻¹ COD at Q_F and V_{up} of 1.7 L d⁻¹ and 0.5 m h⁻¹, respectively. The optimum ranges for the fermentative hydrogen production of the POME were Q_F = 2.1-3.7 L/d and V_{up} = 1.5-2.3 m/h. The experimental results agreed very well with the model prediction.

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- [1] Krishnan, S., Singh, L., Sakinah, M., Thakur, S., Wahid, Z. A., & Alkasrawi, M. (2016). Process enhancement of hydrogen and methane production from palm oil mill effluent using two-stage thermophilic and mesophilic fermentation. *International Journal of Hydrogen Energy*. **41(30)**: 12888-12898. (Elsevier, IF-3.3).
- [2] Krishnan, S., Singh, L., Sakinah, M., Thakur, S., Wahid, Z. A., & Sohaili, J. (2016). Effect of organic loading rate on hydrogen (H₂) and methane (CH₄) production in two-stage fermentation under thermophilic conditions using palm oil mill effluent (POME). *Energy for Sustainable Development*. **34**: 130-138. (Elsevier, IF-2.8).
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