# TREATMENT OF PALM OIL MILL EFFLUENT BY ELECTROCOAGULATION PROCESS

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Doctor of Philosophy

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#### MOHD NASRULLAH BIN ZULKIFLI

Thesis submitted in fulfillment of the requirements for the award of the degree of Doctor of Philosophy

> Faculty of Engineering Technology UNIVERSITI MALAYSIA PAHANG

> > JUNE 2017

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### LIST OF SYMBOLS

$A_a$	active anode surface (mm <sup>2</sup> )
Ap	projected area
D	global desirability function
$d_1$	average flocs size at steady state before breakage
$d_2$	flocs size at breakage
$d_3$	average flocs size at steady state after breakage
$d_e$	inter-electrode distance (mm)
d <sub>hor</sub>	dimension in horizontal
$d_i$	desirability function
$d_s$	surface diameter
d <sub>v</sub>	volumetric diameter
$d_{ver}$	dimension in vertical
$e_r$	residual error
F	Faraday's constant (96,485 C/mol)
f	response function
Fr	recovery factor
Fs	strength factor
Ι	the current (A)
k	specific conductivity
m	the mass of anode dissolution (g)
$M_w$	the molecular weight (g/mol)
Р	perimeter
R	resistance $(\Omega)$
$\mathbb{R}^2$	coefficient of determination
$R_{G1}$	growth rate before breakage
$R_{G2}$	growth rate after breakage
S	floc surface area
t	the time of operation (s)
V	voltage (V)
$\mathbf{X}_1$	current intensity factor for RSM
$\mathbf{X}_2$	electrolysis time factor for RSM
X <sub>3</sub>	inter-electrodes distance factor for RSM
$X_4$	pH factor for RSM
Y	response
$\mathbf{Y}_1$	COD response for RSM
$\mathbf{Y}_2$	BOD response for RSM
Y <sub>3</sub>	SS response for RSM
Z.	the number of electrons involved in the reaction
η <sub>IR</sub>	IR drop

## LIST OF ABBREVIATIONS

ADE	Anaerobic Baffled Filter
ABF	
ADF	Anaerobic Down-flow Filter
ADS	Anaerobically Digested Sludge
AHR	Anaerobic Hybrid Reactor
ANOVA	Analysis of Variance
A-PAM	Anionic Polyacrylamide
BBD	Box-Behnken Design
BC	Before Centuries
BOD	Biochemical Oxygen Demand
BP	Bipolar
C.V	Coefficient of Variation
COD	Chemical Oxygen Demand
C-PAM	Cationic Polyacrylamide
СРКО	Crude Palm Kernel Oil
CPO	Crude Palm Oil
DC	Direct Current
DO	Dissolved Oxygen
DOE	Department of Environment
DoE	Design Of Experiment
EDX	Energy Dispersive X-ray
EFB	Empty Fruit Bunches
EQA	Environment Quality Act
FESEM	Field Emission Scanning Electron Microscope
FFB	Fresh Fruit Bunch
FTIR	Fourier Transform Infrared Spectroscopy
HCPB	Hollow Centered Packed Bed
HR	High range
HRT	Hydraulic Retention Times
IAAB	Integrated Aerobic Anaerobic Bioreactor
MF	Fruit Fibers
MLSS	Mixed Liquor Suspended Solid
MLVSS	Mixed Liquor Volatile Suspended Solid
MP-P	Monopolar Parallel
MP-S	Monopolar Series
OFAT	One Factor at One Time
OLR	Organic Loading Rate
PACI	Polyaluminium Chloride
PKS	Palm Kernel Shells
POME	Palm Oil Mill Effluent
PRESS	Prediction Error Sum of Squares
RF	Rumen Fluid
RO	Reverse Osmosis
RSM	Response Surface Methodology
SBR	Sequencing Batch Reactor Semi-continuous Stirred Tank Reactors
SCSTR	
SI	International System
SS	Suspended Solid
SVI	Sludge Volume Index
TDS	Total Dissolve Solid
TOC	Total Organic Carbon
TP	Total Phosphorus
TSS	Total Suspended Solid

UASB	Up-flow Anaerobic Sludge Bed
UF	Ultra Filtration
UHR	Ultra High range
VFA	Volatile Fatty Acid
VFA/TA	Volatile Fatty Acid to Total Alkalinity
VSS	Volatile Suspended Solid
XRD	X-ray Powder Diffraction

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#### ABSTRAK

Sisa kumbahan kilang minyak kelapa sawit (POME) dikenali sebagai salah satu penyumbang terbesar kepada pencemaran air di Malaysia disebabkan oleh kepekatan permintaan oksigen kimia (COD), permintaan oksigen biokimia (BOD) dan pepejal terampai (SS) yang tinggi. Kaedah-kaedah seperti dengan menggunakan bahan kimia penggumpal, penjerapan, penapisan, rawatan aerobik dan anaerobik, sistem kolam dan sebagainya, memerlukan masa yang panjang dan bahan kimia yang substantif. Maka, rawatan menggunakan teknik elektropenggumpalan telah diperkenalkan dan digunakan. Proses ini menawarkan beberapa kelebihan yang tersendiri seperti kemudahan, keberkesanan, penjimatan masa dan memerlukan kawasan yang kecil sahaja. Sel elektrokimia telah berjaya direkabentuk untuk merawat POME dengan memilih orientasi menegak berbanding orientasi mendatar kerana ianya telah memperolehi penyingkiran COD, BOD dan SS yang tertinggi iaitu masing-masing adalah 57, 53 dan 51%. Monopolar bersiri (MP-S) telah dipilih sebagai susunan elektrod berbanding monopolar selari (MP-P) dan bipolar (BP) kerana memiliki penyikiran tertinggi iaitu 65, 62 dan 60% untuk COD, BOD dan SS masing-masing. Sabut besi dipilih sebagai bahan dan jenis struktur untuk elektrod berbanding plat besi dan aluminium kerana penyingkiran tertingginya masing-masing pada 74, 70 dan 66% untuk COD, BOD dan SS. Parameter beroperasi seperti tempoh masa elektrolisis, keamatan arus, jarak antara elektrod dan pH awal mempunyai pengaruh yang besar terhadap penyingkiran COD, BOD dan SS. Julat terbaik bagi parameter operasi untuk merawat POME dengan berkesan didapati 30 hingga 50 minit untuk tempoh masa elektrolisis, 15 hingga 20 A untuk keamatan arus, 5 hingga 15 mm untuk jarak antara elektrod dan 3 hingga 6 untuk nilai pH awal. Penggunaan elektrik sering menjadi faktor pengehad di dalam proses electrocoagulation, maka keamatan arus yang tinggi (15, 20 dan 25 A) telah diperkenalkan dan dikaji untuk meningkatkan keberkesanan proses. Untuk analisis saiz zarah, purata saiz gumpalan pada keadaan stabil pertama, keadaan pemecahan, keadaan stabil kedua, faktor kekuatan, faktor pemulihan, kadar pertumbuhan pertama dan kadar pemulihan kedua adalah 336 μm, 223 μm, 333 μm, 66.37%, 97.35%, 20.94 μm/min dan 11.89 μm/min. Purata saiz gumpalan pada keadaan stabil kedua bagi keamatan arus untuk 1, 5, 10, 15, 20 dan 25 A masing-masing adalah 168, 252, 333, 463, 538 and 550 µm. Purata saiz gumpalan pada keadaan stabil kedua bagi jarak antara elektrod-elektrod untuk 5, 10, 15, 20, 25 dan 30 mm masing-masing adalah 214, 228, 208, 168, 138 and 97 µm. Purata saiz gumpalan pada keadaan stabil kedua bagi pH untuk 2, 3, 4, 5, 6, 7, 8 dan 9 masing-masing adalah 216, 244, 275, 267, 236, 191, 175 dan 163 µm. Kajian RSM menunjukkan penyingkiran optimum dicapai pada 19.07 A, 44.97 minit, jarak 8.60 mm dan pH 4.37. Hasil jangkaan di bawah keadaan optimum tersebut masing-masing adalah 97.21, 99.26 dan 99.00% untuk penyingkiran COD, BOD dan SS. Kajian pengesahan masing-masing menunjukkan 95.03, 94.52 dan 96.12% untuk penyingkiran COD, BOD dan SS dengan ralat masing-masing sebanyak 2.29, 5.01 dan 1.96%. Secara keseluruhannya, rawatan menggunakan proses elektropenggumpalan menunjukkan keberkesanan dan juga menjimatkan masa dalam meyingkirkan bahan pencemar daripada POME.

#### ABSTRACT

Palm oil mill effluent (POME) is known to be one of the major attributer to water pollution in Malaysia due to its high concentration of chemical oxygen demand (COD), biochemical oxygen demand (BOD) and suspended solid (SS). Various techniques of effluent treatment such as chemical coagulation, adsorption, filtration, aerobic and anaerobic treatment, ponding system etc., have disadvantages such as high retention time and substantive chemical substances. Therefore, in this study electrocoagulation technique was introduced and applied. This process offers some distinctive advantages including a simple set-up, effectively remove high concentration of pollutant, short treatment time and requires only a small treatment space. Electrochemical cell has been successfully designed for POME treatment by choosing the vertical over horizontal orientation which subsequently resulted the highest removal of 57, 53 and 5% for COD, BOD and SS respectively. Monopolar series (MP-S) has been chosen instead of monopolar parallel (MP-P) and bipolar (BP) as the electrode arrangement due to the highest removal of 65, 62 and 60% for COD, BOD and SS respectively. Steel wool has been chosen rather than iron and aluminium plate for the highest removal of 74, 70 and 66% of COD, BOD and SS respectively. Operating parameters such as electrolysis time, current intensity, inter-electrode distance and initial pH have a great influence on the removal of COD, BOD and SS. The best effective range of operating parameters to treat POME were found to be 30 to 50 minutes for electrolysis time, 15 to 20 A for current intensity, 5 to 15 mm for inter-electrode distances and 3 to 6 for initial pH value. Electricity consumption is often become the limiting factor in the electrocoagulation process, therefore in this research, the high intensity of the current (15, 20 and 25) has been introduced and studied to improve the effectiveness of the process. For particle size analysis, the average flocs size at first steady-state, floc size at breakage state, average size at second steady-state, strength factor, recovery factor, first growth rate and second growth rate were found to be 336 µm, 223 µm, 333 µm, 66.37%, 97.35%, 20.94 µm/min and 11.89 µm/min. The average flocs size at the second steady-state for 1, 5 10, 15 20 and 25 A of current intensity were 168, 252, 333, 463, 538 and 550 µm respectively. The average flocs size at the second steady-state for 5, 10, 15, 20, 25 and 30 mm of interelectrode distances were 214, 228, 208, 168, 138 and 97 µm respectively. The average flocs size at second-steady state for pH 2, 3, 4, 5, 6, 7, 8 and 9 were found to be 216, 244, 275, 267, 236, 191, 175 and 163 µm respectively. The optimization study using response surface methodology (RSM) indicated that the optimal COD, BOD and SS removals were achieved at 19.07 A of current intensity, 44.97 minutes of treatment time, 8.60 mm of electrode distance and 4.37 of pH. The predicted results under this optimized condition were 97.21, 99.26 and 99.00% for COD, BOD and SS removal respectively. The validation experiment showed 95.03, 94.52 and 96.12% for COD, BOD and SS removal with 2.29%, 5.01% and 1.96% of standard error respectively. Overall, the treatment by using electrocoagulation process demonstrated an effectiveness and time saving technique for pollutant removal from POME.

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