

**GLYCEROL DRY REFORMING FOR
SYNGAS PRODUCTION OVER
Ag-PROMOTED ON Ni-BASED CATALYSTS**

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Thesis submitted in fulfilment of the requirements
for the award of the degree of
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LIST OF SYMBOLS

F	Flow rate
X _G	Glycerol conversion
Y _{H2}	Hydrogen yield
Y _i	Yield of Carbon containing species
λ	Wavelength
θ	Bragg angle

LIST OF ABBREVIATIONS

BET	Brunauer-Emmett-Teller
CGR	Carbon to glycerol feed ratio
FESEM-EDX	Field emission scanning microscopy/Energy dispersive X-ray
IUPAC	International Union of Pure and Applied Chemistry
OPEC	Organisation of the Petroleum Exporting Countries
SEM	Scanning electron microscopy
TGA	Thermogravimetric analysis
TPC	Temperature programmed calcination
TPD	Temperature programmed desorption
TPO	Temperature programmed oxidation
TPR	Temperature programmed reduction
WHSV	Weight hourly space velocity
XRD	X-ray diffraction

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ABSTRAK

Penggunaan gliserol telah dikaji secara meluas dan merupakan salah satu bahan mentah alternatif dalam pengeluaran gas sintetik (*syngas*). Proses tindakbalas gliserol dan CO₂ adalah satu proses yang menarik kerana ia menukar karbon dioksida, gas rumah hijau kepada gas sintetik dan pada masa yang sama dikeluarkan daripada kitaran karbon. Objektif utama penyelidikan ini adalah untuk mengkaji tindakbalas gliserol dan CO₂ dengan menggunakan mangkin berasaskan nikel yang ditambah logam (perak) dan logam oksida (aluminium oksida dan silikon oksida). Logam perak jarang digunakan sebagai mangkin dalam kajian pembaharuan (*reforming*). Namun, ia telah dibuktikan bahawa logam perak mempunyai kebolehan untuk mengurangkan pengumpulan karbon di permukaan mangkin dan meningkatkan hasil gas hydrogen di samping ianya lebih rendah dari segi kos berbanding logam di dalam kumpulan logam *noble* yang lain. Mangkin telah disediakan melalui kaedah pengisitepuan (*wet impregnation*) menggunakan kombinasi logam-oksida yang berbeza. Pencirian terhadap sifat mangkin telah dinilai menggunakan kaedah penjerapan fizikal N₂ (kaedah *Brunauer-Emmet-Teller* (BET)), analisis pembelauan sinar-X (XRD), mikroskop elektron pengimbasan (SEM), pengkalsinan suhu berprogram (TPC), penurunan suhu berprogram (TPR), pengoksidaan suhu berprogram (TPO), dan penyahherapan suhu berprogram (TPD). Kajian saringan pada peringkat awal telah dijalankan untuk menilai prestasi jenis-jenis oksida yang digunakan dan didapati bahawa Ni/Al₂O₃ memberikan tindakbalas gliserol dan hasil hidrogen yang lebih tinggi berbanding Ni/SiO₂ kerana saiz kristal yang lebih kecil di atas permukaan luar mangkin dan luas permukaan yang tinggi. Selain itu, alumina boleh meningkatkan kesebatian logam serta mengelakkan pemendapan karbon dan pada masa yang sama meningkatkan aktiviti dan kestabilan mangkin. Selain itu, apabila campuran Ag yang berbeza telah ditambah kepada mangkin ini, 3wt% Ag dalam Ni/Al₂O₃ memberikan prestasi mangkin yang terbaik kerana kewujudan zarah aktif yang menyebabkan luas permukaan yang tinggi. Campuran Ag (> 3wt%) menyebabkan pembentukan zarah kecil yang menyelaputi tapak aktif mangkin dan menjelaskan prestasi mangkin. Siasatan lanjut mengenai kesan-kesan faktor lain dalam ses sebuah tindak balas (iaitu suhu tindak balas, berat mangkin yang digunakan dan nisbah CO₂ kepada gliserol (CGR)) kepada pengeluaran gas sintetik telah dijalankan menggunakan mangkin yg terbaik yang diperolehi melalui ujian saringan mangkin, iaitu Ag(3)-Ni/Al₂O₃. Peratusan tindakbalas gliserol dan penghasilan produk yang terbaik ditemui pada suhu 1073 K, CGR 1 dan WHSV 36 L g_{cat}⁻¹ h⁻¹ yang memberikan 41.09% tindakbalas gliserol dan 32.31% hasil hidrogen. Tindakbalas selama 72 jam mendedahkan bahawa mangkin tersebut stabil sepanjang tempoh tersebut selepas mengalami penurunan pada jam yang kesepuluh. Selain itu, kajian terhadap mangkin yang telah digunakan dalam proses tindakbalas tersebut menunjukkan kehadiran karbon jenis yang berserbut pada permukaan mangkin, yang boleh disingkirkan melalui proses pengoksidaan.

ABSTRACT

The use of glycerol has been widely investigated and one of the possible alternatives is as a feedstock in the production of synthesis gas (syngas). The glycerol CO₂ dry reforming process is an attractive process as it converts carbon dioxide, a greenhouse gas, into a synthesis gas and simultaneously removed from the carbon biosphere cycle. The main objective of this research work is to study the process of CO₂ dry reforming of glycerol over noble catalyst i.e. a noble metal (silver) promoted on nickel-based catalyst supported on oxides (aluminium oxide and silicon oxide). Silver is rarely used as catalyst in reforming studies. However, it is proven that silver has the ability to reduce the carbon deposition and increase selectivity of hydrogen production besides lower in cost compared to other noble metal. The catalysts were formulated through wet impregnation method using different combinations of noble metal-oxides support. Their physicochemical characteristics were evaluated using nitrogen physisorption (Brunauer-Emmet-Teller (BET) method), X-ray diffraction (XRD), Scanning electron microscopy (SEM), Temperature programmed calcination (TPC), Temperature programmed reduction (H₂-TPR) and Temperature programmed desorption (TPD). The screening study was conducted to evaluate the performance of different types of supports, and it was found that Ni/Al₂O₃ catalyst series gave higher glycerol conversion and hydrogen yield compared to Ni/SiO₂ catalyst series due to their small crystallites size and high surface area. Moreover, alumina support could increase metal dispersion as well as avoiding the carbon deposition, which simultaneously improved the activity and stability of the catalyst. Apart from that, when different Ag loadings were introduced to these catalysts, 3wt% of Ag in Ni/Al₂O₃ was found to give the best catalyst performance due to the well-dispersion of active sites on the catalyst surface, which created high surface area. Higher Ag loading (>3wt%) resulted in formation of small particles, which covered the active sites of the catalyst thus impaired the catalyst performance. Further investigation on the effect of reaction variables (i.e. reaction temperature, weight hourly space velocity (WHSV) and CO₂-to-glycerol ratio (CGR)) to the production of syngas were conducted using the best catalyst obtained from the screening study. The best reaction condition was found at temperature of 1073 K, CGR of 1 and WHSV of 36 L g_{cat}⁻¹ h⁻¹ (catalyst loading of 0.2 g) which gave 41.09% glycerol conversion and 32.31% hydrogen yield. During the catalyst longevity study, Ag(3)-Ni/Al₂O₃ was found to stabilise along the 72 hours reaction after experiencing a reduction at tenth hour. Apart from that, the study on the catalyst deactivation of the used catalyst shows the presence of filamentous and encapsulated carbon types on the catalyst surface, which can be removed through oxidation.

REFERENCES

- Adhikari, S., Fernando, S., Gwaltney, S., Filipto, S., Markbricka, R., Steele, P. and Haryanto, A. (2007) A thermodynamic analysis of hydrogen production by steam reforming of glycerol. *International Journal of Hydrogen Energy*, 32(14): 2875-2880.
- Adhikari, S., Fernando, S. D., and Haryanto, A. (2009) Hydrogen production from glycerol: An update. *Energy Conversion and Management*, 50(10): 2600-2604.
- Buffoni, I. N., Pompeo, F., Santori, G. F. and Nichio, N. N. (2009) Nickel catalysts applied in steam reforming of glycerol for hydrogen production. *Catalysis Communications*, 10 (2009): 1656–1660
- Chen, H., Ding, Y., Cong, N.T., Dou, B., Dupont, V., Ghadiri, M. and Williams, P.T. (2011) A comparative study on hydrogen production from steam-glycerol reforming: thermodynamics and experimental. *Renewable Energy*, 36 (2011) 779-788.
- Cheng, C.K., Lim, R.H., Ubil, A., Chin, S.Y. and Gim bun, J. (2012) Hydrogen as carbon gasifying agent during glycerol steam reforming over bimetallic Co-Ni catalyst. *Advances in Material Physics and Chemistry*, 2(4):165-168.
- Chiodo, V., Freni, S., Galvagno, A., Mondello, N., and Frusteri, F. (2010) Catalytic features of Rh and Ni supported catalysts in the steam reforming of glycerol to produce hydrogen. *Applied Catalysis A: General* 381 (2010) 1–7
- Ciftci, A., Michel Lighthart, D. A. J., Oben Sen, A., Van Hoof, A. J. F., Friedrich, H. and Hensen, E. J. M. (2014) Pt-Re synergy in aqueous-phase reforming of glycerol and the water–gas shift reaction. *Journal of Catalysis* 311 (2014) 88–101
- Czernik, S., French R., Feik, C. and Chornet, E. (2002). Hydrogen by catalytic steam reforming of liquid by products from biomass thermoconversion process. *Industrial and Engineering Chemistry Research*, 41, 4209-15.
- Dauenhauer, P., Salge, J. and Schmidt, L. (2006). Renewable hydrogen by autothermal steam reforming of volatile carbohydrates. *Journal of Catalysis*, 244(2), 238-247.
- Department of Economic and Social Affairs of United Nation (2015) World population projected to reach 9.7 billion by 2050. (Online)
<http://www.un.org/en/development/desa/news/population/2015-report.html> (12 November 2015)
- Dieuzeide, M.L., Iannibelli, V., Jobbagy, M. and Amadeo, N. (2012). Steam reforming of glycerol over Ni/Mg/ γ -Al₂O₃ catalysts. Effect of calcination temperatures. *Renewable Energy*, 36 (2011) 779-788.

- Ebhish, A., Yaakob, Z., Narayanan, B., Bshish, A. and Wan Daud, W. R. (2011) The Activity of Ni-Based Catalysts on Steam Reforming of Glycerol for Hydrogen Production. *International Journal of Integrated Engineering*, 3(2011): 5-8
- Estellé, J., Salagre, P., Cesteros, Y., Serra, M., Medina, F., & Sueiras, J. E. (2003). Comparative study of the morphology and surface properties of nickel oxide prepared from different precursors. *Solid State Ionics*, 156(1-2), 233–243
- Fan, X., Burton, R. And Zhou, Y. (2010) Glycerol (Byproduct of biodiesel production) as a source for fuels and chemicals – mini review. *The Open Fuels & Energy Science Journal*, 2010 (3): 17-22
- Fogler, H.S. (2006). *Elements of Chemical Reaction Engineering*. 4th ed. Upper Saddle River, NJ, USA: Pearson Education, Inc.
- Foo, S.Y., Cheng, C.K., Tuan-Huy Nguyen and Adesina, A.A. (2012) Syngas production from CH₄ dry reforming over Co-Ni/Al₂O₃ catalyst: Coupled reaction-deactivation kinetic analysis and the effect of O₂ co-feeding on H₂:CO ratio. *International Journal of Hydrogen Energy*, 37, 17019-17026
- Freitas, A.C.D. and Guirardello, R. (2012). Oxidative reforming of methane for hydrogen and synthesis gas production: Thermodynamic equilibrium analysis. *Journal of Natural Gas Chemistry*, 21(2012)571–580.
- Freitas, A.C.D. and Guirardello, R. (2014). Comparison of several glycerol reforming methods for hydrogen and syngas production using Gibbs energy minimization. *International Journal of Hydrogen Energy*, 39(2014): 17969-17984.
- Gallo, A., Pirovano, C., Ferrini, P., Marelli, M., Psaro, R., Santangelo, S., Faggio, G. and Dal Santo, V. (2012). Influence of reaction parameters on the activity of ruthenium based catalysts for glycerol steam reforming. *Applied Catalysis B: Environmental*, 121– 122 (2012) 40– 49.
- Gan, P. K. and Li, Z. D. (2008) An econometric study on long-term energy outlook and the implications of renewable energy utilization in Malaysia. *Energy Policy* 36 (2008): 890–899
- Guo, J., Hou, Z., Gao, J and Zheng, X. (2008) Syngas production via combined oxy-CO₂ reforming of methane over Gd₂O₃-modified Ni/SiO₂ catalysts in a fluidized-bed reactor. *Fuel*, 87, 1348-1354.
- Huang, Z.Y., Xu, C.H., Meng, J., Zheng, C.F., Xiao, H.W., Chen, J. and Zhang, Y.X. (2014). Glycerol steam reforming to syngas over Ni-based catalysts on commercial Linde-type 5A zeolite modified by metal oxides. *Journal of Environmental Chemical Engineering*, 2(1): 598-604.

Iaquaniello, G., Antonetti, E., Cucchiella, B., Palo, E., Salladini, A., Guarinori, A., Lainati, A. and Basini, L. (2012). Natural gas catalytic partial oxidation: A way to syngas and bulk chemicals production. (online) <https://www.intechopen.com/> (14 January 2017)

International Energy Outlook. (2016). EIA projects 48% increase in world energy consumption by 2040. (online) <https://www.eia.gov/todayinenergy> (12 December 2016)

Iriondo, A., Barrio, V., Cambra, J., Arias, P., Güemez, M., Navarro, R., Sánchez-Sánchez, M. and Fierro, J. (2008). Hydrogen Production from glycerol over nickel catalysts supported on Al₂O₃ modified by Mg, Zr, Ce or La. *Topics in Catalysis*, 49(1-2), 46-58.

Iulianelli, A., Seelam, P.K., Liguori, S., Longo, T., Keiski, R., Calabro, V. and Basile, A. (2011). Hydrogen production for PEM fuel cell by gas phase reforming of glycerol as byproduct of bio-diesel. The use of a Pd-Ag membrane reactor at middle reaction temperature. *International Journal of Hydrogen Energy*, 36 (2011), 3827-3834

Jeong, H. and Kang, M. (2010) Hydrogen production from butane steam reforming over Ni/Ag loaded MgAl₂O₄ catalyst. *Applied Catalysis B: Environmental*, 95 (3-4) 446–455

Kim, J., and Lee, D. (2013). Glycerol steam reforming on supported Ru-based catalysts for hydrogen production for fuel cells. *International Journal of Hydrogen Energy*, 38(27), 11853-11862.

Kolesarova, N., Hutnan, M., Bodik, I. and Spalkova, V. (2011). Utilization of biodiesel by-products for biogas production. *Journal of Biomedicine and Biotechnology*, 2011.

Lean, H. H. and Smyth, R. (2010). CO₂ emissions, electricity consumption and output in ASEAN. *Applied Energy*, 87, 1858-1864.

Lean, H. H. and Smyth, R. (2014). Disaggregated energy demand by fuel type and economic growth in Malaysia. *Applied Energy*, 132, 168–177.

Lee, H. C., Siew, K. W., Gimbu, J. and Cheng, C. K. (2013). Application of Cement Clinker as Ni-Catalyst Support for Glycerol Dry Reforming. *Bulletin of Chemical Reaction Engineering & Catalysis*, 8(2).

Lee, H.C., Siew, K. W., Gimbu, J. and Cheng, C. K. (2014). Synthesis and characterisation of cement clinker-supported nickel catalyst for glycerol dry reforming. *Chemical Engineering Journal*, 255: 245-256

Lin, Y.C. (2013). Catalytic valorization of glycerol to hydrogen and syngas. *International Journal of Hydrogen Energy*, 38(6): 2678-2700.

- Luo, N., Fu, X., Cao, F., Xiao, T. and Edwards, P.P. (2008) Glycerol aqueous phase reforming for hydrogen generation over Pt catalyst—Effect of catalyst composition and reaction conditions. *Fuel*, 87 (2008) 3483–3489
- Malveda, M., Blagoev, M., Funada, C., and Liu, J. (2012). Glycerine. (online). <http://chemical.ihs.com/CEH/Public/Reports/662.5000> (24 May 2014)
- Mardhiah, H.H., Ong, H.C., Masjuki, H.H, Lim, S and Lee, H.V. (2017) A review on latest developments and future prospects of heterogeneous catalyst in biodiesel production from non-edible oils. *Renewable and Sustainable Energy Reviews*, 67, 1225-1236
- Mastny, L. (2005). Global fossil fuel consumption surges. (online). <http://www.worldwatch.org/global-fossil-fuel-consumption-surges> (16 May 2014)
- Montero, C., Remiro, A., Arandia, A., Benito, P.L., Bilbao, J. and Gayubo, A.G. (2016) Reproducible performance of a Ni/La₂O₃- α Al₂O₃ catalyst in ethanol steam reforming under reaction-regeneration cycles. *Fuel Processing Technology*, 152 (2016), 215-222
- Montini, T., Singh, R., Das, P., Lorenzut, B., Bertero, N., & Riello, P. et al. (2010). Renewable H₂ from Glycerol Steam Reforming: Effect of La₂O₃ and CeO₂ Addition to Pt/Al₂O₃ catalysts. *Chemistry & Sustainability* 3(5), pp.619-628.
- Nor Shahirah, M.N., Gim bun, J., Asmida Ideris, Maksudur R. Khan and Cheng, C.K. (2017). Catalytic pyrolysis of glycerol into syngas over ceria-promoted Ni/ α -Al₂O₃ catalyst. *Renewable Energy*, 107, 223-234
- Organization of the Petroleum Exporting Countries (OPEC) (2010) World oil outlook 2010. (online). http://www.opec.org/opec_web/static_files_project/media (16 May 2014)
- Pairojpiriyakul, T., Croiset, E., Kiatkittipong, W., Kiatkittipong, K., Arpornwichanop, A. and Assabumrungrat, S. (2013). Hydrogen production from catalytic supercritical water reforming of glycerol with cobalt-based catalysts. *International Journal of Hydrogen Energy*, 38(2013) 4368-4379
- Parizotto N.V., Rocha, K.O., Damyanova, S., Passos, F.B., Zanchet, D., Marques, C.M.P. and Bueno, J.M.C. (2007). Alumina-supported Ni catalysts modified with silver for the steam reforming of methane: Effect of Ag on the control of coke formation. *Applied catalysis A: General*, 330, 12-22.
- Pena, M.A., Gomez, J.P. and Fierro, J.L.G. (1996). New catalytic routes for syngas and hydrogen production. *Applied Catalysis A: General*, 144, 7-57.
- Quispe, C.A.G., Coronado C.J.R. and Carvalho Jr., J.A. (2013). Glycerol: Production, consumption, prices, characterization and new trends in combustion. *Renewable and Sustainable Energy Reviews*, 27 (2013) 475–493

Renewable Energy Policy Network for the 21st Century. (2016) Renewable 2016 Global Status Report. (online) <http://www.ren21.net/status-of-renewables/global-status-report/> (14 January 2017)

Ross, J.R.H., van Keulen, V.N.J., Hegarty, M.E.S. and Seshan, K. (1996). The catalytic conversion of natural gas to useful products. *Catalysis Today*, 30, 193-199

Rosetti, I., Gallo, A., Dal Santo, V., Bianchi, C.L., Nichele, V., Signoretto, M., Finocchio, E., Ramis, G. and Di Michele, A. (2012) Nickel catalysts supported over TiO₂, SiO₂ and ZrO₂ for the steam reforming of glycerol. *ChemCatChem*, 5, 294-306.

Shaikh, P.H., Mohd Nor, N., Sahito, A.A., Nallagownden, P., Elamvazuthi, I. and Shaikh, M.S. (2016). Building energy for sustainable development in Malaysia: A review. *Renewable and Sustainable Energy Reviews, In Press*

Shao, S., Shi, A.W., Liu, C.L., Yang, R.Z. and Dong, W.S. (2014). Hydrogen production from steam reforming of glycerol over Ni/CeZrO catalysts. *Fuel Processing Technology*, 125, 1-7.

Shirai, T., Watanabe, H., Fuji, M. and Takahashi, M. (2009). Structural properties and surface characteristics on aluminium oxide powders. *Ceramic Foundation Engineering Research Center Annual Report*, 9: 23-31

Siew, K.W., Lee, H.C., Gimbun, J. and Cheng, C. K. (2014). Characterization of La-promoted Ni/Al₂O₃ catalysts for hydrogen production from glycerol dry reforming. *Journal of Energy Chemistry*, 23(1): 15-21.

Siew, K.W., Lee, H.C., Gimbun, J. and Cheng, C.K. (2013). Hydrogen Production via Glycerol Dry Reforming over La-Ni/Al₂O₃ Catalyst. *Bulletin of Chemical Reaction Engineering & Catalysis*, 8(2).

Slinn, M., Kendall, K., Mallon, C. and Andrews, J. (2008). Steam reforming of biodiesel by-product to make renewable hydrogen. *Bioresource Technology*, 99 (2008) 5851–5858.

Tan, H.W., Abdul Aziz, A.R. and Aroua, M.K. (2013). Glycerol production and its applications as a raw material: A review. *Renewable and Sustainable Energy Reviews*, 27(2013)118–127.

The Sustainability Cooperative. (2016) What are differences between biofuel, bioethanol, biodiesel and biogas? (online) <https://thesustainabilitycooperative.net/2013/12/26/the-difference-between-biofuel-bioethanol-biodiesel-and-biogas/> (14 January 2017)

Thyssen, V.V., Maia, T.A. and Assaf, E.M. (2013) Ni supported on La₂O₃–SiO₂ used to catalyze glycerol steam reforming. *Fuel*, 105 (2013): 358–363

Valle, B., Alonso, A., Atutxa, A., Gayubo, A. G. and Bilbao, J. (2005) Effect of nickel incorporation on the acidity and stability of HZSM-5 zeolite in the MTO process. *Catalysis Today*, 106 (2005), 118–122

- Valle, B., Remiro, A., Aguayo, A.T., Bilbao, J. and Gayubo, A.G. (2013) Catalysts od Ni/ α -Al₂O₃ and Ni/La₂O₃- α Al₂O₃ for hydrogen production by steam reforming of bio-oil aqueous fraction with pyrolytic lignin retention. *International Journal of Hydrogen Energy*, 38 (2013), 1307-1318.
- Wang, X., Li, M., Li, S., Wang, H., Wang, S. and Ma, X. (2010) Hydrogen production by glycerol steam reforming with/without calcium oxide sorbent: A comparative study of thermodynamic and experimental work. *Fuel Processing Technology*, 91(12): 1812-1818.
- Wang, X., Li, M., Wang, M., Wang, H., Li, S., Wang, S. and Ma, X. (2009) Thermodynamic analysis of glycerol dry reforming for hydrogen and synthesis gas production. *Fuel*, 88(11): 2148-2153.
- Wu, C., Wang, Z., Williams, P.T. and Huang, J. (2013). Renewable hydrogen and carbon nanotubes from biodiesel waste glycerol. *Scientific Report*, 3: 2742.
- Wu, C and Williams, P.T. (2009). Hydrogen production by steam gasification of polypropylene with various nickel catalysts. *Applied Catalysis B: Environmental*, 87(3-4): 152-161.
- Yang, G., Yu, H., Huang, X., Peng, F. and Wang, H. (2012). Effect of calcium dopant on catalysis of Ir/La₂O₃ for hydrogen production by oxidative steam reforming of glycerol. *Applied Catalysis B: Environmental*, 127, 89-98.