PLASTIC TO FUEL: THE EFFECT OF REAL PLASTIC WASTES COMPOSITION

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Thesis submitted in partial fulfilment of the requirements for the award of the degree of Bachelor of Chemical Engineering

Faculty of Chemical & Natural Resources Engineering UNIVERSITI MALAYSIA PAHANG

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Dedicated to my father, and my mother. They are reason of my existence and the only reason I keep going

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ABSTRACT

Plastic is a major composition in municipal waste. Depleting of fossil fuel leads to exploration of alternative fuel production including converting plastic waste to fuel. The objective of this of study is to investigate the effect of real plastic waste composition on a pyrolysis process to fuels. Plastic wastes that compose of shampoo bottle, plastic bag, plastic wrapper and polystyrene were used. Thermal decomposition study of the plastic wastes was done by using Thermogravimetric Analysis. The catalyst used in this research is oil palm biomass ash catalyst. It was cleansed and calcined at 750°C (15°C.min⁻¹) for four hours. Then, the catalyst was then crushed and sieved to have homogenized size of $< 125 \mu m$. The catalyst was characterized by using Scanning Electron Microscope (SEM) with Energy Dispersive X-Ray (EDX) and Brunauer, Emmett and Teller (BET). Nitrogen gas was used to provide oxygen free condition during the investigation. The plastic waste and catalyst weight ratio was set at 10:1. The catalyst was tested in a batch one litre borosilicate reactor and heated up to 450 °C for 30 minutes. The plastic wastes decomposed into liquid, solid residue and gas. The liquid product was collected in a condenser, while the uncondensed gas was collected in the gas bag. The composition of the liquid fuel was analyzed by using Mass spectrometry gas chromatography (GC-MS). The calorific value, moisture, density, turbidity, cetane and octane number of the liquid fuel were also determined. Gas composition of the gas product was determined via Thermal Conductivity Detector gas chromatography (GC-TCD). About 40% of liquid fuel was produced after the pyrolysis for shampoo bottle. The application of catalyst significantly improved the liquid production to 50% of liquid fuel. Liquid fuel quality with averagely high octane number for shampoo bottle and polystyrene are 100 and 98 respectively. Low moisture content (<3 %) was observed in all liquid fuels. The calorific value ranging from 2885.36 cal/g - 4209.31 cal/g was achieved for all plastics samples. A gas product that rich in methane (±3mol%) was obtained. In conclusion, the application of catalyst that derived from waste creates a low cost alternative fuel production via catalytic plastic waste pyrolysis.

ABSTRAK

Bahan fosil api yang semakin berkurang mengilhamkan kaedah bahan api alternatif termasuk menukar sisa plastik kepada bahan api. Objektif pengajian ini adalah untuk mengkaji kesan komposisi plastic sampah sebenar pada proses pirolisis kepada bahan api. Sisa plastik yang dikomposisikan daripada botol syampu, beg plastik, plastik pembungkus dan polistirena, telah digunakan. Kajian penguraian terma bagi sisa plastik telah dilakukan dengan menggunakan 'Thermogravimetric Analysis'. Pemangkin yang digunakan dalam kajian ini adalah pemangkin abu kelapa sawit. Ia telah dibersihkan dan dikalsin pada 750°C dengan 15°C.min⁻¹ selama empat jam. Kemudian, pemangkin telah dihancurkan dan disaring untuk mempunyai saiz <125µm. Pemangkin telah dicirikan dengan menggunakan 'Scanning Electron Microscope' (SEM) dengan 'Energy Dispersive X-Ray' (EDX) dan 'Brunauer, Emmett and Teller' (BET). Gas nitrogen telah digunakan untuk menyediakan keadaan bebas oksigen semasa siasatan dijalankan. Sisa dan pemangkin nisbah berat plastik telah ditetapkan pada 10:1. Pemangkin ini telah diuji di dalam satu liter borosilikat reaktor dan dipanaskan sehingga 450° C selama 30 minit. Sisa plastik telah diuraikan kepada cecair, sisa pepejal dan gas. Produk cecair telah dikumpulkan di dalam pemeluwap, manakala gas yang tidak meluwap telah dikumpulkan dalam beg gas. Komposisi bahan api cecair telah dianalisis dengan menggunakan 'Mass spectrometry gas chromatography' (GC-MS). Jumlah nilai kalori, kelembapan, ketumpatan, kekeruhan, cetana dan oktana bahan api cecair juga telah ditentukan. Komposisi gas produk gas telah dianalisis melalui 'Thermal Conductivity Detector gas chromatography' (GC-TCD). Sebanyak 40% bahan api cecair diperloleh selepas pirolisi. Pengunaan pemangkin menunjukkan peningkatan yang ketara kepada 50% bahan api cecair. Kualiti bahan api cecair dengan purata nombor yang tinggi iaitu 100 oktana untuk botol syampu dan 98 untuk polistirena, kandungan lembapan yang rendah (< 3%). Rangkaian nilai kalori petrol yang bermula daripada 2885.36 kalori/g -4209.31 kalori/g dan produk gas yang kaya dengan metana (\pm 3 mol%) telah diperolehi untuk semau jenis plastik. Kesimpulannya, pengunaan pemangkin yang terhasil daripada sisa menghasilkan bahan api alternatif yang berkos rendah.

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LIST OF ABBREVIATIONS

- HDPE High density polyethylene
- LDPE Low density polyethylene
- PE-Polyethylene
- PP Polyethylene
- PS-Polystyrene
- SPI Society of Plastic Industry
- GC Gas Chromatography
- MS Mass Spectrometry
- TGA Thermal Gravimetric Analysis
- SEM Scanning electron microscope
- POMA Palm Oil Mill Ash

CHAPTER 1

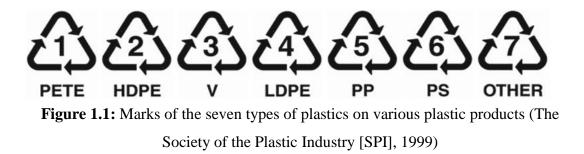
INTRODUCTION

1.1 Background of the Study

Plastic is a high molecular weight material that was invented by Alexander Parkes in 1862 (Brydson, J.A 1999). Plastics are made off inorganic and organic raw materials, such as carbon, silicon, hydrogen, nitrogen, oxygen and chloride. The basic materials used for making plastics are extracted from oil, coal and natural gas (Seymour, 1989). Plastics are made off long chain polymeric molecules (Scott, 1999). Plastics are not presently biodegradable and are extremely troublesome components for landfilling (Ali et al., 2004). In order to assist recycling of the waste plastic, Society of Plastic Industry (SPI) defined a resin identification code system that divides plastics into seven groups based on the chemical structure and applications (The Society of the Plastic Industry [SPI], 1999) They are:

- I. PET (Polyethylene Terephthalate)
- II. HDPE (High Density Polyethylene)
- III. PVC (Polyvinyl Chloride)
- IV. LDPE (Low Density Polyethylene)
- V. PP (Polypropylene)
- VI. PS (Polystyrene)
- VII. Other

Those seven types of plastics are marked on various plastic products as (The Society of the Plastic Industry [SPI], 1999):



Due to the convenience to manufacturing and use, Malaysian domestic plastic production has been increasing since 2001 from RM 4.78 billion to RM 7.25 billion in 2013 as shown in Figure 1-2. (Department of Statistics MATRADE, Malaysia).

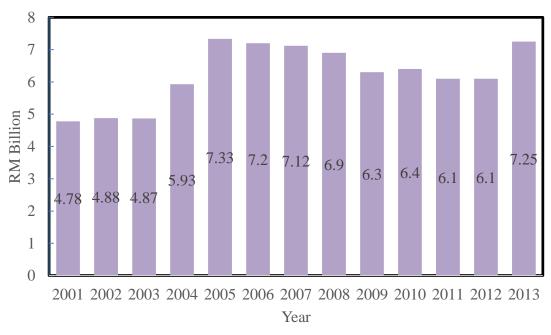


Figure 1.2: Domestic Production of plastic from 2001 till 2013 (Department of Statistics MATRADE, Malaysia)

One of the major concerns for extensive use of the plastics is the disposal of the waste plastic. Since 1999 till 2009, municipal solid waste in Malaysia has increased about 46% (27284 tonnes/day) and 19% of it is plastic waste (Agamuthu and Fauziah, 2009). Plastic waste is hard to decompose naturally and they are non-degradable material. Several method of solid waste disposal is introduced to manage the municipal solid waste such as recycling, composting, incineration, inert landfills, and sanitary landfill, but most of them is not very favorable in term of cost (incineration technology), and area capability for landfilling. Malaysian laws are too general and unsatisfactory

due to lack of resources and municipal budget constraint. The budget for waste collection was ranging from 20% to 70%, based on the size of the municipality (Hassan et al., 2000). Waste are also dumped in the river. For example, it is reported that 31.9% of waste were disposed by open burning, while 6.5% were dumped into the river system in Kuala Lumpur alone (Murad and Siwar, 2007). This has triggered to find an alternative solution for solid waste management where it is affordable and has a great turnover benefit. Pyrolysis is the future process for waste management and alternative energy source. Pyrolysis of plastic was introduced in the early 90's and still being carry out until today. The process has a wide range of potential market including the conversion of plastic to gasoline-diesel fuel (Buekens & Huang, 1998) and the solid product produce can be use as charcoal and fertilizer (Iwuagwu and Ugwuanyi, 2014). However, the optimum pyrolysis process is still ongoing.

1.2 Motivation

Municipal solid waste generation in Malaysia has increased significantly ranging between 25000 – 30000 tons per day (Johari et al., 2014). This shows that the municipal solid waste in Malaysia has not been handle properly in term of the method of the managing solid waste. Besides that, crude oil reserves are vanishing at the rate of 4 billion tonnes a year, and if we continue at this rate without any increase for our growing population or aspiration, our known reserves will be gone by 2052 (Tathagat et al., 2015). The pyrolysis technology can assist reducing this problem by generating alternative energy source. Moreover, the final motivation is regarding oil palm mill ash. Oil palm mill generates large quantities of oil palm product which lead to generate a strong pollutant; amenable to microbial degradation because it is rich in carbon, nitrogen, and minerals. (Iwuagwu and Ugwuanyi, 2014). Oil palm mill ash from oil palm mill boiler is also rich in metal mineral including alumina and silica which can be reuse such as for geopolymer material. Silica and alumina are among typical metal that use in catalyst production.

1.3 Problem Statement

Although pyrolysis to convert waste to fuel has been done by several researchers, the main obstacle to commercial this technology is due to low yield and low product fuel quality. The application of the screw kiln reactor process with the presence of oxygen resulted to produce fuel that rich in alcohol (Serrano et al., 2003). In comparison to commercial fuel quality which rich in aromatics, implementation of catalyst like zeolite and alumina is necessary. It is reported that zeolite, ZSM-5 catalyst effectively improves pyrolysis process in term of fuel quality and the yield of the fuel produce (Miskolczi et al., 2009). Zeolite catalyst is quite expensive. It is not economical for mass production. Therefore, the application of oil palm ash waste that rich in carbon minerals (Iwuagwu and Ugwuanyi, 2014) has huge potential to be use as a catalyst and produce better fuel quality and yield. This also improves environment conservation as well as municipal waste and agricultural waste management. In this investigation, a pyrolysis of plastic waste to fuel by using catalyst that derived from oil palm ash is carried out.

1.4 Objectives

The objective of this study is to investigate the influence of real waste plastic composition in the catalytic pyrolysis to fuel by using oil palm biomass ash catalyst.

1.5 Scopes of Study

The following are the scope of this research:

- The thermal decomposition of plastic waste was done by using Thermal Gravimetric analyser.
- 2) The catalyst was prepared by calcining the catalyst at 750 °C for four hours.
- The experiment of pyrolysis of plastics waste to fuels was set up to test the catalyst performance at 450°C for 30 minutes.
- 4) The gas product composition was determined via GC-TCD. The catalyst was analyzed before the experiments via SEM and BET. The effect of plastic composition on product yield was studied by varying the plastic waste source

including shampoo plastic bottle, plastic bag and polystyrene food container and the mixture of the plastic sources.

5) The analysis of liquid product and characteristics was determined by various analyses in comparison to commercial product.

CHAPTER 2

LITERATURE REVIEW

2.1 Plastics and pyrolysis

Plastic is major components in municipal waste. The abundant amount of plastic waste is due to is massive application in human daily life especially in packaging services. Thus, converting plastic to valuable product is necessary, as plastics decomposition will take for ages. Converting plastics to energy like liquid fuel via pyrolysis interest many researchers recently. Pyrolysis is a thermal cracking process to either gas, solid or liquid product without oxidant. The main factors that effecting the pyrolysis of plastic is the type of plastic, cracking temperature, heating rate, operation pressure, reactor type, residence time and the application of catalyst.

2.2 Type of plastic

The pyrolysis products are related to the chemical composition and chemical structure of the plastics to be pyrolyzed. Plastics can be classified based on its structural shape of polymer molecules, as linear, branched, or cross-linked as illustrated in Figure 2.1.

There is a significant relationship between the density and the branching intensity of polymers. For HDPE and LDPE polymers both of them have the same chemical formula which is $-(CH_2-CH_2)_n$, what differentiate them is, branched polyethylene is also called low density polyethylene (LDPE) which is different from linear polyethylene that is called high density polyethylene (HDPE) (Chanda, 2000). The PE with more branches has relatively lower density (McMurry, 2000).

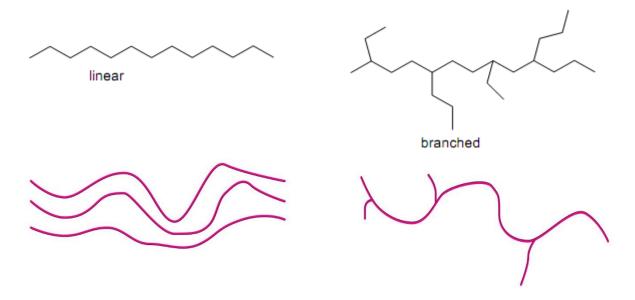


Figure 2.1: Polymer structure, linear and branched

For LDPE polymer there are about 20 branches per 1000 carbon atoms. The relative molecular mass, and the branching, influence the physical properties of LDPE. The branching affects the degree of crystallinity which in turn affects the density of the material. LDPE is generally amorphous and transparent with about 50% crystallinity. The branches prevent the molecules fitting closely together and so it has low density (McMurry, 2000).

The HDPE molecules can fit closer together. This leads to strong intermolecular bonds, making the material stronger, denser and more rigid than LDPE. The polymer is not transparent (McMurry, 2000).

For polystyrene (PS) it is called linear polymer although it contains functional groups as part of the monomer structure (Figure 2.2). The chemical formula of PS is – $[CH_2-CH(C_6H_5)]_n$ –. In branched polymers, at least one of the monomers is connected to more than two functional groups due to the branching points produced from the polymerization process. The functional side group and the branch structure have significant effects on the pyrolysis product. For example, the dominant component in PS pyrolysis products is styrene that is the side group come off from PS carbon backbone. (Karaduman et al., 2001) (Arandes et al., 2003).

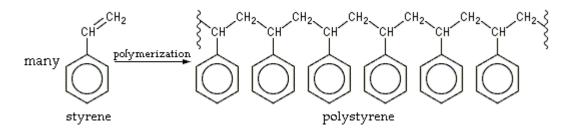


Figure 2.2: Polystyrene chemical structure

2.3 Cracking Temperature and Heating rate

Temperature is one of the most important operating variable, since the temperature dominates the cracking reaction of the polymer materials (Aboulkas et al., 2012).

It is known that pyrolysis temperature plays an important role on product distribution. As material reaches elevated temperatures, the different chemical components undergo thermal degradation that affects the conversion yield and product quality. Aboulkas *et al.* (2012) reported that the increase of the pyrolysis temperature from 400 to 500 – 520 °C caused a significant increase in the oil and gas yields as shown in table 2.2.1. This result was attributed to gas phase cracking reactions to yield increased hydrocarbons. At low temperatures, \leq 400 °C, oil yields are reduced because of the coking reactions of the oil via conversion of the liquid oil to solid product and/or incomplete pyrolysis. There is consequently an optimum temperature where maximum oil yields are obtained.

The major effect of temperature reflects as a change in the yield of gaseous products: as temperature increases, the amounts of gaseous products increase which results as an increase in aliphatic hydrocarbon recovery (Aboulkas et al., 2012). Many studies have shown that temperature has a significant effect on yield and composition of pyrolysis products of polyethylene and polypropylene in a fluidized bed reactor or fixed bed (Aguando et al., 2006; Bagri, & Williams, 2002; Lee, 2006). It has been observed for most of the works that the oil yield increases as the temperature rises and the maximum oil yield produces at 500–550 °C. It is claimed that relatively low pyrolysis temperatures (around 400 °C) favors solid residue formation. Temperatures up to 500–525 °C maximize the production of oils and temperatures above 600 °C maximize gaseous products while minimizing solid residue formation.

Different locations of the temperature sensors in different studies are believed to be one of the most important factors on the different cracking temperature reported (Karaduman et al., 2001). Table 2.1 shows the effect of temperature on the product yield from the pyrolysis of plastics.

Type of plastic	Heating rate (°C)	400	450	500	525	550	600
HDPE	Conversion	93.9	95	99.3	99.6	99.7	99.7
	Oil	85	85.6	88.3	86.1	84.2	82.1
	Gas	8.9	9.4	11	11.7	13.4	16
	Char	6.1	5	0.7	0.4	0.3	0.3
LDPE	Conversion	94.1	95.2	99.5	99.6	99.7	99.7
	Oil	87.2	87.9	89.6	88.6	86.6	84.2
	Gas	6.9	7.3	9.9	11	13.1	15.5
	Char	5.9	4.8	0.5	0.4	0.3	0.3

 Table 2.1: Influence of temperature on the product yield from the pyrolysis of plastics

 (Aboulkas et al., 2012)

Aboulkas et al., (2012) reported that as the heating rate increases, the conversion degree and the yield of gases increase and the yields of oils and char decrease when HDPE and LDPE plastic was pyrolysed. In this work, increasing the heating rate higher than 10 °C min⁻¹, from 10 to 20 °C min⁻¹, caused a slight decrease of 0.8 wt.% in the oil yield as shown in Table 2.2. This slight decrease in the oil yield may be attributed to no more effect of the heating rate on the self-generated (autogenous) gas sweep pyrolysis.

Williams & Williams (1998) suggest that the pyrolysis process may be a diffusion-limited process controlled by heat and product diffusion. They suggest that the extent of diffusion control increases at high heating rates because products are generated faster than they can diffuse out of the pores, consequently secondary coking reactions

will occur. The extent of diffusion control diminishes during the course of the reaction as the shale changes from impervious rock to porous ash as the pyrolysis products leave the matrix. Table 2.2 shows the effect of heating rate on the product yield from the pyrolysis of plastics.

`	Heating rate	2	5	10	15	20
	(°C/min)					
HDPE	Conversion	97.3	98.4	99.3	99.4	99.6
	Oil	88.6	88.5	88.3	87.8	87.4
	Gas	8.7	9.9	11	11.6	12.2
	Char	2.7	1.6	0.7	0.6	0.4
LDPE	Conversion	97.4	98.9	99.5	99.6	99.7
	Oil	89.9	89.8	89.6	88.7	88.3
	Gas	7.5	9.1	9.9	10.9	11.4
	Char	2.6	1.1	0.5	0.4	0.3

 Table 2.2: Influence of heating rate on the product yield from the pyrolysis of plastics

 (Aboulkas et al., 2012)

2.4 Type of reactor

In the batch reactor, the materials are fed into the reactor in batches for pyrolysis either at the start of the process or after all of the fed materials are processed. In Onwudili et al., (2009) works, a 300 mL Parr Mini Bench Top Reactor, Type 4561m stirred pressure reactor made of T 316 stainless steel was used. The reactor was heated using an external mantle type furnace, which contacted the sides and bottom of the reaction vessel. A J thermocouples was use and increment of 10°C of the heating rate. Nitrogen gas was used as reaction atmosphere for all experiments to ensure inert pyrolysis condition. Each experiment was carried out with an initial nitrogen pressure of 0.3 MPa. About 10 g of sample was used in each experiment. A set of experiments was carried out for 1 h each between 350 and 500 °C. After the reactor had cooled, three samples of gas product were carefully taken for gas chromatography analysis. The remaining gas was then discharged, the reactor opened and the vessel weighed to determine then weight of liquid and char products. The char was then separated from the oil by filtration and weighed. Finally, oil from the reactor vessel was transferred into amber glass bottles and placed in a refrigerator until further analysis. The setup of the experiment as shown in figure 2.3.

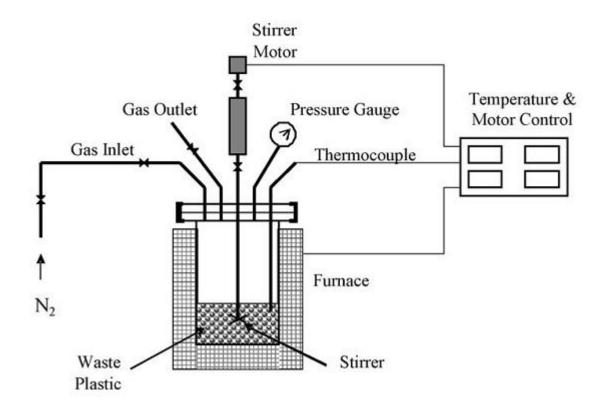


Figure 2.3: Experiment setup for closed batch reactor (Onwudili et al., 2009)

A semi-batch reactor removes the pyrolysis products continuously once they are generated but the feed materials are added initially before the pyrolysis process starts. Some semi-batch process uses inert carrier gas to help remove the pyrolysis products. Kumar and Singh, (2011) use a semi batch reactor is use and is made of stainless steel tube (length-145 mm, internal diameter-37 mm and outer diameter-41 mm) sealed at one end and an outlet tube at other end as shown in Figure 2.4. The reactor is heated externally by an electric furnace, with the temperature being measured by a Cr-Al: K type thermocouple fixed inside the reactor, and temperature is controlled by an external PID controller. About 20g of waste plastics sample were loaded in each pyrolysis reaction. The condensable liquid products/wax were collected through the condenser and weighed. After pyrolysis, the solid residue left inside the reactor was weighed. Then the weight of gaseous/volatile product was calculated from the material balance. Reactions were carried out at different temperatures ranging from 400-550°C.

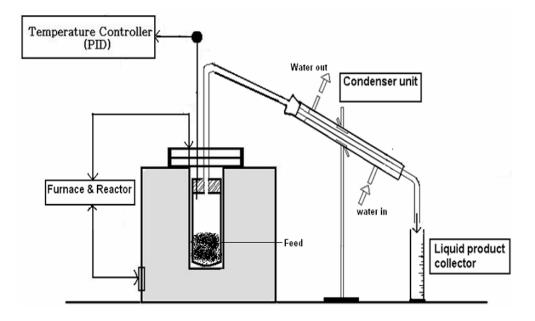


Figure 2.4: Semi-batch reactor pyrolysis process setup (Kumar and Singh, 2011)

In the continuous reactor, the feed materials are input from one part and the products are led out from the other part of the reactor. According to Li et al., (2004) research, a continuous rotary kiln reactor was use for the pyrolysis of scrap tires. The reactor consisted of a pyrolytic rotary kiln main reactor and peripheral systems including a supply system (a storage bin with a screw feeder), a tar condenser and reservoir, a solid residue collection tank, a flue gas cleaner, a demister filter, a gas burner, and an effluent gas sampling system as shown in Figure 2.5.

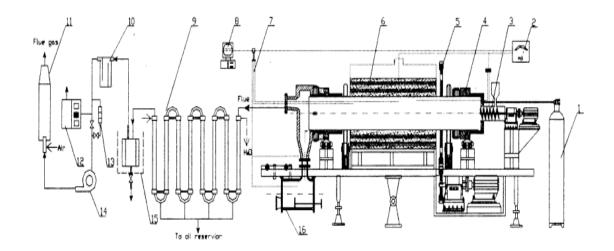


Figure 2.5: Schematic of pilot-scale rotary kiln pyrolysis reactor (Li et al., (2004)

The kiln was designed for continuous operation with tire powder conveyed from a sealed container to the electrically heated rotary kiln by a screw feeder. The feeding rate was regulated from 10 to 30 kg/h. The kiln diameter was 0.3 m, and the overall length was 3.0 m. The effective heated length of the kiln was about 1.8 m. The solids were transported in the kiln as a result of inclination and rotation. At the kiln exit, the residue char fell into a sealed 6 L container. The evolved oil vapors and gases were quickly removed from the reactor by a special induced fan to reduce the residence time. The condenser, with four coils cooled by water and a trap refrigerated by ice, was used to recover pyrolytic oils into the reservoirs. The non-condensable gases passed to the scrubbing unit to remove the acids and finally passed to the burner.

2.5 Residence time

In fast pyrolysis or continuous pyrolysis process, it refers to the contact time of the plastic on the hot surface throughout the reactor. However, in slow pyrolysis and batch process, the residence time means the duration from the time when feedstock plastic start to be heated to the time when the products are removed. Longer residence time favors a further conversion of the primary products thus yielding more thermal stable products such as light molecular weight hydrocarbons, non-condensable petroleum gases. (Miller et al., 2005; Hernández et al., 2006). In a slow pyrolysis, long residence time encourages the carbonization process and produces more tar and char in

Process	Heating rate	Residence	Temperature	Target	
		time	°C	Products	
Slow	Very low	days	450 - 600	Charcoal	
carbonization					
Slow pyrolysis	10 -100K/min	10 – 60 min	450 - 600	Gas, oil, char	
Fast pyrolysis	Up to 1000K/s	0.5 – 5 s	550 - 650	Gas, oil, char	
Flash pyrolysis	Up to	<1 s	450 - 900	Gas, oil, char	
	10000K/s				

Table 2.3: Pyrolysis processes and target products (Jung and Fontana 2006)

In the López et al., (2011) studies, the effect of time versus the product yield was conducted. A 3.5 dm³ semi batch reactor was use at atmospheric pressure with a nitrogen purging at 50 ml/min. The temperature for pyrolysis process was at 500°C with a heating rate of 20°/min. The plastic use was polyethylene and the experiment was conducted for 2 hours to see the effect of time towards product yield as shown in Figure 2.6. It shows that the optimum time for pyrolysis of polyethylene at 500°C is between 25 - 50 min. This is because after 50 minutes, there is less different in the product yield especially for the liquid product yield. If the experiment were conducted longer than 50 minutes, it means that a higher energy consumption which related to cost loss as the product yield does not have a significant change.

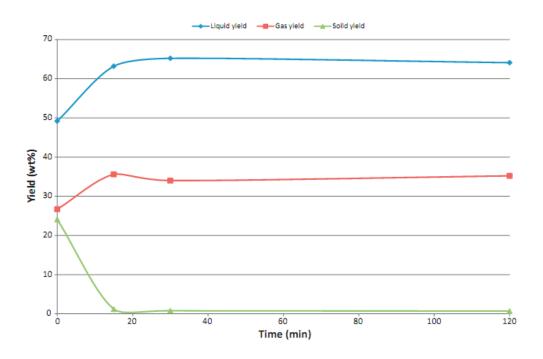


Figure 2.6: Pyrolysis yield (wt%) as a function of time at 500°C (López et al., 2011)

2.6 Catalyst

Catalysts are used in most cases to modify the structure of products and decrease the energy consumption. However, the addition of the catalyst can be troublesome, e.g. the catalyst might be accumulated in the residue or coke (Williams and Williams, 1997). Generally used catalysts for pyrolysis of plastic wastes are mordenite, fluid catalytic cracking (FCC, ZSM-5, etc., but the ZSM-5 and FCC catalysts provided the best possibility to yield hydrocarbons in the boiling range of gasoline. On the other hand, the structure of zeolite and its pore size fundamentally determine the cracking property of the catalyst Not only the structure of products, but also their yields can be considerably modified by catalysts. (Williams and Williams, 1997; Zadgaonkar, 2006; Masuda and Tago, 2006).

The presence of catalyst reduced the liquid fraction and increased the gaseous fraction. Theoretically, the catalyst can enhance the cracking reaction of the pyrolysis gas. Long chain hydrocarbons have been cracked into lighter hydrocarbon gases. Syamsiro et al., (2014) reported that pyrolysis over natural zeolite catalyst produced higher liquid product compared with Y zeolite catalyst. This is due to different activity

between natural zeolite and Y zeolite. Natural zeolite has lower BET surface area than that of Y zeolite. Higher surface area will give more contact between catalyst and pyrolysis gas which means more gas will be cracked to produce shorter chain hydrocarbons.

However, the presence of catalysts has slightly effect to the product yields. The impurity which contains some toxic materials will deactivate the catalysts. Thus, the catalysts will have the activity in the beginning of the reforming process and deactivate in the end of the process. (Syamsiro et al., 2014). Figure 2.7 shows the effect of different types of feedstocks on the product yield and the liquid fraction composition

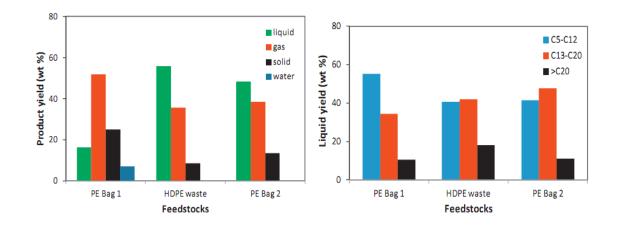


Figure 2.7: Effect of different types of feedstocks on (a) the product yields; and (b) the liquid fraction composition (Syamsiro et al., 2014).

2.6.1 Zeolite properties: pore size (structure) and Si/Al ratio (acidity)

Zeolites are crystalline micro-porous aluminosilicates. Therefore, Si/Al ratio is also an important parameter for zeolites which is applied to classify the zeolites (Barrer, R.M 1985). The high-silica zeolites, with a Si/Al ratio greater than five such as ZSM-5, are widely used in petrochemical industries (Maesen, T. 2007). These zeolites are preferred for polyolefin cracking. Lower Si/Al ratio implies lower acidity and smaller crystal size of zeolite provide higher efficiency in terms of conversion

2.6.2 Palm oil mill ash properties

The solid waste from palm oil mill industry has been increasing annually where it has been reported that the palm oil waste was produced 4 million tons/years in Malaysia only (Zarina et al., 2013). Hence, the solution to overcome the problems is to reuse the waste and produced new composites that are benefit. This ash contains silica (Si) which has potential to develop as geopolymer composites (Zarina et al., 2013). Palm oil fuel ash is rich in SiO₂ as tabulated in table 2.4 which is believed that it can be used as a catalyst for pyrolysis of plastic to replace ZSM-5.

Chemical Component	Palm Ash Composition, Malaysia (wt%)
SiO_2	51.18
Al ₂ O ₃	4.61
Fe_2O_3	3.42
CaO	6.93
MgO	4.02
SO_3	0.36
K ₂ O	5.52
Na ₂ O	0.06
Loi (Loss of ignition)	21.6

Table 2.4: Chemical composition of Palm Oil Mill Ash (Johari et al., 2012)

The high silica content in the catalyst makes the framework to stand high temperatures that this type catalyst is suitable for high temperature pyrolysis and regeneration cycle (Maesen, T. 2007). Figure 2.8 shows the original palm oil mill ash.



Figure 2.8: Original Palm Oil Mill Ash

Megat Johari et al., (2012) have done a research on how to improve the POMA with a certain treatment. Firstly, to remove the coarse particles such as fiber and kernel which are incomplete burned, the POMA was dried in oven at temperature $105 \pm 5^{\circ}$ C for 24 hours and then sieved passing through 300 in sieve. The following step was ground the POFA to achieve more fine particles and then heated again in furnace at temperature $500 \pm 5^{\circ}$ C for 90 minutes to remove unburned carbon and increase the pozzolanic properties. The research shows that the treated POFA will have a significant increase in SiO₂ which is prefer to become the catalyst for pyrolysis of plastic. Table 2.5 summarizes the chemical composition of ground and treated POMA.

Chemical Component	Ground POMA (wt%)	Treated POMA (wt%)
SiO ₂	51.18	65.01
Al ₂ O ₃	4.61	5.72
Fe ₂ O ₃	3.42	4.41
CaO	6.93	8.19
MgO	4.02	4.58
SO ₃	0.36	0.33
K ₂ O	5.52	6.48
Na ₂ O	0.06	0.07
С	19.05	0.09
LOI	21.6	2.53

Table 2.5: Chemical composition of treated POMA (Megat Johari et al., 2012

2.7 Pressure

Operating pressure has significantly effect on both the pyrolysis process and the products. The boiling points of the pyrolysis products are increased under higher pressure, therefore, under pressurised environment heavy hydrocarbons are further pyrolyzed instead of vaporized at given operation temperature (Miranda et al., 2001). Figure 2.9 shows the effect of pressure on hydrocarbon number and their fractions in the pyrolysis products of PE. In effect, under pressurized pyrolysis, more energy is required for further hydrocarbon cracking. It was also found that high pressure increases the yield of non-condensable gases and decreases the yield of liquid products. (Figure 2.10) The average molecular weight of gas product also decreases with the increase of pressure (Sato and Sakata, 2004).

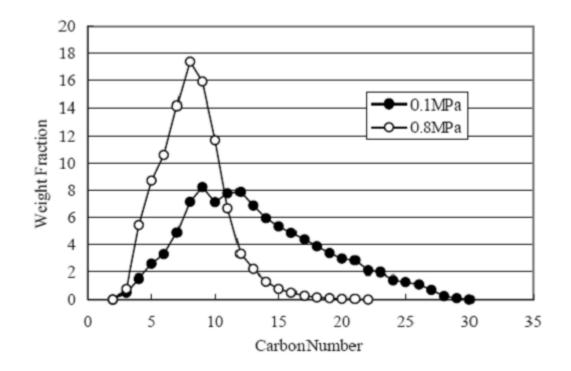


Figure 2.9: Effect of pressure on the distribution of PE pyrolysis product

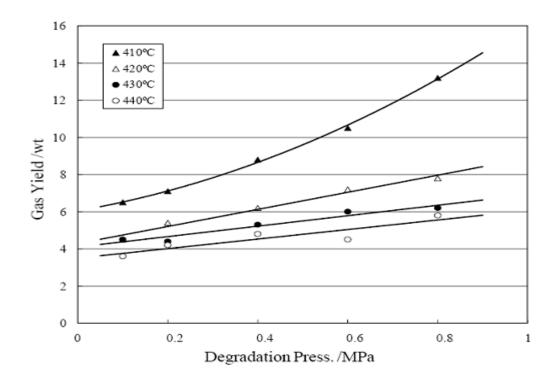


Figure 2.10: Effect of pressure on the yield of gas at different temperature (Sato and Sakata, 2004)

CHAPTER 3

METHODOLOGY

3.1 Introduction

This chapter describes detail description on material, catalyst preparation, sample preparation and testing method of the sample in catalytic pyrolysis of real samples wastes. The catalyst was tested with various type of samples including shampoo bottle, polystyrene and sample composition by mixing the samples at various weight ratio. The mixing composition is based on the real plastic composition in municipal waste.

3.2 Materials

The samples waste like shampoo bottle, plastic wrapper, plastic bag and polystyrene, were obtained at Kolej Kediaman 2 neighbourhood, Universiti Malaysia Pahang. Meanwhile, the oil palm ash was obtained from Lepar Palm Oil Mill, Kuantan, Malaysia. The nitrogen gas will be obtained from Malaysia Oxygen, MOX.



Figure 3.1: (a) Shampoo bottle (b) Plastic bag (c) Plastic wrapper (d) Polystyrene

3.3 Apparatus

Laboratory apparatus that was used are heating mantle, one-liter borosilicate flask, condenser, conical flask, thermocouple and stopwatch.

3.4 Plastics preparation

A shampoo bottle, plastic bag, plastic wrapper and polystyrene were used to represent HDPE, PP, LDPE and PS respectively. A mixture of 35% shampoo bottle, 35% plastic bag, 19% of plastic wrapper and 11% Polystyrene was also prepared. All samples were cleaned and cut into 0.5 - 1 cm pieces.

3.5 Plastics Characterization

The thermal decomposition behavior of the shampoo bottle (HDPE), plastic bag & plastic wrapper (LDPE), and polystyrene (PS) was analyzed at various temperatures via Thermogravimetric analyzer model TGA Q500 V6.7. About five mg of sample was placed in a platinum crucible. The sample was heated up to 890°C at a constant heating rate of 20 °C min⁻¹ in a nitrogen atmosphere at 100 ml min⁻¹. The TGA equipment is shown in figure 3.2.



Figure 3.2: TGA equipment

3.6 Catalyst preparation

The palm oil mill ash was calcined at 750°C for four hours with the increment of 15° C.min⁻¹. The calcine ash was further filter using a sieve filter of size 125 μ m. The catalyst was kept in a tightly seal container.

3.7 Catalyst Characterization

3.7.1 Catalyst pore structure

The BET surface analysis was used to measure the total specific surface area, pore size, and pore volume of the catalyst. The BET analysis was tested by Micromeritics ASAP 2020 Surface Area and Porosity Analyzer. BET analysis provides precise evaluation of materials by nitrogen multilayer adsorption measured as a function of relative pressure using a fully automated analyzer. In other word, the surface area was determined by adsorption of a monolayer of nitrogen molecules on the catalyst surface at the temperature of liquid nitrogen. The catalyst was degassed up to 200°C for six hours prior to analyze. The BET equipment is shown in figure 3.3.



Figure 3.3: BET equipment

3.7.2 Catalyst surface morphology

The fresh and spent catalysts surface topography was analyzed by using a high resolution SEM with an attachment with EDX by focusing electron beam over a surface to create an image. The electrons in the beam interact with the sample, producing various signals that can be used to obtain the information. The EDX technique used to identify the elemental composition of materials where the data generated by EDX analysis consist of spectra showing peaks corresponding to the elements making up the true composition of the sample being analyzed. Figure 3.4 shows the SEM with EDX equipment.



Figure 3.4: SEM with EDX equipment

3.8 Catalyst testing

The experiment setup is shown in Figure 3.7.1. The catalyst testing was carried out in the reactor rig consisted of round one-liter borosilicate flask, condenser, thermocouple, heating mantle, liquid collector and gas bag. A sample of including shampoo bottle, plastic wrapper, plastic bag and polystyrene was used. A mixture of 35% shampoo bottle, 35% plastic bag, 19% of plastic wrapper and 11% Polystyrene was also applied. The feed which consisted of plastic to catalyst at weight ratio of 10:1 was tested at 450°C for 30 minutes. Nitrogen, N₂ at 50 ml.min⁻¹ was used to purge oxidant to provide oxygen free environment and transport all the gases through the reactor. The vapor was passed through condenser. The liquid product was collected in a conical flask at the end of the condenser. The uncondensed gases were collected in a gas bag.

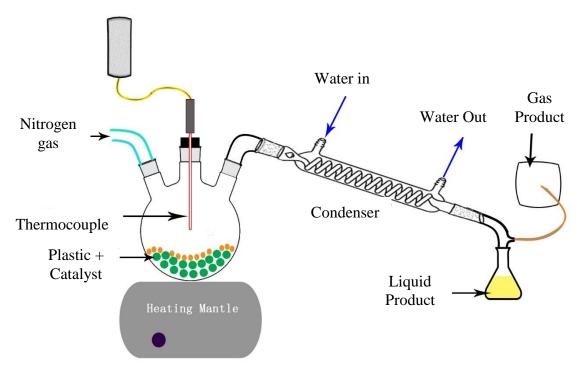


Figure 3.5: Experiment setup

3.9 Gas product Analysis

An Agilent 6890N Gas Chromatograph Thermal Conductivity Detectors (GC-TCD) that equipped with Haysep packed column was used to determine the compound of gas. The column oven was set at 50°C with Helium as the carrier gas flow at 10ml.min⁻¹. Figure 3.6 shows the GC-TCD equipment.



Figure 3.6: Gas Chromatograph Thermal Conductivity Detectors (GC-TCD)

3.10 Liquid product analysis

3.10.1 Product yield calculation

Product yield was determined after the experiment by calculating the mass difference of the apparatus before and after the experiment. The apparatus involved such as conical flask (liquid product), condenser (wax product), rotary flask (solid product). The gas product was determined by calculating the overall mass differences. The yield for the product is calculated using eq 3.1.

The yield percentages were determined by using the following equation,

$$Yield (\%) = \frac{Mass \ Liquid \ (g)}{Mass \ Total \ (g)} \times 100\% \qquad eq 3.1$$

3.10.2 Liquid composition

The liquid product was diluted to 10 fold with dichloromethane (DCM) A Agilent 5975C inert MSD Mass Spectrometry gas chromatography (GCMS) was used. The GC was equipped with DB1 capillary column. The detector and front inlet oven was set at 230 °C and 250 °C respectively. Figure 3.7 shows the GCMS equipment.



Figure 3.7: GCMS equipment

3.10.3 Calorific value

An oxygen bomb 1341 Parr calorimeter that equipped with 6775 Digital Thermometer was applied. About one ml of liquid fuel and 10 cm of titanium fuse was used. The bomb calorimeter was filled up with oxygen and fuse was ignited. Data was recorded for every minute until constant temperature was achieved. Figure 3.8 shows the oxygen bomb 1341 Parr calorimeter.



Figure 3.8: Oxygen bomb 1341 Parr calorimeter.

Calculation was performed to calculate the calorific value by using following eq 3.2

$$Hg = \frac{(\Delta T)(w) - (2.3 \times L)}{m}$$
 eq 3.2

Where:-

w is constant 2409.26 cal/°C

 ΔT is T_{final}-T_{initial} (°C)

L is length of fuse wire burn/consume (cm)

m is mass of sample use (gram)

3.10.4 Cetane and Octane number

The octane and cetane number of the liquid fuel was determined by using portable analyser of Octane Tester SX-200. The analyser was able to measure octane number of gasoline (RON, Research Octane Number), cetane number of diesel fuel, estimation of diesel fuel freezing temperature, purity level, and quality of motor, industrial and transformer (dielectric puncture potential) oil, Motor Octane Number (MON) and antiknock index (AKI (RON+MON)/2) simultaneously

3.11 Density, clarity, moisture content and viscosity

3.11.1 Density

Density was determined by weighting one ml of liquid sample on the analytical weight plate.

3.11.2 Clarity

Clarity is used to determine the extent to which light is either absorbed or scattered by suspended material in liquid fuel. A 2100P Portable Turbidimeter was used. Direct digital readout in NTU (nephelometry turbidity units). The clarity data in a range of 0 to 1000 NTU was achieved

3.11.3 Moisture

A Metrohm 787 KF Titrino with 703 Ti stand (Figure 3.9) was used to analyze moisture content. The Hydranal-Composite 5 reagent and Methanol dryer was used. Methanol dryer was pumped into titration vessel and stirring speed was controlled. Moisture was obtained by determining the volume of reagent and dryer.

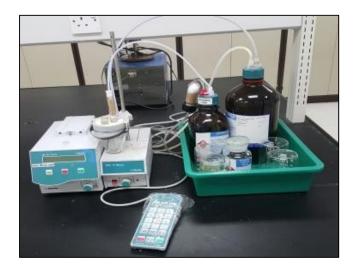


Figure 3.9: Moisture analysis equipment.

3.11.4 Viscosity

The viscosity and kinematic viscosity of the liquid fuel was determined by using Cole Parmer Viscosity bath EW-98928-30 as shown in figure 3.10.

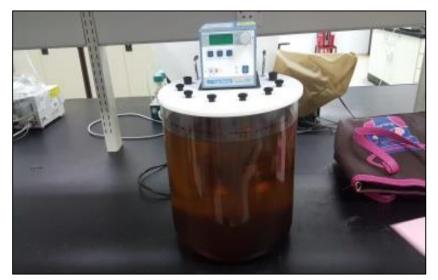


Figure 3.10: Viscosity and kinematic viscosity analysis equipment

The liquid fuel viscosity is in unit of centipoise (cP). Viscosity value was determined by using eq 3.3 and eq 3.4

Kinematic Viscosity
$$\left(\frac{mm^2}{s}\right) = Time(s) \times Viscometer Constant \left(\frac{mm^2}{s^2}\right)$$
 eq 3.3

Where: Viscometer Constant (150L) = $0.033320 \ mm^2/s^2$

Viscosity, mPs.s (cP) = Kinematic Viscosity
$$\left(\frac{mm^2}{s}\right) \times Density \left(\frac{g}{ml}\right)$$
 eq 3.4

The viscometer constant according to the Canon-fenske size is shown in table 3.1

Canon-fenske size	Viscometer Constant (mm2/s2)
25	0.002117
100	0.01512
150	0.03332
200	0.1098
350	0.4899
450	2.374

 Table 3.1: Viscometer Constant

CHAPTER 4

RESULTS AND DISCUSSION

4.1 Introduction

In this chapter, the experimental data and results are tabulated and discussed. This chapter begins by discussing the plastic characterization via TGA for shampoo bottle plastic waste. The characterization of the catalyst is also discussed thoroughly. The outcome of the catalyst testing including the product yield and the product properties are elaborated in this chapter too. The comparable of product to commercial fuel is also briefly done.

4.2 Plastics characterization

The thermogravimetric (TG) of shampoo bottle was carried out in nitrogen gas atmosphere. The thermogravimetric curve of shampoo bottle is presented in Figure 4.1. The detailed TGA analysis is in appendix A. As the evident from the figure 4.1, the degradation behaviors of shampoo bottle in the temperature between $430 - 520^{\circ}$ C. It also indicates that almost 96 wt% of the shampoo bottle decomposed. Shampoo bottle is originally made from virgin HDPE pellet.

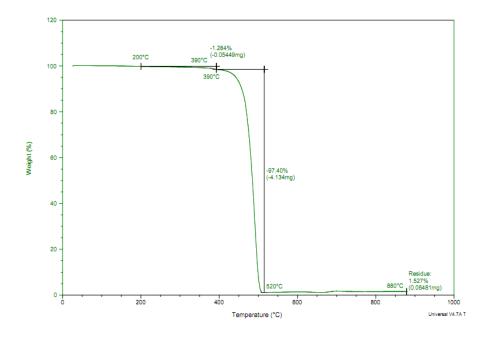


Figure 4.1: TGA Thermograms for shampoo bottle

The thermal degradation of the virgin HDPE is $420 - 490^{\circ}$ C (Ali and Qureshi 2011) which is quite similar with the shampoo bottle. It is believed that the reason why is there a slightly different in the final degradation temperature in the shampoo bottle because it has been added some additive to the plastic such as anti-oxidant, fillers, fire retardant and so on. Mineral flame retardant such as aluminum hydroxide and magnesium hydroxide mainly act as an additive which do not chemically attached to the surrounding system. The use of hydroxides is limited by their relatively low decomposition temperature which limits the maximum processing temperature of the polymers. This might also happen to other real waste plastic types like polystyrene (PS), plastic bag (PP) and plastic wrapper (LDPE) who share the same degradation profile. PP, PS and LDPE are reported to degrade at $430 - 500 \,^{\circ}$ C, $380 - 450 \,^{\circ}$ C and $400 - 500 \,^{\circ}$ C respectively (Ali and Qureshi, 2011) as shown in figure 4.2.

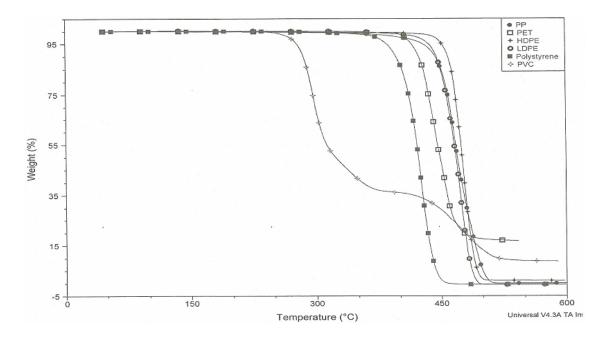


Figure 4.2: TGA thermograms for virgin plastics (Ali & Qureshi 2011)

4.3 Catalyst Characterization

4.3.1 Catalyst pore structure

For the BET analysis the surface area, pore size and pore volume of the catalyst was known. In this study the capability of adsorption and desorption of ash catalyst was determined. The result for the surface area, pore size and pore volume of the catalyst is tabulated in table 4.1. The raw data for the analysis is in appendix C.

I able 4.1: BET ash catalyst				
	Surface area (m ² /g)	Pore size (A)	Pore volume (cm ³ /g)	
Catalyst	0.695	316.962	0.005506	

It can be seen in Table 4.1 that the catalyst pore size is between 2 nm -50 nm. Thus, it is a mesoporous catalyst. Park et al. (2010) carried out investigation on Mesoporous ZSM-5 in pyrolysis of biomass. They reported that the mesoporous ZSM-5 catalyst promote the coke formation faster than conventional ZSM-5 catalysts. The presence of mesoporosity allowed for the formation of larger aromatics which were able to polymerize into coke and at higher temperatures these larger aromatics are more volatile and able to diffuse out of the mesopores of the sample (Foster et al., 2012).

4.3.2 Catalyst surface morphology

catalyst at different focal focus ranging from 1K-5K are shown in figure 4.4.

The generated SEM micrographs and EDX analysis for fresh calcined ash

2016/11/06 NMMD8.1 x3.0k 30 µm 2016/11/06 N D8.1 x4.0k 20

Figure 4.3: (a) Calcine ash catalyst 1K focus (b) Calcine ash catalyst 2K focus (c) Calcined ash catalyst 3K focus (d) Calcined ash catalyst 4K focus (e) Calcined ash catalyst 5K focus

Form the figure 4.3, it shows the catalyst has almost smooth surface area. Pores on the catalyst surface can also be observed in figure 4.3. In higher resolution catalyst image, large pore structure clearly can be observed distributed on the catalyst surface. It is a proof that the catalyst has mesoporous structure. The detailed SEM with EDX result is in appendix B

For the ash catalyst EDX analysis testing, the result is show in figure 4.4 and table 4.2.

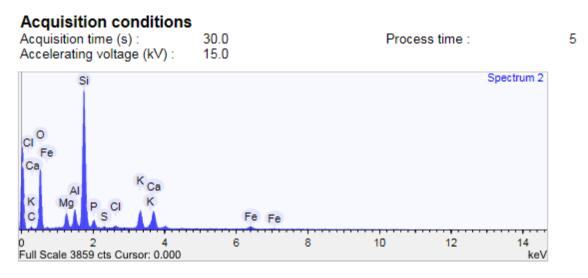


Figure 4.4: Elemental EDX analysis for calcined ash catalyst

		•
Element	Weight%	Atomic%
Carbon	5.134	8.557
Oxygen	49.784	62.291
Magnesium	2.701	2.224
Aluminium	2.817	2.090
Silicon	23.508	16.755
Phosphorus	1.910	1.234
Sulphur	0.334	0.209
Chlorine	0.502	0.284
Potassium	5.371	2.750
Calcium	5.399	2.696
Iron	2.540	0.911

Table 4.2: Summary result for ash catalyst for EDX analysis.

Table 4.2 indicates that the calcined ash catalyst has minerals like Mg, Si, Al, Fe, K and Ca that typically use as a catalyst. The calcined ash catalyst has high

composition of oxygen (62%). This amount might be attributed by the oxygen content in metal oxide. Silicon also gives a high weight percent compare to other element. Carlson & Adriano, (1993) also reported the same observation.

4.4 Catalyst testing

In this study, the effect of real plastics waste is to determine using the calcined ash catalyst. The summarization of the yield% for each of the plastic waste is tabulated in table 4.3.

				Plastic Was	te	
Ту	pes	Plastic	Shampoo	Plastic		M:4
		Bag	Bottle	Wrapper	Polystyrene	Mixture
	Liquid	33.81	50.73	27.47	71.19	48.08
Yield	Solid	26.00	26.80	33.20	24.00	27.32
(%)	Gas	37.20	21.88	38.54	4.02	21.2
	Wax	2.99	0.59	0.79	0.79	3.4

Table 4.3: Yield% for individual plastic waste

From table 4.3, it is known that the yield for liquid is highest for polystyrene compare to other plastic which is 71.19%. This finding is almost similar to Williams & Slaney, (2007) work. They found out that about 71% liquid, 2% gas and 27% solid product was produced in plastic pyrolysis at 500 °C with 5°C min⁻¹ for one hour in a batch reactor.

The shampoo bottle produced about 50.73% liquid, 26.8% solid and 21.88% of gas. According to Sharma et al., (2014), the catalytic pyrolysis of plastic grocery bag (HDPE), yield about 74% liquid, 17% solid and 9% gas. The experiment was conducted in a batch reactor at 440 °C for two hours. Shampoo bottle mostly made of unsaturated hydrocarbon in which it is bonded with either double or triple bond. Thus, it is believed that the hydrocarbon chain is hard to break because of the high strength and density.

For plastic bag and plastic wrapper, more gas was achieved. About 37% and 38% of gas produced in plastic bag and plastic wrapper respectively. Meanwhile, higher liquid product for plastic bag (33%) than plastic wrapper (27%) was obtained. For mixture of plastic wastes, it generates about 48.08% of liquid fuel, 21.2% of gas and 27.31% of solid.

4.5 Gas product Analysis

The composition of the gas product is tabulated in table 4.4. It can be seen that in table 4.4 that the composition (mol%) of methane was observed to be the highest for plastic bag (4.18 mol %) and plastic wrapper (3.5 mol %).. For shampoo bottle, it only contained about 2.52 mol% of methane. The detailed gas analysis via GC-TCD is in appendix D.

Polystyrene generated a low amount of methane gas which is 0.49 mol%. Williams & Bagri, (2004) also reported that their research on catalytic pyrolysis of fuel of PS pellet give a low value of methane gas composition which is 0.1wt%.

 Table 4.4: Gas composition versus area (mol%)

	Plastic Waste				
	Diastia Dag	Shampoo	Plastic	Dolystypopo	Misstan
	Plastic Bag	Bottle	Wrapper	Polystyrene	Mixture
CH ₄ (mol%)	4.18	2.52	3.50	0.49	Nil

4.6 Liquid product analysis

4.6.1 Liquid composition

The detailed GC-MS result is in appendix E and the summarized result is tabulated in table 4.4.

				Area %		
Hydrocarbon group				Plastic Was	te	
		Plastic	Shampoo	Plastic	Dolystyrono	Mixturo
		Bag	Bottle	Wrapper	Polystyrene	Mixture
	C5-C6	-	5.75	2.34	0.34	1.25
	C7-C9	7.81	4.52	9.02	-	18.18
	C ₁₀ -C ₁₂	22.88	11.26	19.82	-	13.91
	C ₁₃ -C ₁₅	27.02	24.04	23.34	-	12.57
Alimbotio	C ₁₆ -C ₁₈	17.87	19.04	18.77	-	14.91
Aliphatic	C ₁₉ -C ₂₁	14.96	27.22	17.16	-	15.73
	C_{22} - C_{24}	1.18	3.77	-	-	1.03
	C ₂₅ -C ₂₇	-	-	-	-	-
	C_{28} - C_{30}	-	-	-	-	-
	> C ₃₀	-	-	-	3.22	-
	benzene	_	_	_	_	0.52
	toluene	_	_	-	4.9	0.97
	ethyl-				1.9	0.97
	benzene	0.51	-	-	10.4	5.45
	styrene	-	-	1.31	29.88	4.01
Aromatic	xylenes	-	-	-	-	-
	isopropyl				20.01	2.22
	benzene	-	-	-	28.01	3.23
	alpha-methyl	-	_	-	5.5	0.99
	styrene					
	$> C_{10}$	-	-	-	12.63	1.38

Table 4.5: GCMS analysis summarize result

From table 4.4, the result shows that plastic bag fuel is rich in $C_{13} - C_{15}$ same goes with the plastic wrapper. For shampoo bottle, $C_{19} - C_{21}$ play a larger number in the liquid properties. For the polystyrene plastic fuel, styrene and isopropyl benzene seems to be the major component in the fuel since polystyrene is made from styrene. According to Pinto et al., (1999), their research resulted in high aromatic composition in polystyrene and more alkanes rather than alkenes in polyethylene composition which supported our finding. For mixture of plastic wastes, it shows a mixture of both aliphatic and aromatic compound exist in the fuel.

4.6.2 Calorific value

The result for the calorific value test for each of the plastic sample is tabulated in table 4.5.

			Plasti	c Waste		
	Plastic	Shampoo	Plastic	Polystyrene	Mixture	RON 95
	Bag	Bottle	Wrapper			
RON	4209.31	3239.28	3003.53	2885.36	3355.02	3103.59

Table 4.6: Calorific value summarization for various plastic waste

From table 4.5, the result shows that plastic bag calorific value is the highest among all others plastic which is 4209.31 cal.g⁻¹. Polystyrene produced the lowest calorific value (2885.36 cal.g⁻¹). When comparing the calorific value with a commercial product which is RON 95, the closest calorific value is plastic wrapper and shampoo bottle which is 3239.28 cal.g⁻¹ and 3003.53 cal.g⁻¹.

4.6.3 Octane number

The result from the octane analysis were tabulated in table 4.6

			Plasti	c Waste		
	Plastic	Shampoo	Plastic	Dolystypopo	Misturo	RON
	Bag	Bottle	Wrapper	Polystyrene	wiixture	95
RON	89	100	84.1	98.7	93.2	95.2

 Table 4.7: RON result

From table 4.6 the result shows that shampoo bottle has the highest RON number which is 100. The second highest RON number is polystyrene which is 98.7. Both of these RON numbers shows a higher RON number compare to the commercial product RON 95.

4.6.4 Density, viscosity, moisture, and clarity

The result for all the testing is summarized in table 4.8.

	Plastic Waste					
	Plastic	Shampoo	Plastic	Dolucturono	Mixture	RON 95
	Bag	Bottle	Wrapper	Polystyrene	MIXture	KUN 95
Density (g.ml ⁻¹)	0.76	0.78	0.78	0.91	0.79	0.72
Clarity (NTU)	2.68	3.46	3.21	5.67	8.67	2.48
Moisture%	2.97	2.35	2.88	2.45	2.64	4.15
Viscosity (cP)	2.244	0.6725	0.828	0.9355	1.281	0.6

Table 4.8: Summary of liquid fuel properties

Beside polystyrene and plastic mixture fuel, fuel from other plastic, namely plastic bag, shampoo bottle and plastic wrapper, have a density in a range of 0.76 - 0.78 g.ml⁻¹. The fuel is rich in aliphatic hydrocarbon (Table 4.4). The fuel consists of long chain hydrocarbon without any benzene ring that make the hydrocarbon less dense.

For polystyrene plastic waste fuel, the density is the highest among all of the plastic waste fuel. This result is related from subchapter 4.5 result. In the polystyrene fuel composition, there were approximately 12% of hydrocarbon $>C_{10}$, also known as polycyclic aromatic. Polycyclic aromatic hydrocarbons are composed of two or more aromatic rings which are fused together when a pair of carbon atoms is shared between them. The density of the polycyclic aromatic is heavier compare to normal aromatic compound. According to Pinto et al., (1999), the density of plastic fuel varies with the

increase of temperature. They reported that the polystyrene fuel has boiling point in a range of <100 °C to <270 °C with a density of $0.7 - 0.85 \text{ kg}^3 \text{.m}^{-3}$.

The highest viscosity value among all the plastics waste fuel is the plastic bag fuel which is 2.244 cP. For shampoo bottle, the viscosity of the fuel is quite low which his 0.6725 cP. It is believed that double bonds can reduce the kinematic viscosity of the liquid fuel. Another factor contributes in reducing the kinematic viscosity is the position of the double bond in the hydrocarbon. However, the position of the double bond is not a major factor that effect the kinematic viscosity. An additional double bond also plays a role where it helps decrease the kinematic viscosity of the fuel but it does not decrease the viscosity to the extent the introduction of the first double does (Kaufmann and Funke, 1938). The viscosity result for polystyrene also give a low value of the viscosity because due to their lack of oxygen or other heteroatoms (Knothe and Steidley, 2005).

The moisture content in the liquid fuel is in the range of 2.35 - 2.97% which is a quite low in percentage. Moisture in liquid fuel lowers the heating value and flame temperature, but on the other hand, water reduces the viscosity and enhances the fluidity, which is good for the atomization and combustion of bio-oil in the engine (Zhang et al., 2007).

Figure 4.6 clearly illustrates the clarity of the fuel that derived from various plastic type. It can be seen that the plastic bag waste fuel gives the lowest NTU number which mean the fuel is clear and translucent to be seen. This is because most of the composition in liquid fuel is between $C_{10} - C_{15}$ for the plastic bag same goes with plastic wrapper.

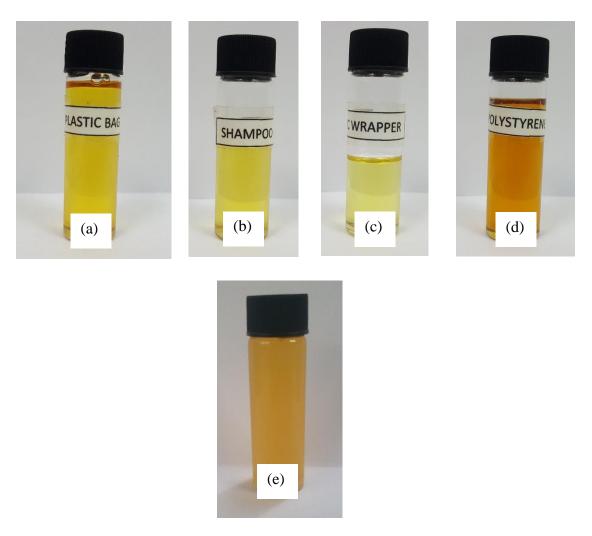


Figure 4.5: Plastic fuel (a) Plastic bag, (b) Shampoo bottle. (c) Plastic wrapper, (d) Polystyrene, (e) mixture of plastic waste

CHAPTER 5

CONCLUSION AND RECOMMENDATION

5.1 Conclusion

The catalyst that derived from oil palm biomass ash is a mesoporous structure with pore size of 31.69 nm. It is also rich in Silica (23.5 %) and other minerals like Mg, Si, Al, Fe, K and Ca.

Pyrolysis of real plastic waste produced gas, wax, condensed liquid hydrocarbons and solid. The best liquid product can be obtained from Polystyrene > Shampoo Bottle > Plastic Bag > Plastic Wrapper. Meanwhile, the mixture of plastic waste yields about 48% of liquid fuel. The best composition and characteristic of the liquid fuel is from shampoo bottle because it is rich in $C_{19} - C_{21}$ (27%) with 3239.28 cal.g⁻¹ calorific value and a low value of viscosity of 0.672 cP and a low value of moisture content which is 2.35%. The RON number of shampoo bottle fuel is 100 which is higher than the commercial product of RON 95. It is concluded that the liquid fuel derived from shampoo bottle is better and greener than a commercial product of RON 95 in term of calorific value, moisture, viscosity and RON number. The production cost is also low because the catalyst use is derived from waste itself.

5.2 Recommendation

For the recommendation for future work, there are actually other parameter can contribute to the quality of liquid fuel via pyrolysis of plastic waste such as retention time, pressure and type of reactor. For retention time, different plastic requires different retention time because some plastic has single, double or triple bond in the hydrocarbon chain that something need more time to crack the hydrocarbon chain into smaller one. For the reactor, it is suggested that the reactor is custom made so the upper lid can be open so that it can easily be clean for the next batch of experiment. The example of the reactor is shown in figure 5.1



Figure 5.1: Custom made 1 liter round bottom flask

REFERENCES

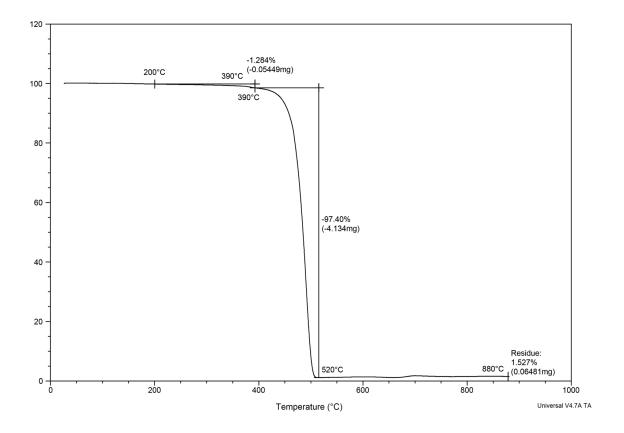
- Aboulkas, A., Makayssi, T., Bilali, L., Nadifiyine, M., & Benchanaa, M. (2012). Copyrolysis of oil shale and plastics: Influence of pyrolysis parameters on the product yields. *Fuel Processing Technology*, 96, 209-213.
- Aguado, J., Serrano, D. P., & Escola, J. M. (2006). Catalytic upgrading of plastic wastes. *Feedstock Recycling and Pyrolysis of Waste Plastics: Converting Waste Plastics into Diesel and Other Fuels*, 73-110.
- Ali, M. F., & Qureshi, M. S. (2011). Catalyzed pyrolysis of plastics: A thermogravimetric study. African Journal of Pure and Applied Chemistry, 5(9), 219-223.
- Arandes, J. M., Ereña, J., Azkoiti, M. J., Olazar, M., & Bilbao, J. (2003). Thermal recycling of polystyrene and polystyrene-butadiene dissolved in a light cycle oil. *Journal of analytical and applied pyrolysis*, 70(2), 747-760.
- Bagri, R., & Williams, P. T. (2002). Fluidised-bed catalytic pyrolysis of polystyrene. *Journal of the Institute of Energy*, 75(505), 117-123.
- Barrer, R.M. (1985). Synthesis of zeolite, Portoroz, Yugosl: Elsevier.
- Benito, P. L., Gayubo, A. G., Aguayo, A. T., Olazar, M., & Bilbao, J. (1996). Effect of Si/Al ratio and of acidity of H-ZSM5 zeolites on the primary products of methanol to gasoline conversion. *Journal of Chemical Technology and Biotechnology*, 66(2), 183-191.
- Buekens, A. (2006). Introduction to feedstock recycling of plastics. *Feedstock recycling and pyrolysis of waste plastics*, 1-41.
- Chanda, M. (2000). Advanced polymer chemistry: a problem solving guide. Marcel Dekker.
- Foster, A. J., Jae, J., Cheng, Y. T., Huber, G. W., & Lobo, R. F. (2012). Optimizing the aromatic yield and distribution from catalytic fast pyrolysis of biomass over ZSM-5. *Applied Catalysis A: General*, 423, 154-161.
- Hernández, M. D. R., García, Á. N., Gómez, A., Agulló, J., & Marcilla, A. (2006). Effect of residence time on volatile products obtained in the HDPE pyrolysis in the presence and absence of HZSM-5. *Industrial & engineering chemistry research*, 45(26), 8770-8778.

- Johari, A., Alkali, H., Hashim, H., Ahmed, S. I., & Mat, R. (2014). Municipal solid waste management and potential revenue from recycling in Malaysia. *Modern Applied Science*, 8(4), 37.
- Johari, M. M., Zeyad, A. M., Bunnori, N. M., & Ariffin, K. S. (2012). Engineering and transport properties of high-strength green concrete containing high volume of ultrafine palm oil fuel ash. *Construction and Building Materials*, 30, 281-288.
- Jung, C. G., & Fontana, A. (2006). Production of Gaseous and Liquid Fuels by Pyrolysis and Gasification of Plastics: Technological Approach.*Feedstock Recycling and Pyrolysis of Waste Plastics: Converting Waste Plastics into Diesel and Other Fuels*, 249-283.
- Karaduman, A., Şimşek, E. H., Cicek, B., & Bilgesü, A. Y. (2001). Flash pyrolysis of polystyrene wastes in a free-fall reactor under vacuum. *Journal of Analytical* and Applied Pyrolysis, 60(2), 179-186.
- Kaufmann, H. P., & Funke, S. (1938). The field of fats. LIX. The viscometry of fats (Zur Viskometrie der Fette (Studien auf dem Fettgebiet, 59. Mitteilung.)). Fette u Seifen, 45(5), 255-62.
- Knothe, G., & Steidley, K. R. (2005). Kinematic viscosity of biodiesel fuel components and related compounds. Influence of compound structure and comparison to petrodiesel fuel components. *Fuel*, 84(9), 1059-1065.
- Kumar, S., & Singh, R. K. (2011). Recovery of hydrocarbon liquid from waste high density polyethylene by thermal pyrolysis. *Brazilian Journal of Chemical Engineering*, 28(4), 659-667.
- Lee, K. H. (2006). Thermal and catalytic degradation of waste HDPE.Feedstock Recycling and Pyrolysis of Waste Plastics: Converting Waste Plastics into Diesel and Other Fuels, 129-160.
- Li, S. Q., Yao, Q., Chi, Y., Yan, J. H., & Cen, K. F. (2004). Pilot-scale pyrolysis of scrap tires in a continuous rotary kiln reactor. *Industrial & engineering chemistry research*, 43(17), 5133-5145.
- López, A., De Marco, I., Caballero, B. M., Laresgoiti, M. F., & Adrados, A. (2011). Influence of time and temperature on pyrolysis of plastic wastes in a semi-batch reactor. *Chemical Engineering Journal*, 173(1), 62-71.
- Maesen, T. (2007). THE ZEOLITE SCENE–ANOVERVIEW. Introduction to Zeolite Molecular Sieves, 168, 1.

- Masuda, T., & Tago, T. (2006). Development of a process for the continuous conversion of waste plastics mixtures to fuel. *Feedstock Recycling and Pyrolysis* of Waste Plastics: Converting Waste Plastics into Diesel and Other Fuels, 161-192.
- McMurry, J. (2000). Organic chemistry. 5th. Edition, RR Donnelly & Sons Willard, Ohio.
- Miller, S. J., Shah, N., & Huffman, G. P. (2005). Conversion of waste plastic to lubricating base oil. *Energy & fuels*, 19(4), 1580-1586.
- Miranda, R., Yang, J., Roy, C., & Vasile, C. (2001). Vacuum pyrolysis of commingled plastics containing PVC I. Kinetic study. *Polymer Degradation and stability*, 72(3), 469-491.
- Murata, K., Sato, K., & Sakata, Y. (2004). Effect of pressure on thermal degradation of polyethylene. *Journal of analytical and applied pyrolysis*,71(2), 569-589.
- Onwudili, J. A., Insura, N., & Williams, P. T. (2009). Composition of products from the pyrolysis of polyethylene and polystyrene in a closed batch reactor: Effects of temperature and residence time. *Journal of Analytical and Applied Pyrolysis*, 86(2), 293-303.
- Park, K. H., Park, H. J., Kim, J., Ryoo, R., Jeon, J. K., Park, J., & Park, Y. K. (2010). Application of hierarchical MFI zeolite for the catalytic pyrolysis of Japanese larch. *Journal of nanoscience and nanotechnology*, 10(1), 355-359.
- Phan, X.K., Yang, J., Bakhtiary-Davijnay, H. (2011), Studies of Macroporous Structured Alumina Based Cobalt Catalysts for Fischer–Tropsch Synthesis. *Catalysis Letter* 141: 1739. doi:10.1007/s10562-011-0702-3
- Pinto, F., Costa, P., Gulyurtlu, I., & Cabrita, I. (1999). Pyrolysis of plastic wastes. 1. Effect of plastic waste composition on product yield. *Journal of Analytical and Applied Pyrolysis*, 51(1), 39-55.
- Rhee, Y., Guin, J.A, Curtis, C.W, (1989). Effects of Pore Structure on Initial Catalytic Activity for Residuum Desulfurization and Coal Liquefaction. *Energy & Fuels* ,3, 391-397
- Sharma, B. K., Moser, B. R., Vermillion, K. E., Doll, K. M., & Rajagopalan, N. (2014). Production, characterization and fuel properties of alternative diesel fuel from pyrolysis of waste plastic grocery bags. *Fuel Processing Technology*, 122, 79-90.

- Syamsiro, M., Saptoadi, H., Norsujianto, T., Noviasri, P., Cheng, S., Alimuddin, Z., & Yoshikawa, K. (2014). Fuel oil production from municipal plastic wastes in sequential pyrolysis and catalytic reforming reactors. *Energy Procedia*, 47, 180-188.
- Williams, E. A., & Williams, P. T. (1997). Analysis of products derived from the fast pyrolysis of plastic waste. *Journal of Analytical and Applied Pyrolysis*, 40, 347-363.
- Williams, P. T., & Bagri, R. (2004). Hydrocarbon gases and oils from the recycling of polystyrene waste by catalytic pyrolysis. *International Journal of Energy Research*, 28(1), 31-44.
- Williams, P. T., & Slaney, E. (2007). Analysis of products from the pyrolysis and liquefaction of single plastics and waste plastic mixtures. *Resources, Conservation and Recycling*, 51(4), 754-769.
- Williams, P. T., & Williams, E. A. (1998). Recycling plastic waste by pyrolysis. *Journal of the Institute of Energy*, 71(487), 81-93.
- Zadgaonkar, A. (2006). Process and equipment for conversions of waste plastics into fuels. Feedstock Recycling and Pyrolysis of Waste Plastics: Converting Waste Plastics into Diesel and Other Fuels, 709-728.
- Zarina, Y., Mohd Mustafa Al Bakri, A., Kamarudin, H., Nizar, K., & Rafiza, A. R. (2013). Review on the various ash from palm oil waste as geopolymer material.
- Zhang, Q., Chang, J., Wang, T., & Xu, Y. (2007). Review of biomass pyrolysis oil properties and upgrading research. *Energy conversion and management*, 48(1), 87-92.

Sample: HDPE Size: 4.2450 mg Method: Ramp

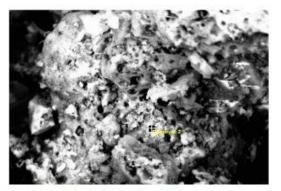


Spectrum details

Project: New project

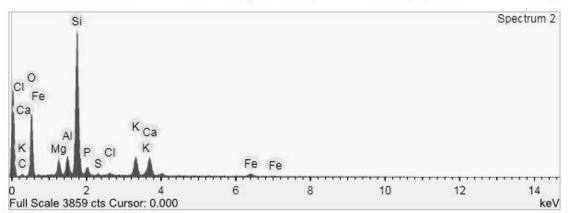
Spectrum name: Spectrum 2

Electron Image Image Width: 58.6 µm



Quantification Settings Quantification method : All Coating element : All elements (normalised)

None



APPENDIX C – BET ANALYSIS

Full Report Set

Sample: 4 Operator: HALIM Submitter: UMP File: C:\2020\DATA\001-711.SMP

Started:	11/9/2016 2:18:16PM
Analysis Adsorptive:	N2
Completed:	11/9/2016 5:24:03PM
Analysis Bath Temp.:	-195.793 °C
Report Time:	11/11/2016 8:23:27AM
Thermal Correction:	No
Sample Mass:	0.3110 g
Warm Free Space:	27.2363 cm ³ Measured
Cold Free Space:	84.1917 cm³
Equilibration Interval:	5 s
Low Pressure Dose:	None
Automatic Degas:	Yes

Summary Report

Surface Area

- Single point surface area at P/Po = 0.300121346: $1.3232 \text{ m}^2/\text{g}$
 - BET Surface Area: 1.3736 m²/g
 - Langmuir Surface Area: 2.1490 m²/g
 - t-Plot Micropore Area: 0.0467 m²/g
 - t-Plot External Surface Area: 1.3269 m²/g
- BJH Adsorption cumulative surface area of pores between 17.000 Å and 3000.000 Å diameter: 0.695 m²/g
- BJH Desorption cumulative surface area of pores between 17.000 Å and 3000.000 Å diameter: 0.7775 m²/g

Pore Volume

Single point adsorption total pore volume of pores less than 1279.335 Å diameter at P/Po = 0.984634127: 0.002254 cm³/g

Single point desorption total pore volume of pores less than 795.043 Å diameter at P/Po = 0.975033947: 0.002746 cm³/g

t-Plot micropore volume: 0.000059 cm³/g

BJH Adsorption cumulative volume of pores between 17.000 Å and 3000.000 Å diameter: 0.005506 cm³/g BJH Desorption cumulative volume of pores between 17.000 Å and 3000.000 Å diameter: 0.005619 cm³/g

Pore Size

Adsorption average pore width (4V/A by BET):	65.6422 Å
Desorption average pore width (4V/A by BET):	79.9752 Å
BJH Adsorption average pore diameter (4V/A):	316.962 Å
BJH Desorption average pore diameter (4V/A):	289.076 Å

Isotherm Tabular Report

Relative Pressure (P/Po)	Absolute Pressure (mmHg)	Quantity Adsorbed (mmol/g)	Elapsed Time (h:min)	Saturation Pressure (mmHg)
(P/Po) 1.#QNAN0000 0.011172672 0.034528383 0.068950458 0.080130254 0.100145332 0.120095809 0.140166149 0.160141527 0.180131203 0.200069901 0.250037142 0.300121346 0.350119407 0.419357297 0.469322471 0.519263245	(mmHg) 1. #QNAN0 8.496140 26.256741 52.432640 60.934196 76.154449 91.325577 106.587852 121.777916 136.978851 152.141022 190.138077 228.224075 266.244568 318.895782 356.891266 394.868195	(mmol/g) 1.#QNAN 0.01026 0.01222 0.01448 0.01500 0.01560 0.01655 0.01695 0.01763 0.01803 0.01803 0.01861 0.01938 0.01938 0.01928 0.01845 0.01768 0.01642	<pre>(h:min) 01:06 01:16 01:18 01:19 01:20 01:22 01:23 01:24 01:26 01:27 01:28 01:30 01:31 01:32 01:34 01:36 01:37</pre>	(mmHg) 760.439331 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0
0.569183271 0.619145475 0.669087854 0.719038260 0.758952096 0.788958505 0.818861777 0.838850479 0.840011404 0.860068490 0.893718199 0.904980946	432.829346 470.822571 508.800720 546.784973 577.137024 599.955078 622.694702 637.894897 638.777710 654.029907 679.618469 688.183105	0.01545 0.01392 0.01262 0.01193 0.01139 0.01096 0.01091 0.01118 0.01156 0.01191 0.01341 0.01562	01:39 01:40 01:41 01:43 01:45 01:45 01:46 01:47 01:49 01:50 01:51 01:53 01:54	1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0 1.#QNAN0

Isotherm Linear Plot

 4 - Adsorption

 Relative Pressure (P/Po)
 Quantity Adsorbed (mmol/g)

 0.0111727
 0.0102609

 0.0345284
 0.0122246

 0.0689505
 0.0144788

0.20007 0.250037 0.300121 0.350119 0.419357 0.469322 0.519263 0.569183 0.619145 0.669088 0.719038 0.758952 0.788959 0.818862 0.83885 0.840011 0.860068 0.893718 0.904981 0.914976 0.925223 0.951287 0.953132 0.959306 0.981548 0.984634 0.999117	0.0149983 0.015605 0.0165542 0.0169488 0.0176348 0.0180306 0.0186137 0.0193762 0.0193762 0.0192765 0.0184461 0.0176808 0.0164204 0.0154504 0.0154504 0.0126172 0.0119327 0.0119327 0.0119327 0.0109591 0.0109591 0.0109591 0.0109591 0.0109591 0.0119107 0.0134147 0.0134147 0.015618 0.0193664 0.0214216 0.0286136 0.0300617 0.0326748 0.0545608 0.0597996 0.065018 0.167253
4 - Desorption	

4 - Desor	ption				
Relative	Pressure	(P/Po)	Quantity	Adsorbed	(mmol/g)
0.999117		0.167253			
0.975034		0.0792147			
0.956975		0.0491755			
0.93519		0.0336485			
0.914743		0.0268084			
0.88661		0.0223328			
0.856419		0.0193964			
0.82137		0.0178298			
0.801297		0.0170944			
0.781199		0.016748			
0.751231		0.0167407			
0.721243		0.0167603			
0.680713		0.0171732			
0.63111		0.0178527			
0.580996		0.0184597			
0.53098		0.0191309			
0.481123		0.0175922			
0.430725		0.016312			
0.380585		0.0160822			
0.330623		0.0157421			

0.28061	0.0152623
0.230592	0.0139363
0.180636	0.0124753
0.122836	0.00932328

Isotherm Log Plot

0.8937180.01341470.9049810.0156180.9149760.01936640.9252230.02142160.9512870.02861360.9531320.03006170.9593060.03267480.9815480.0545608	0.0102609 0.0122246 0.0144788 0.0149983 0.015605 0.0165542 0.0165542 0.0169488 0.0176348 0.0180306 0.0186137 0.0193762 0.0193762 0.0193762 0.0192765 0.0184461 0.0176808 0.0164204 0.0154504 0.0154504 0.0126172 0.0126172 0.0119327 0.0129391 0.0109591 0.0109591 0.0109591 0.0109591 0.0109591 0.0111846 0.0115551 0.0119107 0.0134147 0.015618 0.0193664 0.0214216 0.0300617 0.0326748	0.904981 0.914976 0.925223 0.951287 0.953132 0.959306	R0000000000000000000000000000000000000	
0.953132 0.0300617 0.959306 0.0326748	0.0300617 0.0326748 0.0545608 0.0597996 0.065018	0.953132 0.959306 0.981548 0.98243 0.984634	0 0 0 0	

(P/Po)	Quantity	Adsorbed	(mmol/g)
0.167253			
0.0792147			
0.0491755			
0.0336485			
0.0268084			
0.0223328			
	0.167253 0.0792147 0.0491755 0.0336485 0.0268084	0.167253 0.0792147 0.0491755 0.0336485 0.0268084	0.167253 0.0792147 0.0491755 0.0336485 0.0268084

0.856419	0.0193964
0.82137	0.0178298
0.801297	0.0170944
0.781199	0.016748
0.751231	0.0167407
0.721243	0.0167603
0.680713	0.0171732
0.63111	0.0178527
0.580996	0.0184597
0.53098	0.0191309
0.481123	0.0175922
0.430725	0.016312
0.380585	0.0160822
0.330623	0.0157421
0.28061	0.0152623
0.230592	0.0139363
0.180636	0.0124753
0.122836	0.00932328

BET Surface Area Report

BET Surface Area:	$1.3736 \pm 0.0450 \text{ m}^2/\text{g}$
Slope:	71.263358 ± 2.293554 g/mmol
Y-Intercept:	-0.229769 ± 0.401199 g/mmol
С:	-309.152797
Qm:	0.01408 mmol/g
Correlation Coefficient:	0.9958823
Molecular Cross-Sectional Area:	0.1620 nm ²

Relative Pressure (P/Po)	Quantity Adsorbed (mmol/g)	1/[Q(Po/P - 1)]
0.068950458	0.01448	5.11483
0.080130254	0.01500	5.80804
0.100145332	0.01560	7.13174
0.120095809	0.01655	8.24490
0.140166149	0.01695	9.61813
0.160141527	0.01763	10.81251
0.180131203	0.01803	12.18526
0.200069901	0.01861	13.43683
0.250037142	0.01934	17.23949
0.300121346	0.01938	22.13120

BET Surface Area Plot

4		
Relative Pressure	(P/Po)	1/[Q(Po/P - 1)]
0.0689505	5.11483	
0.0801303	5.80804	
0.100145	7.13174	
0.120096	8.2449	

0.140166	9.61813
0.160142	10.8125
0.180131	12.1853
0.20007	13.4368
0.250037	17.2395
0.300121	22.1312

Langmuir Surface Area Report

Langmuir Surface Area	
Slope	e: 45.403853 ± 0.532055 g/mmol
Y-Intercept	1341.362402 ± 70.773593
mmHg·g/mmol	
k	o: 0.033849 1/mmHg
Qn	n: 0.02202 mmol/g
Correlation Coefficient	0.999451
Molecular Cross-Sectional Area	1: 0.1620 nm ²

Pressure (mmHg)	Quantity Adsorbed (mmol/g)	P/Q (mmHg·g/mmol)
52.432640	0.01448	3621.33
60.934196	0.01500	4062.75
76.154449	0.01560	4880.14
91.325577	0.01655	5516.78
106.587852	0.01695	6288.83
121.777916	0.01763	6905.53
136.978851	0.01803	7597.03
152.141022	0.01861	8173.60
190.138077	0.01934	9831.70
228.224075	0.01938	11778.56

t-Plot Report

Micropore Volume:	0.000059 cm³/g
Micropore Area:	0.0467 m²/g
External Surface Area:	1.3269 m²/g
Slope:	0.003827 ± 0.000218 mmol/g·Å
Y-Intercept:	0.001714 ± 0.000886 mmol/g
Correlation Coefficient:	0.990407
Surface Area Correction Factor:	1.000
Density Conversion Factor:	0.0015468
Total Surface Area (BET):	1.3736 m²/g
Thickness Range:	3.5000 Å to 5.0000 Å
Thickness Equation:	Harkins and Jura

t = $[13.99 / (0.034 - \log(P/Po))]^{0.5}$

Relative	Statistical	Quantity
Pressure	Thickness	Adsorbed
(P/Po)	(Å)	(mmol/g)

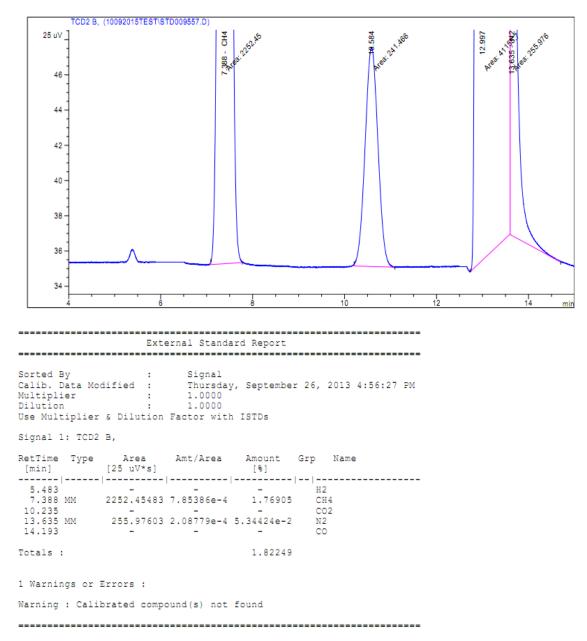
0.011172672	2.6542	0.01026
0.034528383	3.0582	0.01222
0.068950458	3.4209	0.01448
0.080130254	3.5183	0.01500
0.100145332	3.6794	0.01560
0.120095809	3.8285	0.01655
0.140166149	3.9706	0.01695
0.160141527	4.1068	0.01763
0.180131203	4.2394	0.01803
0.200069901	4.3693	0.01861
0.250037142	4.6901	0.01934
0.300121346	5.0130	0.01938
0.350119407	5.3445	0.01928
0.419357297	5.8313	0.01845
0.469322471	6.2121	0.01768
0.519263245	6.6264	0.01642
0.569183271	7.0844	0.01545
0.619145475	7.6000	0.01392

APPENDIX D – GAS ANALYSIS VIA GC-TCD

Plastic Wrapper

Data File C:\CHEM32\1\DATA\10092015TEST\STD009557.D Sample Name: DR RUZINAH

	-			-	
Acq. Operator	:	SUNNY			
Acq. Instrument	:	Instrument 1	Location	:	Vial 2
Injection Date	:	2/18/2016 12:52:35 PM	Inj		
			Inj Volume	:	Manually
Method	:	C:\CHEM32\1\METHODS\GC 1	20 OK.M		
Last changed	:	4/5/2015 6:06:16 PM by a	gilent		
Sample Info	:	PLASTIC KUIH+CALCINED AS	H_1:10		



Plastic Bag

Data File C:\CHEM32\1\DATA\10092015TEST\STD009415.D Sample Name: Real Plastic (Colorless) + Calcined Ash Acq. Operator : SUNNY Acq. Instrument : Instrument 1 Location : Vial 2 Injection Date : 2/12/2016 9:24:36 AM Inj : 1 Acq. Method : C:\CHEM32\1\METHODS\GC_120_OK.M Last changed : 2/11/2016 3:38:58 FM by SUNNY (modified after loading) Analysis Method : C:\CHEM32\1\METHODS\GC 120 OK.M

 External Standard Report

 Sorted By
 :
 Signal

 Calib. Data Modified
 :
 Thursday, September 26, 2013 4:56:27 PM

 Multiplier
 :
 1.0000

 Dilution
 :
 1.0000

 Use Multiplier & Dilution Factor with ISTDe
 Signal 1: TCD2 B,

 RetTime Type
 Area
 Amt/Area
 Amount Grp Name

 [min]
 [25 uV*s]
 [%]

 5.483
 H2

 7.427 MM
 27.39453 7.85386e-4 2.15153e-2
 CH4

 10.235
 CO2

 13.660 MM
 1280.68579 2.08779e-4 2.67380e-1
 N2

 14.193
 CO

 Totals :
 2.88895e-1

Shampoo Bottle

```
      External Standard Report

      Sorted By
      :
      Signal

      Calib. Data Modified
      :
      Thursday, September 26, 2013 4:56:27 PM

      Multiplier
      :
      1.0000

      Dilution
      :
      1.0000

      Use Multiplier & Dilution Factor with ISTDs

      Signal 1: TCD2 B,

      RetTime Type
      Area

      Amt/Area
      Amount

      Grp
      Name

      [min]
      [25 uV*s]

      -
      -

      5.483
      -

      -
      -

      7.408 MM
      1620.43433 7.65386e-4

      1.27267
      CH4

      10.235
      -

      -
      -

      13.666 MM
      1410.16699 2.08779e-4 2.94413e-1

      14.193
      -

      -
      -

      Totals :
      1.56708
```

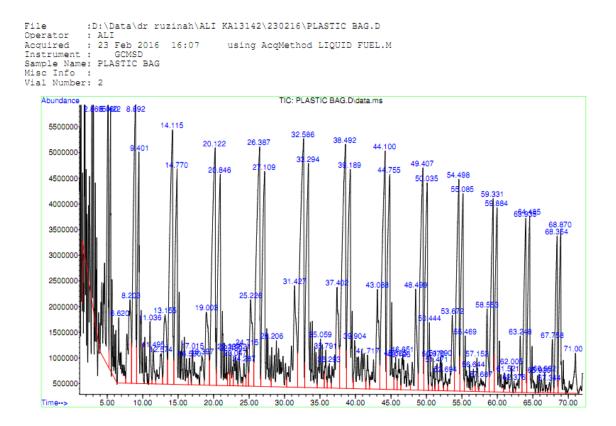
Polystyrene

ata FILE C:\CHEM32\I\DATA\IU0920ISTEST\STD009558.D Sample Name: DR RUZINAH Acq. Operator : SUNNY Acq. Instrument : Instrument 1 Location : Vial 2 Injection Date : 2/18/2016 1:34:43 PM Inj : 1 Inj Volume : Manually Method : C:\CHEM32\I\METHODS\GC_120_OK.M Last changed : 4/5/2015 6:06:16 PM by acilent

	Exte	ernal Standa	ara keport	
Multiplier	iified : : :	1.0000	-	r 26, 2013 4:56:27 PM
Signal 1: TCD2	в,			
RetTime Type [min]	Area [25 uV*s]	Amt/Area	Amount [%]	Grp Name
5.483 7.402 MM 10.235 13.358 14.193	316.99313	7.85386e-4	2.48962e-1	H2 CH4 CO2 N2 CO
Totals :			2.48962e-1	

APPENDIX E – GC-MS ANALYSIS

Plastic Bag



?k∦	RT	Area%	Library/ID	Ref∦	CAS #	Qual
1	2.871	C : 1-	C:\Database\NIST05a.L is-1-Butyl-2-methylcyclopropane -Octene -Octene	6442	038851-69-3 000111-66-0 000111-66-0	90
2	5.061	$\frac{C_{2}}{1}$	C:\Database\NIST05a.L yclopropane, 1-methyl-2-pentyl- -Nonene -Nonene	11145	041977-37-1 000124-11-8 000124-11-8	93
3	5.424	No No	C:\Database\NIST05a.L onane onane onane	12268	000111-84-2 000111-84-2 000111-84-2	94
4	6.620	C) C)	C:\Database\NIST05a.L yclopentene, 1-butyl- yclohexene, 3,3,5-trimethyl- yclopentene,1-(2-methylpropyl)-	10361	002423-01-0 000503-45-7 053098-47-8	59
5	8.201	$\frac{1}{1}$	C:\Database\NIST05a.L ,11-Dodecadiene ,11-Dodecadiene ,13-Tetradecadiene	33506	005876-87-9 005876-87-9 021964-49-8	58
6	8.895	1 · 1 ·	C:\Database\NIST05a.L -Decene -Decene yclooctane, 1,2-dimethyl-	17321	000872-05-9 000872-05-9 013151-94-5	97
7	9.397	D	C:\Database\NIST05a.L ecane ecane ecane	18487	000124-18-5 000124-18-5 000124-18-5	95
8	11.032	C	C:\Database\NIST05a.L yclohexene, 1-butyl- aphthalene, decahydro- enzylamine	16321	003282-53-9 000091-17-8 000100-46-9	43
9	11.491	C) C) tl Sj	C:\Database\NIST05a.L yclohexene, 1-butyl- yclohexane, 1-methyl-4-(1-methyle henyl)-, cis- piro[2.5]octane-1,1-dicarbonitril , 4-methyl-	16436	003282-53-9 001879-07-8 1000151-43-	52
10	12.570	c: 3	C:\Database\NIST05a.L is-Decalin, 2-syn-methyl- ,4-Octadiene, 7-methyl- aphthalene, decahydro-2-methyl-	10330	1000155-85- 037050-05-8 002958-76-1	68
11	13.157	C: 5-	C:\Database\NIST05a.L is-9-Tetradecen-1-ol -Undecyne yclodecene	24365	035153-15-2 002294-72-6 003618-12-0	49
12	14.119		C:\Database\NIST05a.L -Undecene	25902	000821-95-4	95

₽k∦	RT	Area%	Library/ID	Ref∦	CAS# (Qual
			-Undecene -Undecene, (Z)-		000821-95-4 000821-97-6	
13	14.770	U. U	C:\Database\NIST05a.L ndecane ndecane ndecane ndecane	27238	001120-21-4 001120-21-4 001120-21-4	94
14	16.586	3 3	C:\Database\NIST05a.L ,4-Octadiene, 7-methyl- ,4-Octadiene, 7-methyl- yclohexene, 1,2-dimethyl-	10322	037050-05-8 037050-05-8 001674-10-8	60
15	17.014	2 t	C:\Database\NIST05a.L -Decalone,c&t rans-Decalin, 2-methyl- yclohexene, 1-pentyl-	24396	004832-17-1 1000152-47-3 015232-85-6	3 55
16	18.402	B ti 5	C:\Database\NIST05a.L icyclo[3.1.1]heptane, 2,6,6-trime hyl- -Undecyne -Methyloctahydrocoumarin	24356	000473-55-2 002294-72-6 080648-29-9	55
17	19.000	1.05 1 C	C:\Database\NIST05a.L ,11-Dodecadiene yclododecene ,11-Dodecadiene	33497	005876-87-9 001501-82-2 005876-87-9	93
18	20.122	1	C:\Database\NIST05a.L -Dodecene -Dodecene yclododecane	34944	000112-41-4 000112-41-4 000294-62-2	96
19	20.848	D	C:\Database\NIST05a.L odecane odecane odecane	36430	000112-40-3 000112-40-3 000112-40-3	94
20	22.141	C C	C:\Database\NIST05a.L yclohexane, hexyl- yclohexane, (4-methylpentyl)- yclohexane, hexyl-	35057	004292-75-5 061142-20-9 004292-75-5	64
21	22.429	C) 1 6	C:\Database\NIST05a.L yclopropane, 1-butyl-2-pentyl-, t ans- -Dodecene, (E)-	34971	074663-87-9 007206-17-9	50
22	23.049	0.35 6 6	-Dodecene, (E)- C:\Database\NIST05a.L -Tridecene, (Z)- -Tridecene, (E)- -Tridecene, (E)-	44628 44627	007206-17-9 006508-77-6 006434-76-0 023051-84-5	76 72
23	23.626	9 C	C:\Database\NIST05a.L -Methylbicyclo[3.3.1]nonane ycloheptane, methyl- yclopentane, 1,2-dimethyl-3-(1-me	6507	025107-01-1 004126-78-7 000489-20-3	38

thylethyl)-

		engreengr) -			
24	24.288	0.16 C:\Database\NIST05a.L Bicyclo[2.2.1]heptane, 2,2,3-trime	16427	020536-40-7	83
		thyl-, endo- Bicyclo[2.2.1]heptane, 2,2,3-trime thyl-, exo-	16425	020536-41-8	46
		1-Methyl-2-methylenecyclohexane	5854	002808-75-5	44
25	24.715	0.27 C:\Database\NIST05a.L	110945	074685-31-7	~
		5-Eicosyne Cyclodecanol		001502-05-2	-
		1-Hexadecyne		001502-05-2	
		1-nexadecyne	13031	000629-14-3	49
26	25.228	1.17 C:\Database\NIST05a.L			
		1-Heptadecyne	82655	026186-00-5	90
		cis-9-Tetradecen-1-ol	65991	035153-15-2	90
		cis-9-Tetradecen-1-ol	65989	035153-15-2	86
	00.000				
27	26.392	3.88 C:\Database\NIST05a.L 1-Tridecene	4461.9	002437-56-1	99
		1-Tridecene		002437-56-1	
		1-Tridecene		002437-56-1	
		1 11 1000000			÷.,
28	27.108	3.09 C:\Database\NIST05a.L			
		Tridecane		000629-50-5	
		Tridecane		000629-50-5	
		Tridecane	46085	000629-50-5	95
29	28.208	1.22 C:\Database\NIST05a.L			
23	20.200	Bicyclo[3.1.1]heptane, 2,6,6-trime thyl-, [1R-(1.alpha.,2.beta.,5.alp	16447	004795-86-2	64
		ha.)]-			
		Bicyclo[3.1.1]heptane, 2,6,6-trime thyl-	16398	000473-55-2	49
		Cyclododecene	33497	001501-82-2	49
30	31.424	1.70 C:\Database\NIST05a.L			
	51.121	1,13-Tetradecadiene	52919	021964-49-8	91
		5-Nonadecen-1-ol		1000131-11-9	
		1,13-Tetradecadiene	52921	021964-49-8	83
31	32.588	4.27 C:\Database\NIST05a.L	54501	025052 52 0	00
		2-Tetradecene, (E)- 1-Tetradecene		035953-53-8 001120-36-1	
		1-Dodecene		000112-41-4	
		1 00000000	0.010		
32	33.293	3.43 C:\Database\NIST05a.L			
		Tetradecane		000629-59-4	
		Tetradecane		000629-59-4	
		Tetradecane	55972	000629-59-4	96
33	35.056	0.63 C:\Database\NIST05a.L			
55	55.050	Cyclotetradecane	54517	000295-17-0	91
		Cyclododecane		000294-62-2	
		Pentafluoropropionic acid, octadec			
		yl ester			
24	25 702	0.24 Gr) Database) NIGTOFA 1			

34 35.793 0.24 C:\Database\NIST05a.L

₽k⋕	RT	Area%	Library/ID	Ref#	CAS#	Qual
			yclohexene, 1-octyl-		015232-87-8	
			yclohexene,1-hexyl-		003964-66-7	
		C	yclohexene,1-hepty1-	43182	015232-86-7	1 72
35	36.295	0.22	C:\Database\NIST05a.L			
		1	-Dodecene	34944	000112-41-4	43
		C	yclooctane, 1,5-dimethyl-	17397	021328-57-4	38
			yclopropane, 1-butyl-2-pentyl-, c s-	35079	074663-88-0	38
36	37.406	1.48	C:\Database\NIST05a.L			
		1	-Pentadecyne	63039	000765-13-9	9 87
		1	,12-Tridecadiene	43179	021964-48-7	1 86
			,12-Tridecadiene		021964-48-7	
37	38.495	4.05	C:\Database\NIST05a.L			
		1	-Pentadecene	64454	013360-61-7	1 97
		1	-Pentadecene	64457	013360-61-7	1 95
			-Pentadecene		013360-61-7	
38	39.189	3.00	C:\Database\NIST05a.L			
50	55.105		ent adecane	66066	000629-62-9	97
			entadecane		000629-62-9	
			leptadecane		000629-78-7	
			leptadecalle	05524	000029-78-7	51
39	39.905		C:\Database\NIST05a.L			
			yclopentadecane		000295-48-7	
			,12-Tridecadiene		021964-48-7	
		1	-Docosene	129889	001599-67-3	3 46
40	41.721	0.27	C:\Database\NIST05a.L			
		C	Cyclohexene, 1-nonyl-	63043	015232-88-9	9 70
		Е	Bicyclo[3.1.0]hexan-2-one, 5-(1-me	17044	000513-20-2	2 62
			hylethyl)-			
			H-Indene, octahydro-5-methyl-	16347	019744-64-0	58
41	43.088	1.41	C:\Database\NIST05a.L			
		1	,15-Hexadecadiene	73063	021964-51-2	2 95
			,13-Tetradecadiene	52921	021964-49-8	3 94
			-Hexadecyn-1-ol	83989	000822-21-9	93
42	44.103	3.51	C:\Database\NIST05a.L			
46	44.105		-Hexadecene	74521	000629-73-2	99
			-A-Hexadecene		1000130-87-	
			-Hexadecene		000629-73-2	
			lexadecene	74519	000025-75-2	. 50
43	44.755		C:\Database\NIST05a.L		AAAF	
			lexadecane		000544-76-3	
			lexadecane		000544-76-3	
		Н	lexadecane	76092	000544-76-3	3 96
44	45.620	0.24	C:\Database\NIST05a.L			
			-(But-3-enyl)-cyclohexanone	24098	003636-03-1	62
			<pre>Syclohexane, 1-(cyclohexylmethyl)-</pre>		054823-95-9	
			-methyl-, trans-	24299		
		C	<pre>cyclohexane, 1-(cyclohexylmethyl)- ?-methyl-, cis-</pre>	52954	054824-04-3	3 53
	46.460					

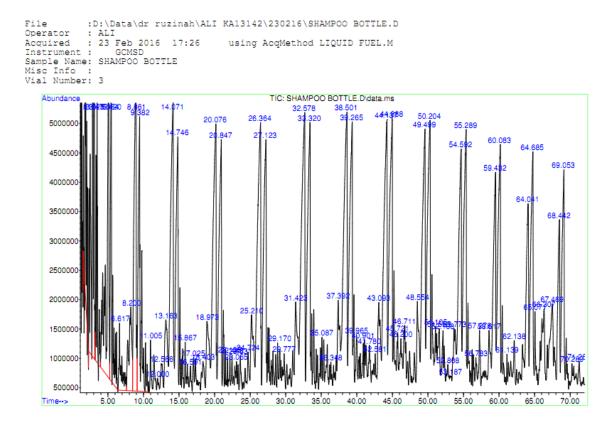
45 46.122 0.27 C:\Database\NIST05a.L

₽ k. #	RT	Area%	Library/ID	Ref#	CAS#	Qual
			richloroacetic acid, undec-2-enyl ester	132994	1000299-26-	1 62
			-11,13-Dimethyl-11-tetradecen-1-o acetate	113402	1000131-36-	6 58
		ti	icyclo[3.1.1]heptane, 2,6,6-trime hyl-, [1R-(1.alpha.,2.alpha.,5.al ha.)]-	16450	004863-59-6	55
46	46.656		C:\Database\NIST05a.L -Hexadecene, (Z)-	74526	034303-81-6	05
		C	yclopentadecane	64458	000295-48-7	95
			yclohexadecane	74524	000295-65-8	93
47	48.493		C:\Database\NIST05a.L ,15-Hexadecadiene	73063	021964-51-2	90
		C	is-11-Tetradecen-1-ol ,19-Eicosadiene		034010-15-6	
48	49.401		C:\Database\NIST05a.L	110001	011011 00 1	
40	49.401	3	-Heptadecene, (Z)-		1000141-67-	
			-14-Hexadecenal -Heptadecene		330207-53-9 002579-04-6	
49	50.032		C:\Database\NIST05a.L			
	001000	H	eptadecane		000629-78-7	
			ept adecane ept adecane		000629-78-7 000629-78-7	
50	50.448	0.37 (C:\Database\NIST05a.L			
			-Heptadecene, (Z)- -Heptadecene		1000141-67-006765-39-5	
			-14-Hexadecenal		330207-53-9	
51	50.972		C:\Database\NIST05a.L			
			yclohexadecane -Octadecene, (E)-	93546	000295-65-8	92
		8	-Heptadecene	84040	054290-12-9	83
52	51.474		C:\Database\NIST05a.L ridecanedial	65765	063521-76-6	70
		В	icyclo[3.1.1]heptane, 2,6,6-trime		000473-55-2	
			hyl– xirane, tridecyl–	76039	018633-25-5	46
53	51.986		C:\Database\NIST05a.L			
		b	<pre>yclohexane, 1,1'-(1,4-butanediyl) is-</pre>	73075	006165-44-2	49
		C	<pre>yclohexane, (1-methylpropyl)- yclohexane, 1,1'-(1,5-pentanediyl</pre>		007058-01-7	
			bis-			
54	52.691		C:\Database\NIST05a.L	02524	DECEEN DO O	
		1	2-Heptadecyn-1-ol H-Indene, octahydro-5-methyl-	16347	056554-76-8 019744-64-0	46
		Sj	piro[5.6]dodecane	33517	000181-15-7	42
55	53.674		C:\Database\NIST05a.L -Hexadecyne	73057	000629-74-3	93
			,19-Eicosadiene		014811-95-1	

₽k∦	RT	Area%	Library/ID	Ref#	CAS#	Qual
		1,	19-Eicosadiene	110851	014811-95-	1 91
56	54.497	$\frac{1-6}{E-1}$:\Database\NIST05a.L Octadecene 15-Heptadecenal Nonadecene	93518	000112-88- 1000130-97 018435-45-	-9 99
57	55.084	Oct He:	:\Database\NIST05a.L tadecane xadecane tadecane	76093	000593-45- 000544-76- 000593-45-	3 95
58	55.469	5-0 E-1	:\Database\NIST05a.L Dctadecene, (E)- 7-Octadecene 15-Heptadecenal	93545	007206-21- 1000130-92 1000130-97	-0 95
59	56.644	Ox: (-	:\Database\NIST05a.L irane, hexadecyl-)-trans-Pinane 13-Tetradecadiene	16289	007390-81- 033626-25- 021964-49-	4 60
60	57.156	$\frac{1}{11}$:\Database\NIST05a.L Nonadecene -Dodecenol clododecanemethanol	45961	018435-45- 035289-31- 001892-12-	7 60
61	57.691	Z-1 1-1	:\Database\NIST05a.L 5-Nonadecene Nonadecene xadecanenitrile	102860	1000131-11 018435-45- 000629-79-	5 90
62	58.556	1, 18	:\Database\NIST05a.L 19-Eicosadiene -Nonadecen-1-ol 13-Tetradecadiene	113465	014811-95- 1000142-89 021964-49-	-2 91
63	59.336	$\frac{Z}{1-1}$:\Database\NIST05a.L 5-Nonadecene Nonadecene Nonadecene	102860	1000131-11 018435-45- 018435-45-	5 95
64	59.880	Noi Noi	:\Database\NIST05a.L nadecane nadecane ptadecane	104272	000629-92- 000629-92- 000629-78-	5 96
65	61.525	1, Bi	:\Database\NIST05a.L 19-Eicosadiene cyclo[10.8.0]eicosane, cis- clododecanemethanol	110854	014811-95- 1000155-82 001892-12-	-2 64
66	62.006	De n-J	:\Database\NIST05a.L cane, 2-cyclohexyl- Amylcyclohexane clohexane, (1-methylethyl)-	25925	013151-73- 029949-27- 000696-29-	7 52
67	62.380		:\Database\NIST05a.L Eicosene	112101	003452-07-	1 91

Pk #	RT	Area%	Library/ID	Ref#	CAS# Qual
			-14-Hexadecenal -Hexadecanol, 2-methyl-		330207-53-9 83 002490-48-4 55
68	63.245	1, 1,	C:\Database\NIST05a.L ,19-Eicosadiene ,19-Eicosadiene icyclo[10.8.0]eicosane, (E)-	110851	014811-95-1 94 014811-95-1 90 1000155-85-0 90
69	63.940	Cy E-	C:\Database\NIST05a.L ycloeicosane -14-Hexadecenal -Nonadecene	83987	000296-56-0 98 330207-53-9 98 018435-45-5 94
70	64.484	E i He	C:\Database\NIST05a.L icosane eptadecane eptadecane	85523	000112-95-8 99 000629-78-7 95 000629-78-7 95
71	65.916	Cy	C:\Database\NIST05a.L yclohexane, 1-(cyclohexylmethyl)- -methyl-, trans-	52955	054823-95-9 59
		O2 y] Cy	<pre>xalic acid, cyclohexylmethyl prop l ester yclopentane, 1,2-dimethyl-3-(1-me hylethyl)-</pre>		1000309-68-1 50 000489-20-3 50
72	66.663	De Cy	C:\Database\NIST05a.L ecane, 2-cyclohexyl- yclohexane, (1-methylpropyl)- yclohexane, (1-methylpropyl)-	17414	013151-73-0 86 007058-01-7 64 007058-01-7 59
73	67.347	1, E, ic	C:\Database\NIST05a.L ,19-Eicosadiene ,E,Z-1,3,12-Nonadecatriene-5,14-d ol yclododecanemethanol	121084	014811-95-1 64 1000131-11-4 59 001892-12-2 58
74	67.753	00 1,	C:\Database\NIST05a.L ctadecanal ,19-Eicosadiene ,19-Eicosadiene	110851	000638-66-4 94 014811-95-1 91 014811-95-1 91
75	68.351	Z- 1-	C:\Database\NIST05a.L -5-Nonadecene -Nonadecene D-Heneicosene (c,t)	102860	1000131-11-8 99 018435-45-5 97 095008-11-0 95
76	68.875	He He	C:\Database\NIST05a.L eneicosane eneicosane ctadecane	122436	000629-94-7 99 000629-94-7 96 000593-45-3 95
77	71.000	Be he Di	C:\Database\NIST05a.L enzenemethanamine, N-hydroxy-N-(p enylmethyl)- ibenzylamine, N-nitro- -Pentene, 3,3,4-trimethyl-5-pheny -	86498	000621-07-8 12 095835-70-4 12 1000150-35-3 10

Shampoo Bottle



₽k#	RT	Area%	Library/ID	Ref∦	CAS# Q	Jual
1	1.813	I 1	C:\Database\NIST05a.L sopropylcyclobutane -Heptene -Heptene	3229	000872-56-0 000592-76-7 000592-76-7	86
2	3.020	O H	C:\Database\NIST05a.L ctane eptane, 2,4-dimethyl- eptane, 2,4-dimethyl-	12289	000111-65-9 002213-23-2 002213-23-2	72
3	3.469	c c	C:\Database\NIST05a.L yclotrisiloxane, hexamethyl- yclotrisiloxane, hexamethyl- yclotrisiloxane, hexamethyl-	73121	000541-05-9 000541-05-9 000541-05-9	83
4	5.050	C 1	C:\Database\NIST05a.L yclopropane, 1-methyl-2-pentyl- -Nonene -Nonene	11145	041977-37-1 000124-11-8 000124-11-8	93
5	5.424	N	C:\Database\NIST05a.L onane onane onane	12267	000111-84-2 000111-84-2 000111-84-2	94
6	6.620	C 4	C:\Database\NIST05a.L yclopentene, 1-butyl- -Octyne, 2-methyl- H-Indene, octahydro-, trans-	10295	002423-01-0 010306-94-2 003296-50-2	59
7	8.201	1 M t	C:\Database\NIST05a.L ,11-Dodecadiene ethoxyacetic acid, 1-cyclopentyle hyl ester yclohexanemethanol, 2-methyl-	47053	005876-87-9 1000282-69-5 002105-40-0	5 47
8	8.863	1 1	C:\Database\NIST05a.L -Decene -Decene yclooctane, 1,2-dimethyl-	17321	000872-05-9 000872-05-9 013151-94-5	97
9	9.387	D D	C:\Database\NIST05a.L ecane ecane ecane	18485	000124-18-5 000124-18-5 000124-18-5	95
10	11.000	CN	C:\Database\NIST05a.L yclopentene, 1-pentyl- aphthalene, decahydro- yclopentene, 1-(3-methylbutyl)-	16321	004291-98-9 000091-17-8 037689-15-9	68
11	12.004	B t P C	C:\Database\NIST05a.L icyclo[3.1.1]heptane, 2,6,6-trime hyl-, [1R-(1.alpha.,2.alpha.,5.al ha.)]- yclooctene, 1,2-dimethyl- icyclo[2.2.2]octane, 2-methyl-	16326	004863-59-6 054299-96-6 000766-53-0	43
				20000	contes es V	

12 12.570 0.14 C:\Database\NIST05a.L

₽k#	RT	Area%	Library/ID	Ref#	CAS#	Qual
		C	aphthalene, decahydro-2-methyl- yclohexene, 1,2-dimethyl- icyclo[4.1.0]heptane, 3-methyl-	5818	002958-76-1 001674-10-8 041977-47-3	64
13	13.158	1, C:	C:\Database\NIST05a.L ,13-Tetradecadiene is-9-Tetradecen-1-ol -Undecyne	65989	021964-49-8 035153-15-2 002294-72-6	62
14	14.066	3- 1-	C:\Database\NIST05a.L -Undecene, (Z)- -Undecene -Undecene	25904	000821-97-6 000821-95-4 000821-95-4	93
15	14.749	Ui Ui	C:\Database\NIST05a.L ndecane ndecane ndecane	27238	001120-21-4 001120-21-4 001120-21-4	94
16	15.871	C	C:\Database\NIST05a.L yclohexane, pentyl- -Amylcyclohexane yclohexane, pentyl-	25925	004292-92-6 029949-27-7 004292-92-6	72
17	16.586	3, 3,	C:\Database\NIST05a.L ,4-Octadiene, 7-methyl- ,4-Octadiene, 7-methyl- -Octyne, 2-methyl-	10322	037050-05-8 037050-05-8 055402-15-8	58
18	17.024	$\frac{C_1}{1}$	C:\Database\NIST05a.L yclohexene, 1-pentyl- ,11-Dodecadiene yclohexene,1-hexyl-	33507	015232-85-6 005876-87-9 003964-66-7	59
19	18.402	9- Bi tl	C:\Database\NIST05a.L -Octadecyne icyclo[3.1.1]heptane, 2,6,6-trime hyl- -Undecyne	16398	035365-59-4 000473-55-2 002294-72-6	58
20	18.969	1 1	C:\Database\NIST05a.L ,11-Dodecadiene -Octadecyne yclododecene	92236	005876-87-9 000629-89-0 001501-82-2	91
21	20.079	1.1.	C:\Database\NIST05a.L -Dodecene -Dodecene yclododecane	34944	000112-41-4 000112-41-4 000294-62-2	94
22	20.849	D	C:\Database\NIST05a.L odecane odecane odecane	36429	000112-40-3 000112-40-3 000112-40-3	95
23	22.130	C) C)	C:\Database\NIST05a.L yclohexane, hexyl- yclohexane, hexyl- H-Pyrrole, 2,3-dihydro-1-methyl-	34975	004292-75-5 004292-75-5 033838-11-8	74

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24	22.440	6 C	C:\Database\NIST05a.L -Dodecene, (E)- yclopentane, (3-methylbutyl)- yclopentane, 1-pentyl-2-propyl-	17410	007206-17-9 5 001005-68-1 5 062199-51-3 4	2
25	23.060	1 6	C:\Database\NIST05a.L -Tridecene -Tridecene, (Z)- -Eicosyne	44628	002437-56-1 9 006508-77-6 7 071899-38-2 5	2
26	23.637	9 C	C:\Database\NIST05a.L -Methylbicyclo[3.3.1]nonane ycloheptane, methyl- -Cyclohexylheptene	6507	025107-01-1 5 004126-78-7 3 114614-83-4 3	8
27	24.726	1 5 D	C:\Database\NIST05a.L -Pentadecyne -Eicosyne odeca-1,6-dien-12-ol, 6,10-dimeth 1-	110845	000765-13-9 5 074685-31-7 5 1000156-13-8	8
28	25.207	B t	C:\Database\NIST05a.L icyclo[3.3.2]decan-9-one rans-Decalin, 2-methyl- -Nonadecen-1-ol	24396	028054-91-3 9 1000152-47-3 1000131-11-9	87
29	26.360	1 1	C:\Database\NIST05a.L -Tridecene -Tridecene -Tridecene	44617	002437-56-1 9 002437-56-1 9 002437-56-1 9	7
30	27.119	T T	C:\Database\NIST05a.L ridecane ridecane ridecane	46087	000629-50-5 9 000629-50-5 9 000629-50-5 9	7
31	29.170	C 3	C:\Database\NIST05a.L yclopentene, 1-octyl- -Dodecyne yclopentene,1-(2-methylpropyl)-	33484	052315-44-3 9 006790-27-8 5 053098-47-8 4	0
32	29.779	c c	C:\Database\NIST05a.L yclohexasiloxane, dodecamethyl- yclohexasiloxane, dodecamethyl- yclohexasiloxane, dodecamethyl-	179153	000540-97-6 7 000540-97-6 6 000540-97-6 4	8
33	31.424	1 5	C:\Database\NIST05a.L ,13-Tetradecadiene -Nonadecen-1-ol -Cyclohexyl-1-pentene	113464	021964-49-8 9 1000131-11-9 005729-54-4 8	90
34	32.577	2 1	C:\Database\NIST05a.L -Tetradecene, (E)- -Tetradecene -Tetradecene	54512	035953-53-8 9 001120-36-1 9 001120-36-1 9	6
35	33.314		C:\Database\NIST05a.L etradecane	55975	000629-59-4 9	7

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			"etradecane "etradecane		000629-59-4 000629-59-4	
36	35.088	0	C:\Database\NIST05a.L Cyclopentadecane Cyclotetradecane Cyclotetradecane	54515	000295-48-7 000295-17-0 000295-17-0	95
37	36.348	i i	C:\Database\NIST05a.L Cyclopropane, 1-butyl-2-pentyl-, c S- Cyclohexane, 1,1-dimethyl- Cyclopentane, (1-methylbutyl)-	6568	074663-88-0 000590-66-9 004737-43-3	38
38	37.395	1.33 1	C:\Database\NIST05a.L ,12-Tridecadiene ,12-Tridecadiene 1-Hexadecen-1-ol, (Z)-	43178 43179	021964-48-7 021964-48-7 056683-54-6	91 91
39	38.506	1	C:\Database\NIST05a.L Pentadecene Pentadecene Pentadecene	64457	013360-61-7 013360-61-7 013360-61-7	96
40	39.264	H H	C:\Database\NIST05a.L Pentadecane Pentadecane Pentadecane	66067	000629-62-9 000629-62-9 000629-62-9	95
41	39.969	1	C:\Database\NIST05a.L Cyclopentane, 2-isopropyl-1,3-dime hyl- Cyclopentadecane Triallylmethylsilane	64459	032281-85-9 000295-48-7 001112-91-0	50
42	40.899	r F	C:\Database\NIST05a.L n-Nonylcyclohexane leptylcyclohexane n-Nonylcyclohexane	44631	002883-02-5 005617-41-4 002883-02-5	64
43	41.785	0	C:\Database\NIST05a.L Cyclohexene, 1-nonyl- .H-Indene, octahydro-5-methyl- Cyclohexene, 3-nonyl-	16347	015232-88-9 019744-64-0 015232-79-8	70
44	42.576	C E	C:\Database\NIST05a.L Cyclododecanemethanol Pentadecane, 3-methyl- Tetradecanal	76102	001892-12-2 002882-96-4 000124-25-4	56
45	43.088	1	C:\Database\NIST05a.L ,15-Hexadecadiene -Hexadecyne ,Z-2,15-Octadecedien-1-ol acetate	73057	021964-51-2 000629-74-3 1000130-95-	93
46	44.135	1	C:\Database\NIST05a.L -Hexadecene Z-8-Hexadecene L-Hexadecene	74523	000629-73-2 1000130-87- 000629-73-2	5 98

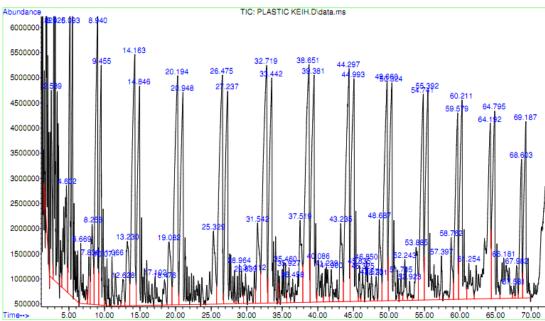
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47	44.883	Hea	:\Database\NIST05a.L kadecane kadecane kadecane	76092	000544-76- 000544-76- 000544-76-	-3 96
48	45.716	Oxa ade Cyc	:\Database\NIST05a.L alic acid, cyclohexylmethyl tetr ecyl ester clohexadecane -Oxabicyclo[10.1.0]tridecane	74525	1000309-69 000295-65- 000286-99-	-8 46
49	46.197	Cyc 1-0	:\Database\NIST05a.L clododecanemethanol Octadecanol Heptadecanol	105754	001892-12- 000112-92- 001454-85-	-5 64
50	46.710	Cyc Z-8	:\Database\NIST05a.L clohexadecane 3-Hexadecene Docosene	74523	000295-65- 1000130-87 001599-67-	7-5 91
51	48.558	1,1 1,1	:\Database\NIST05a.L 19-Eicosadiene 13-Tetradecadiene -Hexadecen-1-ol, (Z)-	52921	014811-95- 021964-49- 056683-54-	-8 76
52	49.498	3-F E-1	:\Database\NIST05a.L Heptadecene, (Z)- l4-Hexadecenal Heptadecene	83987	1000141-67 330207-53- 002579-04-	9 99
53	50.203	Her Her	:\Database\NIST05a.L ptadecane ptadecane decane, 2,6,11-trimethyl-	85523	000629-78- 000629-78- 031295-56-	-7 96
54	51.100	Cyc 1-0	:\Database\NIST05a.L clopentadecane Octadecene clotetradecane	93544	000295-48- 000112-88- 000295-17-	-9 90
55	51.549	Oxi Cyc	:\Database\NIST05a.L irane, tetradecyl- clododecanemethanol Nonadecanol	55891	007320-37- 001892-12- 001454-84-	-2 60
56	52.104	Cyc Tet	:\Database\NIST05a.L clopentane, (2-methylpropyl)- tradecanal chloroacetic acid, heptadecyl es	65973	003788-32- 000124-25- 1000282-98	4 49
57	52.809	1H- 1,2	:\Database\NIST05a.L -Indene, octahydro-5-methyl- 2-Diheptylcyclopropene 2-Dioctylcyclopropene	82657	019744-64- 035365-53- 001089-40-	8 53
58	53.183	0.40 C:	:\Database\NIST05a.L			

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		2	Heptadecane, 3-methyl- 2-Thiopheneacetic acid, 3,5- vlcyclohexyl ester Carbonic acid, isobutyl octa ester	-dimeth 93158	006418-44- 1000278-92 1000314-61	-2 43
59	53.770	F 1	C:\Database\NIST05a.L 2-2-Octadecadecen-1-ol ,13-Tetradecadiene ,19-Eicosadiene	52921	1000131-10 021964-49- 014811-95-	8 78
60	54.593	1 F	C:\Database\NIST05a.L -Octadecene 2-15-Heptadecenal -Nonadecene	93518	000112-88- 1000130-97 018435-45-	-9 99
61	55.287	0	C:\Database\NIST05a.L Octadecane Octadecane Pentadecane	94930	000593-45- 000593-45- 000629-62-	3 97
62	56.783	9	C:\Database\NIST05a.L)-Octadecene, (E)- Pentadecanethiol (-)-trans-Pinane	88046	007206-25- 025276-70- 033626-25-	4 64
63	57.274	3	C:\Database\NIST05a.L B-Hexadecene, (Z)- Cyclohexane, (1-methylpropy) Cyclohexane, (1,3-dimethylbu	L)- 17414	034303-81- 007058-01- 061142-19-	7 46
64	58.620	C F	C:\Database\NIST05a.L Cyclododecanemethanol 2-2-Octadecadecen-1-ol 1,19-Eicosadiene	104257	001892-12- 1000131-10 014811-95-	-2 64
65	59.432	2	C:\Database\NIST05a.L Z-5-Nonadecene Z-Nonadecene Z-Nonadecene	102860	1000131-11 018435-45- 018435-45-	5 95
66	60.083	1 1	C:\Database\NIST05a.L Ionadecane Ionadecane Ieptadecane	104272	000629-92- 000629-92- 000629-78-	5 96
67	61.141	5	C:\Database\NIST05a.L -Eicosene, (E)- 2-5-Nonadecene 2-Nonadecene	102861	074685-30- 1000131-11 018435-45-	-8 96
68	62.134	I r	C:\Database\NIST05a.L Decane, 2-cyclohexyl- h-Amylcyclohexane Cyclohexane, pentyl-	25925	013151-73- 029949-27- 004292-92-	7 49
69	64.046	0	C:\Database\NIST05a.L Cycloeicosane Eicosene		000296-56- 003452-07-	

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		Е	-15-Heptadecenal	93518	1000130-97-9 96
70	64.687	E	C:\Database\NIST05a.L Licosane Octadecane Licosane	94930	000112-95-8 99 000593-45-3 95 000112-95-8 93
71	65.072	5 1	C:\Database\NIST05a.L -Eicosene, (E)- -Nonadecene -Tricosene, (Z)-	102860	074685-30-6 70 018435-45-5 64 027519-02-4 62
72	66.311	9 Z	C:\Database\NIST05a.L -Tricosene, (Z)- -5-Nonadecene -Tricosene, (Z)-	102861	027519-02-4 96 1000131-11-8 95 027519-02-4 95
73	67.465	C 1	C:\Database\NIST05a.L Octadecane -Octadecene lexadecane, 2,6,10,14-tetramethyl-	93544	000593-45-3 95 000112-88-9 90 000638-36-8 87
74	68.437	Z 1	C:\Database\NIST05a.L -5-Nonadecene -Nonadecene -Tricosene, (Z)-	102860	1000131-11-8 99 018435-45-5 97 027519-02-4 96
75	69.056	H	C:\Database\NIST05a.L leneicosane leneicosane octadecane	122436	000629-94-7 99 000629-94-7 96 000593-45-3 95
76	70.285	1 9	C:\Database\NIST05a.L -Tricosene -Tricosene, (Z)- -Eicosene, (E)-	138119	018835-32-0 99 027519-02-4 93 074685-30-6 89
77	71.257	3 U	C:\Database\NIST05a.L -(4,8,12-Trimethyltridecyl) furan Indecane, 2-cyclohexyl- Decane, 2-cyclohexyl-	84051	1000245-55-1 83 013151-77-4 70 013151-73-0 55

Plastic Wrapper

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Instrument : GCMSD
Sample Name: PLASTIC KEIH
Misc Info :
Vial Number: 5
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      Abundance
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₽k∦	RT	Area%	Library/ID	Ref#	CAS#	Qual
1	1.824	1-Hept	ene, 5-methyl-, (E)-	3310	000592-76- 007385-82-2 000592-76-	2 55
2	2.540	Cycloh Cycloh	atabase\NIST05a.L bexene, 4-methyl- bexene, 1-methyl- bexane, methylene-	2812	000591-47-9 000591-49-1 001192-37-6	l 62
3	3.031	Octane Heptar	atabase\NIST05a.L e ne, 2,4-dimethyl- ne, 2,4-dimethyl-	12289	000111-65-9 002213-23-2 002213-23-2	2 72
4	4.601	Styrer Styrer		4751	000100-42-5 000100-42-5 000694-87-1	5 59
5	5.093	1-None	propane, 1-methyl-2-pentyl-	11252	000124-11-8 041977-37-3 000124-11-8	l 91
6	6.674	Cyclop Cyclop	atabase\NIST05a.L pentene, 1-butyl- pentene, 1-pentyl- pentene, 1-pentyl-	16315	002423-01-0 004291-98-9 004291-98-9	9 50
7	7.838	1-Ethy Cyclob	atabase\NIST05a.L /l-5-methylcyclopentene hexane, ethenyl- l ethyl cyclopentene	5781	097797-57-4 000695-12-5 019780-56-4	5 46
8	8.254	1,11-E 1,11-E	ntabase∖NIST05a.L Dodecadiene Dodecadiene en-1-ol, (E)-	33506	005876-87-9 005876-87-9 010339-60-3	9 50
9	8.938	2.97 C:\Da 1-Dece 1-Dece 1-Dece	ene	17320	000872-05-9 000872-05-9 000872-05-9	9 97
10	9.451	2.11 C:\Da Decane Decane Decane)	18485	000124-18-5 000124-18-5 000124-18-5	5 95
11	10.070	2-Meth Cyclop	atabase\NIST05a.L hylbicyclo[3.2.1]octane pentane, pentylidene- lopentylcyclopentene	16329	1000215-28- 053366-55-5 002690-17-1	5 68
12	11.064	Cyclop	ntabase\NIST05a.L pentene, 1-pentyl- palene, decahydro- decene	16321	004291-98-9 000091-17-8 003618-12-0	3 68

Pk∦	RT	Area%	Library/ID	Ref#	CAS#	Qual
13	12.623	Naj ci:	:\Database\NIST05a.L phthalene, decahydro-2-methyl- s-Decalin, 2-syn-methyl- 8-Nonadiene, 2,8-dimethyl-	24400	002958-76-1 1000155-85- 020054-25-5	6 64
14	13.232	1, 5-1	:\Database\NIST05a.L 13-Tetradecadiene Undecyne ,14-Eicosadienoic acid, methyl e er	24365	021964-49-8 002294-72-6 002463-02-7	62
15	14.162	1-1 3-1	:\Database\NIST05a.L Undecene Undecene, (Z)- Undecene	25915	000821-95-4 000821-97-6 000821-95-4	93
16	14.845	Uno	:\Database\NIST05a.L decane decane decane	27238	001120-21-4 001120-21-4 001120-21-4	94
17	17.099	Cy Cy	:\Database\NIST05a.L clohexene, 1-pentyl- clohexene, 3-pentyl- clohexene,1-hexyl-	24389	015232-85-6 015232-92-5 003964-66-7	52
18	18.477	5-1 Bi th	:\Database\NIST05a.L Undecyne cyclo[3.1.1]heptane, 2,6,6-trime yl-)-trans-Pinane	16398	002294-72-6 000473-55-2 033626-25-4	58
19	19.086	1, 1,	:\Database\NIST05a.L 11-Dodecadiene 11-Dodecadiene clododecene	33506	005876-87-9 005876-87-9 001501-82-2	90
20	20.197	1 - 1 - 1 - 1 - 1	:\Database\NIST05a.L Dodecene Dodecene clodecane	34944	000112-41-4 000112-41-4 000293-96-9	94
21	20.945	Do: Do:	:\Database\NIST05a.L decane decane decane	36430	000112-40-3 000112-40-3 000112-40-3	95
22	25.324	1-1 ci:	:\Database\NIST05a.L Heptadecyne s-9-Tetradecen-1-ol cyclo[3.3.2]decan-9-one	65989	026186-00-5 035153-15-2 028054-91-3	86
23	26.478	$\frac{1-1}{1-1}$:\Database\NIST05a.L Tridecene Tridecene Tridecene	44617	002437-56-1 002437-56-1 002437-56-1	97
24	27.236	2.94 C	:\Database\NIST05a.L			

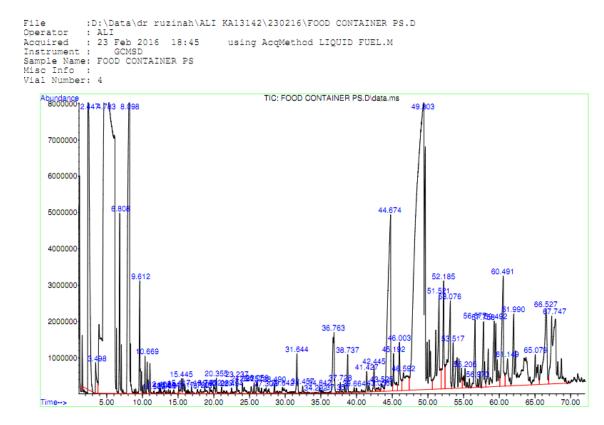
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		Tr	idecane		46084	000629-50-	5 96
		Tr	idecane		46086	000629-50-	5 95
		Tr	idecane		46085	000629-50-	5 95
25	28.967		:\Database\NIST05	a.L			
			clotridecane			000295-02-	
			Nonene, 5-buty1-			007367-38-	
		Су	clotetradecane		54513	000295-17-	0 58
26	29.843		:\Database\NIST05				
			clohexasiloxane,			000540-97-	
			clohexasiloxane,			000540-97-	
		Су	clohexasiloxane,	dodecamethy1-	179151	000540-97-	6 43
27	31.114		:\Database\NIST05	a.L			
			Pentadecyne			000765-13-	
			Hexadecyne			000629-74-	
		Ζ,	6-Dimethylbicyclo	[3.2.1]octane	16365	1000215-28	-2 58
28	31.541		:\Database\NIST05				
			13-Tetradecadiene			021964-49-	
			Cyclohexyl-1-pent			005729-54-	
		ci	s-7-Dodecen-1-yl	acetate	75866	014959-86-	5 72
29	32.716	3.92 C	:\Database\NIST05	a.L			
		2-	Tetradecene, (E)-		54521	035953-53-	8 98
		1-	Tetradecene		54512	001120-36-	1 96
		1-	Tetradecene		54508	001120-36-	1 95
30	33.443	3.07 C	:\Database\NIST05	a.L			
		Te	tradecane		55975	000629-59-	4 97
		Te	tradecane			000629-59-	
		Те	tradecane		55973	000629-59-	496
31	35.461	0.54 C	:\Database\NIST05	a.L			
		Cy	clopentene, 1-oct	y1-	43184	052315-44-	3 53
			Octyne, 2-methyl-		10299	055402-15-	8 52
		Су	clopentene,1-hept	y1-	33526	004292-00-	6 50
32	35.931	0.22 C	:\Database\NIST05	a.L			
		Cy	clohexene, 1-octy	1-	52924	015232-87-	8 87
			clohexene, 1-hexyl		33523	003964-66-	7 76
		Су	clohexene, 3-octy	1-	52925	015232-94-	7 68
33	36.455	0.16 C	:\Database\NIST05	a.L			
		Cy	clopentane, 1,2-d		17461	000489-20-	3 52
			ylethyl)-	ul 2 contul o	25020	074662 00	0.46
		is	clopropane, 1-but	.yı-z-pentyı-, c	35079	074663-88-	0 46
		Су	clooctane, 1,5-di	methyl-	17397	021328-57-	4 43
34	37.523	1.10 C	:\Database\NIST05	a.L			
	0.1000		13-Tetradecadiene		52919	021964-49-	8 90
			12-Tridecadiene	-		021964-48-	
			13-Tetradecadiene			021964-49-	
35	38.655	3 95 0	:\Database\NIST05	a. L			
55	50.055		Pentadecene		64454	013360-61-	7 97
			Pentadecene			013360-61-	
		1	- chessee one		01107	010000-01-	

₽k∦	RT	Area%	Library/ID	Ref#	CAS#	Qual
		1	-Pentadecene	64455	013360-61-	793
36	39.382	P P	C:\Database\NIST05a.L entadecane entadecane entadecane	66067	000629-62- 000629-62- 000629-62-	9 96
37	40.087	c t c	C:\Database\NIST05a.L yclopentane, 2-isopropyl-1,3-dime hyl- ycloheptane, methyl- yclohexanemethanol	6515	032281-85- 004126-78- 000100-49-	7 46
38	41.240	c c	C:\Database\NIST05a.L yclohexadecane yclotetradecane -Hexadecene, (Z)-	54515	000295-65- 000295-17- 034303-81-	0 87
39	41.903	C C B	C:\Database\NIST05a.L yclohexene, 3-nonyl- yclohexene, 1-nonyl- icyclo[4.1.0]heptane, 2-methyl-7- entyl-	63043	015232-79- 015232-88- 055937-92-	9 70
40	43.238	1 1	C:\Database\NIST05a.L ,15-Hexadecadiene ,13-Tetradecadiene 1-Hexadecen-1-ol, (Z)-	52919	021964-51- 021964-49- 056683-54-	8 90
41	44.295	$\frac{1}{Z}$	C:\Database\NIST05a.L -Hexadecene -8-Hexadecene -Hexadecene	74523	000629-73- 1000130-87 000629-73-	-5 98
42	44.990	H H	C:\Database\NIST05a.L exadecane exadecane exadecane	76093	000544-76- 000544-76- 000544-76-	3 98
43	45.834	O y c	C:\Database\NIST05a.L xalic acid, cyclohexylmethyl prop l ester is-11-Hexadecenal -Tetradecenal, (Z)-	83994	1000309-68 053939-28- 053939-27-	9 47
44	46.325	(B t	C:\Database\NIST05a.L -)-trans-Pinane icyclo[3.1.1]heptane, 2,6,6-trime hyl- ,15-Hexadecadiene	16406	033626-25- 000473-55- 021964-51-	2 52
45	46.848	0.41 C C	C:\Database\NIST05a.L yclohexadecane yclohexadecane yclopentadecane	74525 74524	000295-65- 000295-65- 000295-48-	895 893
46	47.575	1	C:\Database\NIST05a.L -Pentadecyne -Methyloctahydrocoumarin		000765-13- 080648-29-	

₽k∦	RT	Area%	Library/ID	Ref#	CAS∦ Ç	Qual
		1	H-Indene, octahydro-5-methyl-	16347	019744-64-0	46
47	48.205	0 3 0	C:\Database\NIST05a.L Cyclohexane, 1-(cyclohexylmethyl)- B-methyl-, trans- Cyclohexane, 1-(cyclohexylmethyl)- H-methyl-, cis-		054823-95-9 054823-97-1	
		Т	etradecanenitrile	63714	000629-63-0	62
48	48.686	1 1	C:\Database\NIST05a.L ,13-Tetradecadiene ,13-Tetradecadiene sis-11-Tetradecen-1-ol	52919	021964-49-8 021964-49-8 034010-15-6	89
49	49.658	3 E	C:\Database\NIST05a.L 3-Heptadecene, (Z)- 3-14-Hexadecenal 3-Heptadecene	83987	1000141-67-3 330207-53-9 054290-12-9	99
50	50.320	E	C:\Database\NIST05a.L leptadecane leptadecane oodecane, 2,6,11-trimethyl-	85523	000629-78-7 000629-78-7 031295-56-4	96
51	51.709	E t T	C:\Database\NIST05a.L Bicyclo[3.1.1]heptane, 2,6,6-trime hyl- Tridecanedial -)-trans-Pinane	65765	000473-55-2 063521-76-6 033626-25-4	70
52	52.243	t C	C:\Database\NIST05a.L rans-Undec-4-enal Cyclopentane, decyl- Dichloroacetic acid, heptadecyl es er	64463	068820-35-9 001795-21-7 1000282-98-2	60
53	52.926	1	C:\Database\NIST05a.L H-Indene, octahydro-5-methyl- 4-Methyl-pent-3-enyl)-cyclohexane R)-(-)-(Z)-14-Methyl-8-hexadecen- -ol	33544	019744-64-0 1000185-19-1 030689-78-2	42
54	53.888	1	C:\Database\NIST05a.L is-9-Tetradecen-1-ol ,19-Eicosadiene ,13-Tetradecadiene	110850	035153-15-2 014811-95-1 021964-49-8	90
55	54.742	1 E	C:\Database\NIST05a.L -Octadecene -15-Heptadecenal -Nonadecene	93518	000112-88-9 1000130-97-9 018435-45-5	99
56	55.394	C F	C:\Database\NIST05a.L Octadecane Pentadecane Octadecane	66065	000593-45-3 000629-62-9 000593-45-3	94
57	57.402		C:\Database\NIST05a.L -Nonadecene	102859	018435-45-5	72

²k∦	RT	Area%	Library/ID	Ref#	CAS# Qual
			/clohexane, (1,3-dimethylbutyl)- -Octadecene, (E)-		061142-19-6 46 007206-25-9 38
58	58.759	Ζ, 1,	C:\Database\NIST05a.L .Z-2,15-Octadecedien-1-ol acetate .15-Hexadecadiene .19-Eicosadiene	73063	1000130-95-1 89 021964-51-2 86 014811-95-1 81
59	59.581	Z - 1 -	C:\Database\NIST05a.L -5-Nonadecene -Nonadecene -Nonadecene	102860	1000131-11-8 99 018435-45-5 95 018435-45-5 94
60	60.212	No No	C:\Database\NIST05a.L onadecane onadecane eptadecane	104272	000629-92-5 96 000629-92-5 95 000629-78-7 94
61	61.258	1 - Z -	C:\Database\NIST05a.L -Nonadecene -5-Nonadecene yclotetracosane	102861	018435-45-5 98 1000131-11-8 96 000297-03-0 95
62	64.196	E- Cy	C:\Database\NIST05a.L -15-Heptadecenal ycloeicosane -Octadecene	112104	1000130-97-9 98 000296-56-0 98 000112-88-9 97
63	64.794	Ei Oc	C:\Database\NIST05a.L icosane ctadecane icosane	94930	000112-95-8 99 000593-45-3 95 000112-95-8 94
64	66.183	1- Pe	C:\Database\NIST05a.L -Octadecene entacosane ctadecanal	153747	000112-88-9 70 000629-99-2 53 000638-66-4 50
65	67.582	1- 9-	C:\Database\NIST05a.L -Docosene -Tricosene, (Z)- -Heptadecene	138119	001599-67-3 94 027519-02-4 91 006765-39-5 53
66	67.977	0) (I 1-	C:\Database\NIST05a.L kirane, hexadecyl- R)-(-)-(Z)-14-Methyl-8-hexadecen- -ol 13-Tetradecadiene	94911	007390-81-0 95 030689-78-2 86 021964-49-8 78
67	68.608	1.26 C Z- 1-	::>=retradecadiene C:\Database\NIST05a.L -5=Nonadecene Nonadecene)=Heneicosene (c,t)	102861 102860	1000131-11-8 99 018435-45-5 97 095008-11-0 96
68	69.184	He He	C:\Database\NIST05a.L eneicosane eneicosane etratriacontane	122436	000629-94-7 99 000629-94-7 95 014167-59-0 91

Polystyrene



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1	2.444	Tol Tol	\Database\NIST05a.L Jene Jene	2400	000108-88-3 000108-88-3	93
2	3.501	0.34 C: Cyc	uene \Database\NISTO5a.L lotrisiloxane, hexamethyl	- 73123	000108-88-3	83
		Cyc	lotrisiloxane, hexamethyl lotrisiloxane, hexamethyl		000541-05-9 000541-05-9	
3	4.783	Sty. Sty	\Database\NIST05a.L rene rene yclo[4.2.0]octa-1,3,5-tri	4751	000100-42-5 000100-42-5 000694-87-1	96
4	6.813	Ben	\Database\NIST05a.L zaldehyde zaldehyde zene, 2-propenyl-	4936	000100-52-7 000100-52-7 000300-57-2	90
5	8.094	.al	\Database\NIST05a.L phaMethylstyrene phaMethylstyrene phaMethylstyrene	8693	000098-83-9 000098-83-9 000098-83-9	93
6	9.611	Ben Ben	\Database\NIST05a.L zene, 1-propenyl- zene, cyclopropyl- zene, 2-propenyl-	8691	000637-50-3 000873-49-4 000300-57-2	89
7	10.669	Ace Ace	\Database\NIST05a.L tophenone tophenone tophenone	9074	000098-86-2 000098-86-2 000098-86-2	91
8	11.587	Ben n-P	\Database\NIST05a.L zene, (1,1-dimethylethoxy entylpyrazine zene, butoxy-	23571	006669-13-2 006303-75-9 001126-79-0	38
9	12.410	Oxi Ben 1-	\Database\NIST05a.L rane, 2-methyl-2-phenyl- zeneacetaldehyde, .alpha. zeneacetaldehyde, .alpha.	-methy 14863	002085-88-3 000093-53-8 000093-53-8	94
10	13.072	Tri Tet ca-	\Database\NIST05a.L quinacene racyclo[5.3.0.0<2,6>.0<3, 4,8-diene zene, (1-methylene-2-prop	10>]de 12715	006053-74-3 034324-40-8 002288-18-8	93
11	13.649	1-U 3-T	\Database\NIST05a.L ndecene etradecene, (E)- ndecene, (Z)-	54530	000821-95-4 041446-68-8 000821-97-6	80
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12 14.375 0.03 C:\Database\NIST05a.L

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		Be	nzene, 2-butenyl- nzene, 1-butenyl-, (E)- nzene, (2-methyl-1-propenyl)-	13605	001560-06-1 9 001005-64-7 9 000768-49-0 9	
13	15.112	2- 18	:\Database\NIST05a.L Phenylpropenal -Inden-1-one, 2,3-dihydro- Phenyl-1-aza-bicyclo[1.1.0]butan	14079	004432-63-7 8 000083-33-0 4 017945-94-7 3	46
14	15.444	Be	:\Database\NIST05a.L nzene, (1-ethyl-2-propenyl)- nzene, (1-methylenebutyl)- nzene, (1-methylenebutyl)-	20794	019947-22-9 005676-32-4 005676-32-4	91
15	17.719	Be	:\Database\NIST05a.L nzene,2-cyclopenten-1-yl- nzene, 1-cyclopenten-1-yl- nzene, (2-cyclopropylethenyl)-	19678	037689-22-8 000825-54-7 1000142-01-6	91
16	18.146	1H Na	:\Database\NIST05a.L -Indene, 1-ethenyl-2,3-dihydro- phthalene, 1,2-dihydro-6-methyl- -Indene, 4,7-dimethyl-	19689	051783-46-1 9 002717-47-7 9 006974-97-6 8	90
17	18.755	Cy Cy	:\Database\NIST05a.L clopentasiloxane, decamethyl- clopentasiloxane, decamethyl- clopentasiloxane, decamethyl-	161017	000541-02-6 000541-02-6 000541-02-6	81
18	19.492	1- Cy	:\Database\NIST05a.L Dodecene clododecane Undecanol	34948	000112-41-4 9 000294-62-2 9 000112-42-5 9	64
19	20.357	Be 1-	:\Database\NIST05a.L nzene, 1-hexynyl- Phenylbicyclo[2.1.1]hexane 2,3-Trimethylindene	28463	001129-65-3 9 029508-78-9 9 004773-83-5 4	50
20	21.094	Ве 1,	:\Database\NIST05a.L nzene, (1-methylenepentyl)- 3-Propanediol, 2-methyl-2-phenyl x-1-ene,2,5-diphenyl-	33222	020826-80-6 024765-53-5 032375-29-4	72
21	22.494	Be Be	:\Database\NIST05a.L nzene, hexyl- nzene, hexyl- nzene, hexyl-	30792	001077-16-3 001077-16-3 001077-16-3	42
22	23.241	Be 1H	:\Database\NIST05a.L nzene, 3,5-hexadienyl- -Imidazole, 1-(phenylmethyl)- -Imidazole, 1-(phenylmethyl)-	28311	039669-95-9 5 004238-71-5 004238-71-5	43
23	24.032	Be Be	:\Database\NIST05a.L nzene,2-cyclopenten-1-yl- nzene, 1-cyclopenten-1-yl- nzene, 1-cyclopenten-1-yl-	19681	037689-22-8 000825-54-7 000825-54-7	94

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24	25.260	Be 1H 3-	:\Database\NIST05a.L nzene, 3-heptynyl- -Imidazole, 1-(phenylmethyl)- Benzyl-4-bromo-1,2,3-triazole 1- ide	28304	056293-04-0 004238-71-5 1000099-47-	43
25	26.061	He Be	:\Database\NIST05a.L xa-2,4-dienylbenzene nzene, 1,3-hexadienyl- nzene, 1,3-hexadienyl-	28454	079482-86-3 041635-77-2 041635-77-2	78
26	27.301	(4 en 1-	:\Database\NIST05a.L -Methyl-1-methylenepent-4-enyl)b zene Phenyl-1-heptyne -Indene, 1-methyl-3-propyl-	37867	063942-88-1 014374-45-9 111400-83-0	43
27	28.486	0.07 C Bi Bi	:\Database\NIST05a.L phenyl phenyl phthalene, 2-ethenyl-	25990	000092-52-4 000092-52-4 000827-54-3	76
28	29.640	Cy Cy	:\Database\NIST05a.L clohexasiloxane, dodecamethyl- clohexasiloxane, dodecamethyl- clohexasiloxane, dodecamethyl-	179153	000540-97-6 000540-97-6 000540-97-6	86
29	31.648	Di Di	:\Database\NIST05a.L phenylmethane phenylmethane phenylmethane	35102	000101-81-5 000101-81-5 000101-81-5	95
30	32.460	Te Te	:\Database\NIST05a.L tradecane tradecane tradecane	55972	000629-59-4 000629-59-4 000629-59-4	98
31	34.297	Pe ,8 4-	:\Database\NIST05a.L ntacyclo[7.5.0.0(2,7).0(3,5).0(4)]tetradeca-10,12-diene Pentadecyne, 15-chloro- clopentane, ethylidene-	86735	088056-67-1 056554-70-2 002146-37-4	25
32	34.842	0.08 C 1, 1,	:\Database\NIST05a.L 1'-Biphenyl, 3-methyl- 1'-Biphenyl, 3-methyl- 1'-Biphenyl, 4-methyl-	35109 35115	000643-93-6 000643-93-6 000644-08-6	96 94
33	36.765	Be Be	:\Database\NIST05a.L nzene, 1,1'-(1,2-ethanediyl)bis- nzene, 1,1'-(1,2-ethanediyl)bis- nzene, 1,1'-(1,2-ethanediyl)bis-	44685	000103-29-7 000103-29-7 000103-29-7	50
34	37.352	5- ta 7-	:\Database\NIST05a.L Methyl-1-phenylbicyclo[3.2.0]hep ne Phenylbicyclo[3.2.0]heptan-6-one 6-Heptadiene, 2-methyl-6-phenyl-	47500	1000217-30- 073788-97-3 051708-97-5	42

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35	37.726	0.08 C:	\Database\NIST05a.L			
		1-P	entadecene	64457	013360-61-	7 98
		2-1	Cetradecene, (E)-	54521	035953-53-	8 91
		5-0	Octadecene, (E)-	93546	007206-21-	5 91
36	38.741	Ben	\Database\NIST05a.L nzene, 1,1'-(1-methyl-1,2-ethane v1)bis-	54595	005814-85-	7 90
		Ben	<pre>izene, 1,1'-(1-methyl-1,2-ethane v1)bis-</pre>	54594	005814-85-	7 90
			henylbutyric acid	31725	004593-90-	2 59
37	39.660		\Database\NIST05a.L	50050	000330 51	1 05
			phaMethylstilbene		000779-51-	
			lbene, .alphamethyl-, (E)-		000833-81-	
			(4-Methoxyphenyl)-2-hydroxyimino cetamide	53297	1000143-61	-3 90
20	41 422	0 26 0.	Detabage NICTOFA I			
38	41.422		NIST05a.L	50060	000779-51-	1 01
			phaMethylstilbene		095676-48-	
		1-	enanthrene, 9,10-dihydro-1-methy	52975	095676-48-	5 66
		Ant	hracene, 9,10-dihydro-2-methyl-	52971	000948-67-	4 60
39	42.448	0.28 C:	\Database\NIST05a.L			
			inic acid, diethyl-, 1-phenyl-1 openyl ester	58461	034602-33-	0 72
			zene, (1-ethyl-2-propenyl)-	20800	019947-22-	9 64
			zene, 1,1'-(1-butene-1,4-diyl)b		070388-65-	
			-, (Z)-	05107	070300-03	/ 01
40	43.056	0.04 C:	\Database\NIST05a.L			
		Cyc	lohexane, 1-phenyl-3,4-divinyl- 1R,3trans,4trans)-	66109	1000160-00	-5 91
		, (clohexane, 1-phenyl-3,4-divinyl- (1R,3cis,4cis)-		1000160-00	
		Ben	zenepropanoic acid, ethyl ester	41456	002021-28-	5 38
4 1	43.526		\Database\NIST05a.L			
			lexadecene		000629-73-	
			Ionadecene		018435-45-	
		1-0	locosene	129889	001599-67-	3 81
42	44.669	4.48 C	\Database\NIST05a.L			
			zene, 1,1'-(1,3-propanediyl)bis	54576	001081-75-	0 97
			zene, 1,1'-(1,3-propanediyl)bis		001081-75-	
		Ben	zene, 1,1'-(1,3-propanediyl)bis		001081-75-	
		Den	izene, 1,1 -(1,5-propaneury1,bis	54575	001001-75	0 90
43	45.193		\Database\NIST05a.L			
			2-Diphenylcyclopropane		029881-14-	
			(4-Methoxyphenyl)-2-hydroxyimino	53297	1000143-61	-3 90
		-ac	cetamide zene, 1,1'-cyclopropylidenebis-	52974	003282-18-	6 87
				56914	003202-10-	0 07
44	46.005		\Database\NIST05a.L	6440.2	001520-44-	1 02
			zene, 1,1'-(1-methyl-1,3-propan yl)bis-	04493	001320-44-	1 33
		Ben	zene, 1,1'-(3-methyl-1-propene- B-diyl)bis-	63118	007614-93-	9 64
		-, -				

₽ k #	RT	Area%	Library/ID	Ref#	CAS# Qual
			enzene, 1,1'-(1,2-dimethyl-1,2-et enediyl)bis-, (E)-	63120	000782-06-9 62
45	46.592	Be et 9-	C:\Database\NIST05a.L enzene, 1,1'-[1-(2-propenyl)-1,2- chanediyl]bis- -Methyl-9H-carbazole -Methylsulfonyl-1,2-diphenylethan	43890	005729-55-5 96 027323-29-1 30 015733-05-8 30
46	49.305	N- Be 3-	C:\Database\NIST05a.L -Benzyl-1H-benzimidazole enzene, (3-nitropropyl)- -Benzyl-4-bromo-1,2,3-triazole 1- kide	32997	004981-92-4 27 022818-69-5 27 1000099-47-9 22
47	51.517	2, 1 1- 3-	C:\Database\NIST05a.L 3-Diazabicyclo[2.2.1]hept-2-ene, 1,4-diphenyl- -(4-Methylphenyl)-4-phenylbuta-1, -diene	71521	106230-80-2 87 037985-11-8 62
48	52.190	1.25 (ıran, 2,5-diphenyl- C:\Database\NIST05a.L		000955-83-9 38
		1, Be Be	enzene, 1,1'-(3-methyl-1-propene- .3-diyl)bis- enzene, 1,1'-(1-butenylidene)bis- enzene, 1,1'-(1,2-dimethyl-1,2-et enediyl)bis-, (E)-	63092	007614-93-9 89 001726-14-3 86 000782-06-9 62
49	53.076	Be is Ir	C:\Database\NIST05a.L enzene, 1,1'-(1-butene-1,4-diyl)b s-, (Z)- odan, 1-methyl- enzene, (1-ethyl-2-propenyl)-	13588	070388-65-7 87 000767-58-8 72 019947-22-9 72
50	53.514	1, .ä ni	C:\Database\NIST05a.L 3-Propanediol, 2-methyl-2-phenyl alphaMethylalphaphenylsucci imide ex-1-ene,2,5-diphenyl-	49259	024765-53-5 64 001497-17-2 64 032375-29-4 59
51	55.202	(1 yc Be di .t	C:\Database\NIST05a.L L-Benzyl-1H-indol-3-yl)-acetaldeh de enzene, 1,1'-(1-ethyl-1,3-propane iyl)bis- petaAlanine, N-(3-ethoxy-3-oxop pyl)-N-(phenylmethyl)-, ethyl es	74551	1000188-47-3 14 000838-45-9 11 006938-07-4 9
52	56.580	te 0.77 (2, Bi 2,		81266	007283-49-0 99 118476-61-2 92 087433-33-8 90
53	56.975	Bu	C:\Database\NIST05a.L utylated Hydroxytoluene enzene, 1,1'-(1-methyl-2-butynyli		000128-37-0 47 054372-84-8 47

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		Phe	e)bis- nol, 4,6-di(1,1-dimethylethyl)- ethyl-	71398	000616-55-	7 46
54	57.755	2-M ((N	\Database\NIST05a.L ethylbenzyl cyanide -(2-Cyanoethyl)-N-methylamino)- indolyl)methylene)malononitrile		022364-68- 1000240-68	
		3(2	H)-Furanone, dihydro-2,2-dimeth 5-phenyl-	49861	063678-00-	2 20
55	59.496	2,3	\Database\NIST05a.L -Diazabicyclo[2.2.1]hept-2-ene, 4-diphenyl-	90805	106230-80-	2 94
		1,5 Tri	-Diphenylpyrazole cyclo[9.2.2.2(4,7)]heptadeca-1(,2,4(17),5,7(16),11(15),12-hept		006831-89- 049576-90-	
56	60.489	1-(\Database\NIST05a.L 4-Methylphenyl)-4-phenylbuta-1,	71521	037985-11-	8 55
		2,3	iene -Diazabicyclo[2.2.1]hept-2-ene, 4-diphenyl-	90805	106230-80-	2 45
			ane, 2,5-diphenyl-	71478	026569-47-	1 35
57	61.152	2-B 1-P	\Database\NIST05a.L uten-1-one, 1,3-diphenyl- henoxyphthalazine uten-1-one, 1,3-diphenyl-	72688	000495-45- 100537-30- 000495-45-	2 46
58	61.985	1,5	\Database\NIST05a.L -Diphenyl-1,5-hexadiene zene, [(3-phenyl-2-propenyl)thi		1000211-27 010276-14-	
			zene, 1,1'-(1,5-hexadiene-1,6-d)bis-	81279	004439-45-	6 43
59	65.083	1H-	\Database\NIST05a.L Cyclopenta[1]phenanthrene, 2,3- ydro-	70036	000723-98-	8 83
		Nap	hthalene, 2-(phenylmethyl)- hthalene, 2-(phenylmethyl)-		000613-59- 000613-59-	
60	66.525	Nap 1H- dih	\Database\NIST05a.L hthalene, 2-(phenylmethyl)- Cyclopenta[1]phenanthrene, 2,3- ydro- mino-2,6-dimethoxylepidine	70036	000613-59- 000723-98- 074509-65-	8 55
61	67.742	3.22 C: Hep Tet	\Database\NIST05a.L tadecane ratetracontane ratriacontane	85524 188836	000629-78- 007098-22- 014167-59-	797 891

Mixture

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File :D:\Data\dr ruzinah\ALI KA13142\280916\Z.D

Operator : FIZA

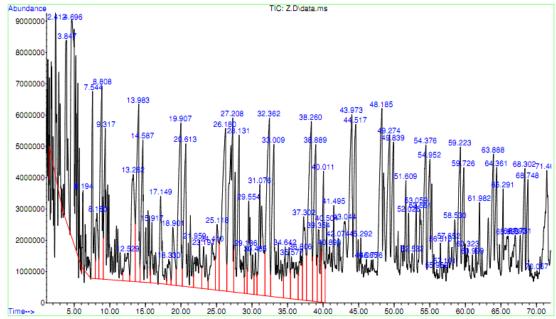
Acquired : 29 Sep 2016 10:24 using AcqMethod LIQUID FUEL.M

Instrument : GCMSD

Sample Name: 2

Wisc Info :

Vial Number: 2
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1	2.412	Tol Tol	\Database\NIST05a.L uene uene uene	2400	000108-88-3 000108-88-3 000108-88-3	3 94
2	3.843	2,4 2,4	\Database\NIST05a.L -Dimethyl-1-heptene -Dimethyl-1-heptene leptene, 5-methyl-	11183	019549-87-2 019549-87-2 013151-04-7	2 90
3	4.698	1,3 Sty	\Database\NIST05a.L ,5,7-Cyclooctatetraene rrene syclo[4.2.0]octa-1,3,5-triene	4752	000629-20-9 000100-42-5 000694-87-1	5 96
4	6.193	Ben Ben	\Database\NIST05a.L zaldehyde zaldehyde zaldehyde	4936	000100-52-7 000100-52-7 000100-52-7	93
5	7.539	.al .al	\Database\NIST05a.L phaMethylstyrene phaMethylstyrene phaMethylstyrene	8693	000098-83-9 000098-83-9 000098-83-9	93
6	8.180	Cyc 1,1	\Database\NIST05a.L lodecene 1-Dodecadiene looctene, 3-methyl-	33507	003618-12-0 005876-87-9 013152-05-1	9 52
7	8.810	1-D 1-D	∖Database\NIST05a.L ecene ecene ecene	17320	000872-05-9 000872-05-9 000872-05-9	9 97
8	9.312	Dec	\Database\NIST05a.L ane ane ane	18485	000124-18-5 000124-18-5 000124-18-5	5 95
9	12.527	Bic thy 1,7	\Database\NIST05a.L yclo[3.1.1]heptane, 2,6,6-trime - -Nonadiene, 4,8-dimethyl- yclo[2.2.2]octane, 2-methyl-	24404	000473-55-2 062108-28-5 000766-53-0	5 64
10	13.265	Cyc Cyc	\Database\NIST05a.L lopentane, propyl- lopentane, propyl- leptene, 2-methyl-, (E)-	6511	002040-96-2 002040-96-2 000692-96-6	2 52
11	13.980	$1 - 0 \\ 1 - 0$	\Database\NIST05a.L Indecene Indecene Indecene, (Z)-	25904	000821-95-4 000821-95-4 000821-97-€	93
12	14.589	Und	\Database\NIST05a.L lecane lecane		001120-21-4 001120-21-4	

₽k#	RT	Area%	Library/ID	Ref#	CAS# Q	ual
		Те	tradecane	55974	000629-59-4	90
13	15.914	Et Cy	:\Database\NIST05a.L hanone, 1-cyclohexy1- clohexanone, 2,3-dimethy1- ran, 2,3-dihydro-3-methy1-	11061	000823-76-7 013395-76-1 001708-27-6	38
14	17.153	2- Cy 4-	:\Database\NIST05a.L Isopropeny1-5-methy1hex-4-enal clopropanemethanol, 2-methy1-2-(methy1-3-penteny1)- 11-Dimethy1-2,6,10-dodecatrien-1 1	34921	075697-98-2 098678-70-7 1000196-53-3	40
15	18.328	2, 3,	:\Database\NIST05a.L 7-Octadiene, 4-methyl- 4-Octadiene, 7-methyl- cloundecene, 1-methyl-	10330	1000061-78-0 037050-05-8 088828-82-4	60
16	18.905	9- 1,	:\Database\NIST05a.L Eicosyne 11-Dodecadiene Z-2,13-Octadecadien-1-ol	33507	071899-38-2 005876-87-9 1000131-10-0	90
17	19.909	$\frac{1}{1}$:\Database\NIST05a.L Dodecene Dodecene Undecanol	34944	000112-41-4 000112-41-4 000112-42-5	94
18	20.614	Do Do	:\Database\NIST05a.L decane decane decane decane	36429	000112-40-3 000112-40-3 000112-40-3	95
19	21.960	Be Be	:\Database\NIST05a.L nzene, cyclohexyl- nzene, (3-methylcyclopentyl)- nzene, cyclohexyl-	29537	000827-52-1 005078-75-1 000827-52-1	42
20	23.188	Be No Na	:\Database\NIST05a.L nzene, (3-methylcyclopentyl)- nane, 4,5-dimethyl- phthalene, 2-ethyl-1,2,3,4-tetra dro-	27253	005078-75-1 017302-23-7 032367-54-7	35
21	24.406	4- Pe	:\Database\NIST05a.L Isopropylcyclohexanone ntane, 3-methylene- ntane, 3-methylene-	1466	005432-85-9 000760-21-4 000760-21-4	38
22	25.122	$13 \\ 1 -$:\Database\NIST05a.L -Oxabicyclo[10.1.0]tridecane Octadecyne Pentadecyne	92239	000286-99-7 000629-89-0 000765-13-9	72
23	26.179	1 - 1 - 1 - 1	:\Database\NIST05a.L Tridecene Tridecene Tridecene	44614	002437-56-1 002437-56-1 002437-56-1	97

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24	27.204	Cyc 2-U Cyc	:\Database\NIST05a.L clohexane, 1,2,4-trimethyl- Undecene, 4-methyl- clohexane, 1,3,5-trimethyl-, (1. pha.,3.alpha.,5.beta.)-	34999	002234-75-5 091695-32-8 001795-26-2	43
25	28.134	4-3 Cyc	:\Database\NIST05a.L Isopropyl-1,3-cyclohexanedione clohexane, 1,1-dimethyl-2-propyl xane, 2,3,4-trimethyl-	25982	062831-62-3 081983-71-3 000921-47-1	49
26	29.138	Tr: 1 (7-1	:\Database\NIST05a.L ichloroacetic acid, undec-10-eny ester Fetradecyne 13-Tetradecadiene	52910	1000280-51- 035216-11-6 021964-49-8	49
27	29.555	Ber y1 4- Ber	:\Database\NIST05a.L nzene, (3-methyl-1-methylenepent)- (para-Tolyl)-butyric acid nzenepropanoic acid, 3-phenylpro l ester	41409	074810-69-8 004521-22-6 060045-27-4	64
28	30.484	5-1 Cyc	:\Database\NIST05a.L Phenethyl-2H-pyrazol-3-ol clopropylphenylmethane nzenepropanenitrile	13603	1000311-62- 001667-00-1 000645-59-0	27
29	31.071	Tr: 6-1	:\Database\NIST05a.L iallylsilane Dodecene, (E)- cane, 3-cyclohexyl-	34957	001116-62-7 007206-17-9 013151-74-1	35
30	32.364	2-1 1-1	:\Database\NIST05a.L Tetradecene, (E)- Tetradecene Tetradecene	54512	035953-53-8 001120-36-1 001120-36-1	96
31	33.005	Tet	:\Database\NIST05a.L tradecane tradecane tradecane	55972	000629-59-4 000629-59-4 000629-59-4	97
32	34.639	17- 2,5 dre Cyc	:\Database\NIST05a.L -Pentatriacontene 5-Cyclohexadiene-1,4-dione, 3-hy pxy-2-methyl-5-(1-methylethyl)- clopropanemethanol, 2-methyl-2-(42794	006971-40-0 004586-58-7 098678-70-7	35
33	35.579	0.81 C ci: 1-0 lol	methyl-3-pentenyl)- :\Database\NIST05a.L s-11-Hexadecenal Cyclopentyl-4-(1-methylethyl)cyc hexane Pentadecyne	52948	053939-28-9 1000215-44- 000765-13-9	4 46
34	36.808	0.52 C	:\Database\NIST05a.L			

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		Benzene,	1,1'-(1,2-ethanediyl)bis- 1,1'-(1,2-ethanediyl)bis- 1,1'-(1,2-ethanediyl)bis-	44684	000103-29-7 000103-29-7 000103-29-7	7 55
35	37.299	1-Pentad cis-11-T	base\NIST05a.L ecyne etradecen-1-ol decadiene	65996	000765-13-9 034010-15-6 021964-48-7	5 93
36	38.260	1-Pentad 1-Pentad		64456	013360-61-7 013360-61-7 007206-25-9	7 91
37	38.891	1.41 C:\Data Pentadec Pentadec Pentadec	ane	66067	000629-62-9 000629-62-9 000629-62-9	9 96
38	39.350	1-Undece	base\NIST05a.L ne, 8-methyl- acetic acid, heptadecyl es ecene	159590	074630-40-3 1000282-98- 006765-39-5	-2 60
39	40.012	Cyclohex Bacchotr	base\NIST05a.L ane, 1,2,4-trimethyl- icuneatin c oropropionic acid, heptade r	148777	002234-75-5 066563-30-2 1000283-04-	2 50
40	40.504	Cyclohex Cyclohex	base\NIST05a.L ane, 1,2,4-trimethyl- ane, 1,2,4-trimethyl- thyl-3-heptene trans	11235	002234-75-5 002234-75-5 019550-75-5	5 55
41	40.899	Heptaflu cyl este Cyclopen	base\NIST05a.L orobutyric acid, n-pentade r tane, 1-buty1-2-propy1- ane, methy1-	35063	1000216-79- 062199-50-2 001502-38-1	2 53
42	41.497	6-Tridec Cyclohex	base\NIST05a.L ene, 7-methyl- ane, 1,2,4-trimethyl- ane, 1,1,2-trimethyl-	11237	024949-42-6 002234-75-5 007094-26-0	5 46
43	42.074	Oxirane, -, cis-(Bicyclo[3.1.1]heptan-3-one, 2,6,6- l-, (1.alpha.,2.beta.,5.al	24332	057457-72-4 015358-88-0 074646-37-0	50
44	43.046	1.03 C:\Data 1,19-Eic 1,19-Eic	- base\NIST05a.L osadiene	110851 110850	014811-95-1 014811-95-1 056683-54-6	83 81

₽k∦	RT	Area%	Library/ID	Ref#	CAS#	Qual
45	43.975	1-H Z-8	:\Database\NIST05a.L Hexadecene 3-Hexadecene Hexadecene	74523	000629-73- 1000130-8 000629-73-	7-5 96
46	44.520	Hea	:\Database\NIST05a.L kadecane kadecane kadecane	76093	000544-76- 000544-76- 000544-76-	-3 97
47	45.289	Cyc ene 1,1	<pre>\Database\NIST05a.L clohexane, 1,1'-(1-methylethylid e)bis- l'-Bicyclohexyl, 2-ethyl-, cis- clohexane, 1,2-diethyl-1-methyl-</pre>	52936	054934-90- 050991-12- 061141-79-	-3 43
48	46.069	Ber 1,3 Ber her Ber	<pre>\Database\NIST05a.L bzene, 1,1'-(3-methyl-1-propenediyl)bis- bzene, 1,1'-(1,2-dimethyl-1,2-et bediyl)bis-, (Z)- bzene, 1,1'-(1,2-dimethyl-1,2-et bediyl)bis-, (E)-</pre>	63119	007614-93- 000782-05- 000782-06-	-8 52
49	46.774	7-F Thi ior	:\Database\NIST05a.L Hexadecenal, (Z)- ieno[2,3-d]-1,3-thiaselenol-2-th he Dodecanol, 3,7,11-trimethyl-	84091	056797-40- 081803-09- 006750-34-	-0 56
50	48.184	N-H Ber	:\Database\NIST05a.L Benzyl-1H-benzimidazole bzene, 3-butynyl- bzene, (3-nitropropyl)-	12680	004981-92- 016520-62- 022818-69-	-0 22
51	49.273	3-H E-1	:\Database\NIST05a.L Heptadecene, (Z)- L4-Hexadecenal Heptadecene	83987	1000141-6 330207-53- 006765-39-	-9 99
52	49.840	Нер Нер	:\Database\NIST05a.L >tadecane >tadecane >tadecane	85525	000629-78- 000629-78- 000629-78-	-7 96
53	51.613	Cyc Hey Cyc	:\Database\NIST05a.L clohexane, 1,2,4-trimethyl- kadecane clohexane, 1,1,3,5-tetramethyl-, is-	76092	002234-75- 000544-76- 050876-32-	-3 35
54	52.029	Cyc Cyc Bio	:\Database\NIST05a.L clopentane, (2-methylbutyl)- clohexane, 1-ethyl-2-propyl- cyclo[3.1.1]heptan-3-one, 6,6-di chyl-2-(2-methylpropyl)-	25967	053366-38- 062238-33- 1000163-91	-9 38
		0 00 0	Detel			

55 52.531 0.39 C:\Database\NIST05a.L

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		1	-Methyl-Z-4-tetradecene -Decanol, 2-hexyl- yclopentane, 1-pentyl-2-propyl-	86865	1000130-78-3 64 002425-77-6 60 062199-51-3 60
56	53.055	3 C	C:\Database\NIST05a.L -Trifluoroacetoxy-6-ethyldecane yclohexane, 1,2,4-trimethyl- ecane, 1,1'-oxybis-	11235	116436-59-0 43 002234-75-5 43 002456-28-2 30
57	53.664	$\frac{1}{Z}$	C:\Database\NIST05a.L ,19-Eicosadiene ,Z-2,15-Octadecedien-1-ol acetate ,19-Eicosadiene	129818	014811-95-1 74 1000130-95-1 70 014811-95-1 64
58	54.379	E 1	C:\Database\NIST05a.L -15-Heptadecenal -Octadecene -Nonadecene	93544	1000130-97-9 99 000112-88-9 98 018435-45-5 95
59	54.956	0	C:\Database\NIST05a.L ctadecane ctadecane 0-Methylnonadecane	94931	000593-45-3 97 000593-45-3 96 056862-62-5 91
60	55.960	2 9	C:\Database\NIST05a.L -Tetradecene, (E)- -Octadecene, (E)- -Octadecene, (E)-		035953-53-8 70 007206-25-9 62 007206-21-5 62
61	56.505	2 t 2 1	C:\Database\NIST05a.L ,4-Dimethylhexanedioic acid, 6-me hyl ester ,2-Dimethyl-3-heptene trans -Cyclohexyl-1-(4-ethylcyclohexyl) thane	11219	1000187-74-2 35 019550-75-5 35 002027-13-6 35
62	57.103	C	C:\Database\NIST05a.L yclohexane, 1,1'-propylidenebis- ecane, 4-cyclohexyl- yclopentane, (2-methylpropyl)-	74535	054934-91-7 58 013151-75-2 55 003788-32-7 53
63	57.648	C 11 6 0	C:\Database\NIST05a.L yclopropanecarboxylic acid, 2-phe ylethyl ester -Methyl-3-nitro-6,7-dihydro-9H-5- xa-9-azabenzocyclohepten-8-one henyl ethyl tiglate	72205	1000245-59-4 27 134076-63-4 20 055719-85-2 18
64	58.535	1 1	C:\Database\NIST05a.L ,19-Eicosadiene ,19-Eicosadiene ,E-2,13-Octadecadien-1-ol	110850	014811-95-1 96 014811-95-1 91 1000131-10-3 86
65	59.218	\mathbf{z}	C:\Database\NIST05a.L -5-Nonadecene -Nonadecene -14-Hexadecenal	102860	1000131-11-8 99 018435-45-5 95 330207-53-9 95
		1 00			

66 59.731 1.39 C:\Database\NIST05a.L

₽k∦	RT	Area%	Library/ID	Ref#	CAS∉ Qual
		No	onadecane onadecane ept adecane	104271	000629-92-5 96 000629-92-5 96 000629-78-7 91
67	60.319	I: 	C:\Database\NIST05a.L soquinoline, 1,2,3,4-tetrahydro-1 ally1-6,7-dimethoxy-3,3-dimethy1- H-Pyrazole, 3,5-dipheny1- aphthalene, 1-phenoxy-	71299	180461-39-6 25 001145-01-3 25 003402-76-4 25
68	61.002	0.58 (Ti Z: 3- (1 B:	C:\Database\NIST05a.L riallylsilane inc, bis[2-(1,1-dimethylethyl)-3, -dimethylcyclopropyl]-, [1.alpha. lR*,2R*),2.beta.]- icyclo[2.2.1]heptane-2,5-dione, 1	25058 133356	001116-62-7 53 074793-36-5 47 004230-32-4 43
69	61.985	3.18 (Cy Cy	7,7-trimethyl- C:\Database\NIST05a.L yclohexane, 1,1,2-trimethyl- yclohexane, 1,1,3,5-tetramethyl-, cis- yclooctane, ethyl-	17447	007094-26-0 38 050876-32-9 30 013152-02-8 30
70	63.886	Cy E-	C:\Database\NIST05a.L ycloeicosane -15-Heptadecenal -Nonadecene	93518	000296-56-0 95 1000130-97-9 95 018435-45-5 94
71	64.356	E: He	C:\Database\NIST05a.L icosane eptadecane icosane	85523	000112-95-8 99 000629-78-7 94 000112-95-8 94
72	65.296	1- 10 Cy	C:\Database\NIST05a.L -Cyclopentyl-4-(1-methylethyl)cyc ohexane yclooctane, 1-methyl-3-propyl- yclohexane, 2,4-diethyl-1-methyl-	35064	1000215-44-4 53 255885-37-1 47 061142-70-9 47
73	65.937	E- 9-	C:\Database\NIST05a.L -15-Heptadecenal -Tricosene, (Z)- -Tricosene, (Z)-	138119	1000130-97-9 97 027519-02-4 96 027519-02-4 96
74	66.995	He He	C:\Database\NIST05a.L eptadecane eptadecane exadecane, 2,6,10,14-tetramethyl-	85525	000629-78-7 92 000629-78-7 91 000638-36-8 90
75	67.732	$\frac{1}{2}$	C:\Database\NIST05a.L ,19-Eicosadiene Z)-14-Tricosenyl formate icyclo[10.8.0]eicosane, cis-	159805	014811-95-1 91 077899-10-6 90 1000155-82-2 64
76	68.298	Z- 1-	C:\Database\NIST05a.L -5-Nonadecene -Nonadecene D-Heneicosene (c,t)	102860	1000131-11-8 99 018435-45-5 97 095008-11-0 95

₽k⋕	RT	Area%	Library/ID	Ref#	CAS#	Qual
77	68.747	747 1.81 C:\Database\NIST05a.L				
		Hene	icosane	122435	000629-94-1	7 98
		Hene	icosane	122436	000629-94-1	7 96
		Hept	adecane	85523	000629-78-	7 95
78	70.061	0.74 C:\	Database\NIST05a.L			
		1-No	nadecene	102860	018435-45-5	5 83
		Isot	ridecanol-	57271	027458-92-0	0 68
		3-не	ptadecene, (Z)-	84042	1000141-67	-3 50
79	71.471	3.07 C:\	Database\NIST05a.L			
		Benz	onitrile, m-phenethyl-	62228	034176-91-5	5 25
		2-Pr	openoic acid, 3-[(phenylmethyl o]-, (E)-	52240	013831-01-3	1 22
			ene, (5-iodopentyl)-	107726	099858-37-4	1 12