

# Numerical solutions of free convection boundary layer flow on a solid sphere with Newtonian heating in a micropolar fluid

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**Abstract** In this paper, the problem of free convection boundary layer flow on a solid sphere in a micropolar fluid with Newtonian heating, in which the heat transfer from the surface is proportional to the local surface temperature, is considered. The transformed boundary layer equations in the form of partial differential equations are solved numerically using an implicit finite-difference scheme. Numerical solutions are obtained for the local wall temperature, the local skin friction coefficient, as well as the velocity, angular velocity and temperature profiles. The features of the flow and heat transfer characteristics for different values of the material or micropolar parameter  $K$ , the Prandtl number  $Pr$  and the conjugate parameter  $\gamma$  are analyzed and discussed.

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## Nomenclature

$a$  radius of the sphere  
 $h_s$  heat transfer parameter for Newtonian heating  
 $C_f$  skin friction coefficient  
 $f$  dimensionless stream function  
 $g$  acceleration due to gravity  
 $Gr$  Grashof number  
 $H$  angular velocity of micropolar fluid  
 $j$  microinertia density  
 $K$  material parameter of micropolar fluid  
 $k$  thermal conductivity  
 $Pr$  Prandtl number  
 $Re$  Reynolds number  
 $T$  fluid temperature  
 $T_\infty$  ambient temperature  
 $U_\infty$  free stream velocity  
 $u, v$  velocity components along the  $x$  and  $y$   
directions, respectively  
 $x, y$  Cartesian coordinates along the sphere and  
normal to it, respectively

## Greek Letters

$\beta$  thermal expansion coefficient  
 $\gamma$  conjugate parameter for Newtonian heating  
 $\mu$  dynamic viscosity  
 $\nu$  kinematic viscosity  
 $\theta$  dimensionless temperature  
 $\kappa$  vortex viscosity

- $\varphi$  spin gradient viscosity
- $\rho$  fluid density
- $\psi$  stream function

## 1 Introduction

The essence of the theory of micropolar fluid flow lies in the extension of the constitutive equation for Newtonian fluid, so that more complex fluids such as particle suspensions, liquid crystal, animal blood, lubrication and turbulent shear flows can be described by this theory. The theory of micropolar fluid was first proposed by Eringen [1]. Extensive review of the theory and applications can be found in the review article by Ariman et al. [2]. Nazar et al. [3, 4] studied the free convection boundary layer flow on a solid sphere in a viscous and micropolar fluid with constant wall temperature (CWT) and constant heat flux (CHF), respectively. Generally, in modelling the convective boundary layer flow problems, the boundary conditions that were usually applied are constant wall temperature or heat flux. However, the Newtonian heating (NH) conditions have been used only recently by Merkin [5] to study the free convection boundary layer over vertical surfaces with Newtonian heating. The asymptotic solution near the leading edge and the full numerical solution along the whole plate domain have been obtained numerically, whilst the asymptotic solution far downstream along the plate has been obtained analytically. On the other hand, the situation with Newtonian heating occurs in many important engineering devices, for example in heat exchanger where the conduction in solid tube wall is greatly influenced by the convection in the fluid flowing over it. Further, for conjugate heat transfer around fins where the conduction within the fin and the convection in the fluid surrounding it must be simultaneously analyzed in order to obtain the vital design information and also in convection flows set up when the bounding surfaces absorb heat by solar radiation (see Chaudhary and Jain [6]).

Recent demands in heat transfer engineering have requested researchers to develop various new types of heat transfer equipments with superior performance, especially compact and light-weight ones. Increasing the need for small-size units, focuses have been cast on the effects of the interaction between developments of the thermal boundary layers in both fluid streams, and of axial wall conduction, which usually affects the heat exchanger performance. Since the early paper

by Luikov et al. [7], many contributions to the topic of conjugate heat transfer have been produced. Excellent reviews of the topics of conjugate heat transfer problems can be found in the book by Martynenko and Khramtsov [8] and the review paper by Kimura et al. [9]. Recently, Salleh et al. [10–14] and Merkin et al. [15] considered the forced convection boundary layer flow at a forward stagnation point, free, mixed and forced convection boundary layer flows on a sphere, horizontal circular cylinder and stretching sheet with Newtonian heating, respectively. These problems have been extended to viscous and micropolar fluids by many investigators such as [16–20] in various ways either with constant wall temperature and concentration, constant heat and mass fluxes or with heat generation.

Therefore, the aim of the present paper is to study the free convection boundary layer flow on a solid sphere with Newtonian heating in a micropolar fluid. The full governing boundary layer equations are first transformed into a system of non-dimensional equations via the non-dimensional variables, and then into non-similar partial differential equations before they are solved numerically by the Keller-box method, an implicit finite-difference scheme as described in the book by and Cebeci and Bradshaw [21]. Results are presented for the local wall temperature, the local skin friction coefficient, as well as the velocity, angular velocity and temperature profiles.

## 2 Mathematical model

Consider a heated sphere of radius  $a$ , which is immersed in a viscous and incompressible micropolar fluid of ambient temperature  $T_\infty$ . The surface of the sphere is subjected to a Newtonian heating (NH). We assume that the equations are subjected to a Newtonian heating of the form proposed by Merkin [5]. Under the Boussinesq and boundary layer approximations, the basic equations are (see Eringen [1], Nazar et al. [3, 4])

$$\begin{aligned} \frac{\partial}{\partial \bar{x}}(\bar{r}\bar{u}) + \frac{\partial}{\partial \bar{y}}(\bar{r}\bar{v}) &= 0, \\ \rho \left( \bar{u} \frac{\partial \bar{u}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{u}}{\partial \bar{y}} \right) &= (\mu + \kappa) \frac{\partial^2 \bar{u}}{\partial \bar{y}^2} + \rho g \beta (T - T_\infty) \sin\left(\frac{\bar{x}}{a}\right) + \kappa \frac{\partial \bar{H}}{\partial \bar{y}}, \end{aligned} \tag{1}$$

$$\rho j \left( \bar{u} \frac{\partial \bar{H}}{\partial \bar{x}} + \bar{v} \frac{\partial \bar{H}}{\partial \bar{y}} \right) = -\kappa \left( 2\bar{H} + \frac{\partial \bar{u}}{\partial \bar{y}} \right) + \varphi \frac{\partial^2 \bar{H}}{\partial \bar{y}^2}, \quad (3)$$

$$\bar{u} \frac{\partial T}{\partial \bar{x}} + \bar{v} \frac{\partial T}{\partial \bar{y}} = \frac{\nu}{Pr} \frac{\partial^2 T}{\partial \bar{y}^2}, \quad (4)$$

where  $\bar{r}(\bar{x}) = a \sin(\bar{x}/a)$  and we assume that  $\varphi = (\mu + (\kappa/2))j$ . The boundary conditions of (1)–(4) are

$$\begin{aligned} \bar{u} = \bar{v} = 0, \quad \frac{\partial T}{\partial \bar{y}} = -h_s T, \\ \bar{H} = -n \frac{\partial \bar{u}}{\partial \bar{y}} \quad \text{at } \bar{y} = 0, \end{aligned} \quad (5)$$

$$\bar{u} \rightarrow 0, \quad T \rightarrow T_\infty, \quad \bar{H} \rightarrow 0 \quad \text{as } \bar{y} \rightarrow \infty,$$

where  $\bar{u}$  and  $\bar{v}$  are the velocity components along the  $\bar{x}$  and  $\bar{y}$  directions, respectively,  $T$  is the local temperature,  $\rho$  is the fluid density,  $g$  is the gravity acceleration,  $\beta$  is the thermal expansion coefficient,  $\nu = \frac{\mu}{\rho}$  is the kinematic viscosity,  $\mu$  is the dynamic viscosity,  $\kappa$  is the vortex viscosity,  $\bar{H}$  is the angular velocity of micropolar fluid,  $j$  is the microinertia density,  $\varphi$  is the spin gradient viscosity,  $Pr$  is the Prandtl number and  $h_s$  is a heat transfer parameter for Newtonian heating.

It is worth mentioning that in boundary conditions (5),  $n$  is a constant and  $0 \leq n \leq 1$ . The value  $n = 0$ , which indicates  $\bar{H} = 0$  at the wall, represents concentrated particle flows in which the particle density is sufficiently great that microelements close to the wall are unable to rotate or it is called “strong” concentration of microelements [22, 23]. The case corresponding to  $n = \frac{1}{2}$  results in the vanishing of antisymmetric part of the stress tensor and represents “weak” concentration of microelements [24]. In this case, the particle rotation is equal to fluid vorticity at the boundary for fine particle suspension. When  $n = 1$ , we have flows which are representative of turbulent boundary layer [25]. The case of  $n = \frac{1}{2}$  is considered in the present study, in order to compare some results with those of Nazar et al. [3, 4] for the CWT and CHF cases in viscous fluids, respectively, who also considered the case of  $n = \frac{1}{2}$  (refer [11]). It is worth mentioning that the correct boundary condition to be applied to the spin is still an open question. However, the most common boundary conditions used in the literature are the vanishing of the spin on the boundary, the so-called strong interaction ( $n = 0$ ) and the opposite extreme, the weak interaction ( $n = \frac{1}{2}$ ), which is the vanishing of the momentum stress on the boundary [23].

We introduce now the following non-dimensional variables (Nazar et al. [3]):

$$\begin{aligned} x = \frac{\bar{x}}{a}, \quad y = Gr^{1/4} \left( \frac{\bar{y}}{a} \right), \quad r = \frac{\bar{r}}{a}, \\ u = \left( \frac{a}{\nu} \right) Gr^{-1/2} \bar{u}, \quad v = \left( \frac{a}{\nu} \right) Gr^{-1/4} \bar{v}, \quad (6) \\ H = \left( \frac{a^2}{\nu} \right) Gr^{-3/4} \bar{H}, \quad \theta = \frac{T - T_\infty}{T_\infty}, \end{aligned}$$

where  $Gr = \frac{g\beta T_\infty a^3}{\nu^2}$  is the Grashof number for Newtonian heating (NH). The microinertia density  $j$  is taken to be  $j = a^2 Gr^{-1/2}$ . Substituting variables (6) into (1)–(4) then become

$$\frac{\partial}{\partial x}(ru) + \frac{\partial}{\partial y}(rv) = 0 \quad (7)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = (1 + K) \frac{\partial^2 u}{\partial y^2} + \theta \sin x + K \frac{\partial H}{\partial y} \quad (8)$$

$$u \frac{\partial H}{\partial x} + v \frac{\partial H}{\partial y} = -K \left( 2H + \frac{\partial u}{\partial y} \right) + \left( 1 + \frac{K}{2} \right) \frac{\partial^2 H}{\partial y^2} \quad (9)$$

$$u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y} = \frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} \quad (10)$$

where  $K$  is the material or micropolar parameter defined as  $K = \frac{\kappa}{\mu}$ . The boundary conditions are

$$\begin{aligned} u = v = 0, \quad \frac{\partial \theta}{\partial y} = -\gamma(1 + \theta), \\ H = -\frac{1}{2} \frac{\partial u}{\partial y} \quad \text{at } y = 0 \end{aligned} \quad (11)$$

$$u \rightarrow 0, \quad \theta \rightarrow 0, \quad H \rightarrow 0 \quad \text{as } y \rightarrow \infty$$

where  $\gamma = ah_s Gr^{-1/4}$  represents the conjugate parameter for Newtonian heating. We notice that (11) gives  $\theta = 0$  when  $\gamma = 0$ , corresponding to having  $h_s = 0$  and hence no heating from the sphere exists (see Salleh et al. [11, 12]). To solve (7) to (10), subjected to the boundary conditions (11), we assume the following variables:

$$\begin{aligned} \psi = xr(x)f(x, y), \quad \theta = \theta(x, y), \\ H = xh(x, y) \end{aligned} \quad (12)$$

where  $\psi$  is the stream function defined as

$$u = \frac{1}{r} \frac{\partial \psi}{\partial y} \quad \text{and} \quad v = -\frac{1}{r} \frac{\partial \psi}{\partial x} \quad (13)$$

which satisfies the continuity equation (7). Thus, (8) to (10) then become

$$(1 + K) \frac{\partial^3 f}{\partial y^3} + \left(1 + \frac{x}{\sin x} \cos x\right) f \frac{\partial^2 f}{\partial y^2} - \left(\frac{\partial f}{\partial y}\right)^2 + \frac{\sin x}{x} \theta + K \frac{\partial h}{\partial y} = x \left(\frac{\partial f}{\partial y} \frac{\partial^2 f}{\partial x \partial y} - \frac{\partial f}{\partial x} \frac{\partial^2 f}{\partial y^2}\right), \tag{14}$$

$$\left(1 + \frac{K}{2}\right) \frac{\partial^2 h}{\partial y^2} + \left(1 + \frac{x}{\sin x} \cos x\right) f \frac{\partial h}{\partial y} - \frac{\partial f}{\partial y} h - K \left(2h + \frac{\partial^2 f}{\partial y^2}\right) = x \left(\frac{\partial f}{\partial y} \frac{\partial h}{\partial x} - \frac{\partial f}{\partial x} \frac{\partial h}{\partial y}\right), \tag{15}$$

$$\frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} + \left(1 + \frac{x}{\sin x} \cos x\right) f \frac{\partial \theta}{\partial y} = x \left(\frac{\partial f}{\partial y} \frac{\partial \theta}{\partial x} - \frac{\partial f}{\partial x} \frac{\partial \theta}{\partial y}\right), \tag{16}$$

subject to the boundary conditions

$$f = \frac{\partial f}{\partial y} = 0, \quad \frac{\partial \theta}{\partial y} = -\gamma(1 + \theta),$$

$$h = -\frac{1}{2} \frac{\partial^2 f}{\partial y^2} \quad \text{at } y = 0 \tag{17}$$

$$\frac{\partial f}{\partial y} \rightarrow 0, \quad \theta \rightarrow 0, \quad h \rightarrow 0 \quad \text{as } y \rightarrow \infty$$

At the lower stagnation point of the sphere,  $x \approx 0$ , (14) to (16) reduce to the following ordinary differential equations:

$$(1 + K) f''' + 2ff'' - f'^2 + \theta + Kh' = 0 \tag{18}$$

$$\left(1 + \frac{K}{2}\right) h'' + 2fh' - f'h - K(2h + f'') = 0 \tag{19}$$

$$\frac{1}{Pr} \theta'' + 2f\theta' = 0 \tag{20}$$

and the boundary conditions become

$$f(0) = f'(0) = 0, \quad \theta'(0) = -\gamma(1 + \theta(0)),$$

$$h(0) = -\frac{1}{2} f''(0) \quad \text{at } y = 0, \tag{21}$$

$$f' \rightarrow 0, \quad \theta \rightarrow 0, \quad h \rightarrow 0 \quad \text{as } y \rightarrow \infty$$

where primes denote differentiation with respect to  $y$ . The physical quantities of interest in this problem are the local skin friction coefficient,  $C_f$  and the local wall temperature,  $\theta_w(x)$ , which are given by (when  $\gamma = 1$ )

$$C_f = \left(1 + \frac{K}{2}\right) x \frac{\partial^2 f}{\partial y^2}(x, 0), \tag{22}$$

$$\theta_w(x) = -1 - \frac{\partial \theta}{\partial y}(x, 0)$$

where  $C_f = \tau_w/(\rho U_\infty^2)$  is the skin friction coefficient and  $\tau_w = [(\mu + \kappa)(\partial \bar{u}/\partial \bar{y}) + \kappa \bar{H}]_{\bar{y}=0}$  is the wall shear stress.

At the lower stagnation point of the sphere,  $x \approx 0$ , the skin friction coefficient and the wall temperature are measured by  $f''(0)$  and  $\theta(0)$ , respectively.

### 3 Solution procedure

Equations (14) to (16) subject to boundary conditions (17) are solved numerically using the Keller-box method as described in the book by Cebeci and Bradshaw [21]. The solution is obtained by the following four steps:

- reduce (14) to (16) to a first-order system,
- write the difference equations using central differences,
- linearize the resulting algebraic equations by Newton’s method, and write them in the matrix-vector form,
- solve the linear system by the block tridiagonal elimination technique.

The step size  $\Delta y$  in  $y$ , and the edge of the boundary layer  $y_\infty$  had to be adjusted for different values of parameters to maintain accuracy.

### 4 Results and discussion

Equations (14) to (16) subject to the boundary conditions (17) are solved numerically using the Keller-box method for the case of Newtonian heating (NH) with four parameters considered, namely the material parameter  $K$ , the Prandtl number  $Pr$ , the conjugate parameter  $\gamma$  and the coordinate running along the surface of the sphere,  $x$ . The numerical solution starts at the lower stagnation point of the sphere,  $x \approx 0$ , and proceeds round the sphere up to the point  $x = 120^\circ$ . Values of  $K$  considered are  $K = 0$  (Newtonian fluid), 1, 2 and 3 (micropolar fluid) and values of  $Pr$  considered are  $Pr = 0.7, 1$  and 7 at different positions  $x = 0^\circ, 10^\circ, 20^\circ, 30^\circ, 40^\circ, 50^\circ, 60^\circ, 70^\circ, 80^\circ, 90^\circ, 100^\circ, 110^\circ$ , and  $120^\circ$ . It is worth mentioning that small values of  $Pr (\ll 1)$  physically correspond to liquid metals, which have high thermal conductivity but low viscosity, while large values of  $Pr (\gg 1)$  correspond to high-viscosity oils. It is worth pointing out that specifically, Prandtl number  $Pr = 0.7, 1.0$  and  $7.0$  correspond

to air, electrolyte solution such as salt water and water, respectively.

The values of the skin friction coefficient and the wall temperature in a Newtonian fluid ( $K = 0$ ) and  $\gamma = 1$  are shown in Table 1. In order to verify the accuracy of the present method, the present results are compared with those reported by Salleh et al. [12]. It is found that the agreement between the previously published results with the present ones is very good. We can conclude that this method works efficiently for the present problem and we are also confident that the results presented here are accurate.

Tables 2 and 3 present the values of the wall temperature,  $\theta(0)$  and the skin friction coefficient,  $f''(0)$

**Table 1** Values of the skin friction coefficient  $f''(0)$  and the wall temperature  $\theta(0)$  at the lower stagnation point of the sphere,  $x \approx 0$ , when  $Pr = 0.7, 1$  and  $7, K = 0$  (Newtonian fluid) and  $\gamma = 1$

| $Pr$ | $f''(0)$           |         | $\theta(0)$        |         |
|------|--------------------|---------|--------------------|---------|
|      | Salleh et al. [12] | Present | Salleh et al. [12] | Present |
| 0.7  | 8.9610             | 8.9609  | 26.4590            | 26.4584 |
| 1    | 6.1411             | 6.1409  | 17.2876            | 17.2861 |
| 7    | 1.2487             | 1.2489  | 3.3635             | 3.3651  |

**Table 2** Values of the wall temperature  $\theta(0)$  at the lower stagnation point of the sphere,  $x \approx 0$ , for various values of  $K$  when  $Pr = 0.7, 1$  and  $7$  and  $\gamma = 1$

| $Pr$ | $\theta(0)$ |         |         |
|------|-------------|---------|---------|
|      | 0.7         | 1       | 7       |
| $K$  | Present     | Present | Present |
| 0    | 26.4584     | 17.2861 | 3.3651  |
| 1    | 38.3841     | 25.2867 | 4.6309  |
| 2    | 49.1395     | 32.4395 | 5.5150  |
| 3    | 59.3500     | 39.2872 | 6.4152  |

**Table 3** Values of the skin friction coefficient  $f''(0)$  at the lower stagnation point of the sphere,  $x \approx 0$ , for various values of  $K$  when  $Pr = 0.7, 1$  and  $7$  and  $\gamma = 1$

| $Pr$ | $f''(0)$ |         |         |
|------|----------|---------|---------|
|      | 0.7      | 1       | 7       |
| $K$  | Present  | Present | Present |
| 0    | 8.9609   | 6.1409  | 1.2489  |
| 1    | 7.4816   | 5.1336  | 0.9790  |
| 2    | 6.8457   | 4.6987  | 0.8600  |
| 3    | 6.4721   | 4.4437  | 0.7900  |

at the lower stagnation point of the sphere for various values of  $K$  when  $Pr = 0.7, 1$  and  $7$  and  $\gamma = 1$ , respectively. It is found that for fixed  $Pr$ , as  $K$  increases, the value of  $\theta(0)$  increases but  $f''(0)$  decreases. Also, it is found that for fixed  $K$ , as  $Pr$  increases, both  $\theta(0)$  and  $f''(0)$  decrease. From these tables, the values of  $\theta(0)$  are higher for micropolar fluid ( $K \neq 0$ ) than those for a Newtonian fluid ( $K = 0$ ) but the values of  $f''(0)$  are lower for micropolar fluid ( $K \neq 0$ ) than those for a Newtonian fluid ( $K = 0$ ).

Tables 4 to 7 present the values of the local wall temperature  $\theta_w(x)$  and the local skin friction coefficient  $C_f$  for various values of  $x$  when  $Pr = 0.7, 1$  and  $7, K = 0$  and  $1$  and  $\gamma = 1$ , respectively. It is found that, for fixed  $K$ , as  $Pr$  increases, both the  $\theta_w(x)$  and  $C_f$  decrease. From these tables, for a fixed  $Pr$ , as  $x$  increases, i.e. from the lower stagnation point of the sphere,  $x \approx 0$ , and proceeds round the sphere up to the point  $x = 120^\circ$ , both the values of  $\theta_w(x)$  and  $C_f$  increase. On the other hand, the values of  $\theta_w(x)$  and  $C_f$  are higher for micropolar fluid ( $K = 1$ ) than those for a Newtonian fluid ( $K = 0$ ).

The graphs of  $f''(x, 0)$  and  $\theta(x, 0)$  for some values of  $Pr$  when  $K = 1$  and  $\gamma = 1$  are plotted in Figs. 1 and 2, respectively. It is found that, as  $Pr$  increases, both  $f''(x, 0)$  and  $\theta(x, 0)$  decrease. For small values of  $Pr$  ( $\ll 1$ ) the difference value changing is higher than for large values of  $Pr$  ( $\gg 1$ ) and it is seen that the surface temperature is very sensitive to the Prandtl

**Table 4** Values of the local wall temperature,  $\theta_w(x)$  for various values of  $x$  when  $Pr = 0.7, 1$  and  $7, K = 0$  and  $\gamma = 1$

| $Pr$ | $\theta_w(x)$ |         |         |
|------|---------------|---------|---------|
|      | 0.7           | 1       | 7       |
| $x$  | Present       | Present | Present |
| 0°   | 26.4590       | 17.2876 | 3.3635  |
| 10°  | 56.8602       | 36.1847 | 5.4172  |
| 20°  | 59.4033       | 37.7239 | 5.5141  |
| 30°  | 61.1367       | 38.7087 | 5.5857  |
| 40°  | 62.7065       | 39.6506 | 5.6687  |
| 50°  | 64.3987       | 40.7060 | 5.7880  |
| 60°  | 66.2689       | 41.8821 | 5.9499  |
| 70°  | 68.5102       | 43.2987 | 6.1331  |
| 80°  | 71.1541       | 44.9755 | 6.3583  |
| 90°  | 74.2967       | 46.9734 | 6.6289  |
| 100° | 78.0623       | 49.3714 | 6.9555  |
| 110° | 82.6233       | 52.2792 | 7.3530  |
| 120° | 88.2340       | 55.8588 | 7.8427  |

**Table 5** Values of the local skin friction coefficient,  $C_f$  for various values of  $x$  when  $Pr = 0.7, 1$  and  $7, K = 0$  and  $\gamma = 1$

| $Pr$ | 0.7     | 1       | 7       |
|------|---------|---------|---------|
| $x$  | Present | Present | Present |
| 0°   | 0.0000  | 0.0000  | 0.0000  |
| 10°  | 2.8206  | 1.8939  | 0.2909  |
| 20°  | 5.7090  | 3.8817  | 0.5854  |
| 30°  | 8.7332  | 5.8418  | 0.8785  |
| 40°  | 11.5864 | 7.7431  | 1.1618  |
| 50°  | 14.3102 | 9.5616  | 1.4186  |
| 60°  | 16.7934 | 11.2211 | 1.6778  |
| 70°  | 19.1415 | 12.7925 | 1.9052  |
| 80°  | 21.2356 | 14.1966 | 2.1172  |
| 90°  | 23.0291 | 15.4035 | 2.3029  |
| 100° | 24.4695 | 16.3780 | 2.4569  |
| 110° | 25.4947 | 17.0803 | 2.5741  |
| 120° | 26.0269 | 17.4585 | 2.6466  |

**Table 7** Values of the local skin friction coefficient,  $C_f$  for various values of  $x$  when  $Pr = 0.7, 1$  and  $7, K = 1$  and  $\gamma = 1$

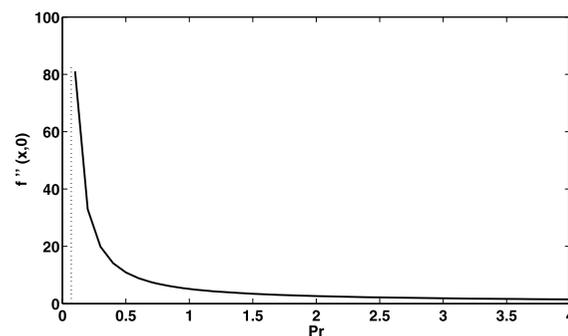
| $Pr$ | 0.7     | 1       | 7       |
|------|---------|---------|---------|
| $x$  | Present | Present | Present |
| 0°   | 0.0000  | 0.0000  | 0.0000  |
| 10°  | 3.7233  | 2.5231  | 0.3796  |
| 20°  | 7.6625  | 5.1853  | 0.7686  |
| 30°  | 11.5608 | 7.8181  | 1.1500  |
| 40°  | 15.2420 | 10.3761 | 1.5207  |
| 50°  | 18.9680 | 12.8203 | 1.8764  |
| 60°  | 22.2741 | 15.0547 | 2.2030  |
| 70°  | 25.4072 | 17.1748 | 2.5154  |
| 80°  | 28.2108 | 19.0749 | 2.7984  |
| 90°  | 30.6248 | 20.7150 | 3.0470  |
| 100° | 32.5814 | 22.0499 | 3.2546  |
| 110° | 34.0003 | 23.0267 | 3.4144  |
| 120° | 34.6476 | 23.5785 | 3.5171  |

**Table 6** Values of the local wall temperature,  $\theta_w(x)$  for various values of  $x$  when  $Pr = 0.7, 1$  and  $7, K = 1$  and  $\gamma = 1$

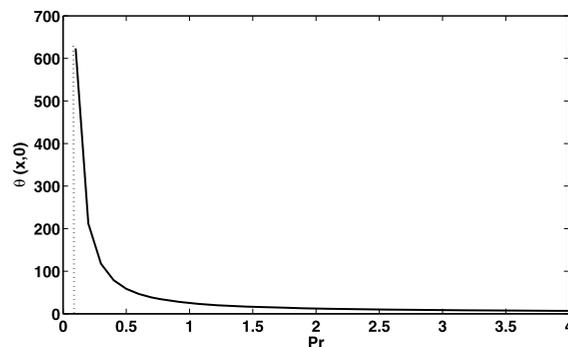
| $Pr$ | 0.7      | 1       | 7       |
|------|----------|---------|---------|
| $x$  | Present  | Present | Present |
| 0°   | 38.3841  | 25.2867 | 4.6309  |
| 10°  | 87.8744  | 56.9775 | 8.1822  |
| 20°  | 92.0951  | 59.5915 | 8.3870  |
| 30°  | 94.7977  | 61.2801 | 8.5329  |
| 40°  | 97.2352  | 62.8666 | 8.6958  |
| 50°  | 100.0066 | 64.5873 | 8.8945  |
| 60°  | 102.9836 | 66.4993 | 9.1265  |
| 70°  | 106.5506 | 68.7977 | 9.4142  |
| 80°  | 110.7602 | 71.5168 | 9.7615  |
| 90°  | 115.7666 | 74.7564 | 10.1802 |
| 100° | 121.7694 | 78.6456 | 10.6867 |
| 110° | 129.0451 | 83.3636 | 11.3034 |
| 120° | 135.5077 | 89.1734 | 12.0632 |

number variations. To get a physically acceptable solution,  $Pr$  must be greater than or equals to some critical value, say  $Pr_c$ , i.e.  $Pr \geq Pr_c$ , depending on  $\gamma$ . It can be seen from these figures that  $f''(x, 0)$  and  $\theta(x, 0)$  become large as  $Pr$  approaches the critical value  $Pr_c = 0.025$  when  $\gamma = 1$ .

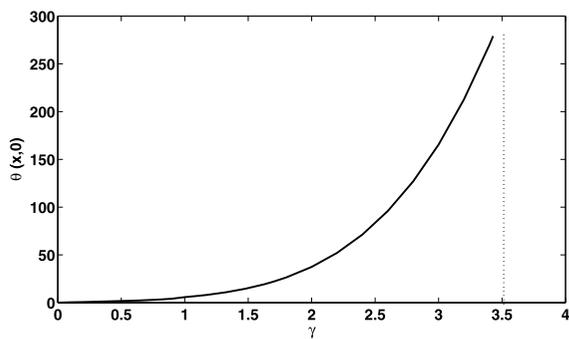
Figure 3 illustrates the variation of the wall temperature  $\theta(x, 0)$  with conjugate parameter  $\gamma$  when  $Pr = 7$  and  $K = 1$ . Also, to get a physically acceptable solu-



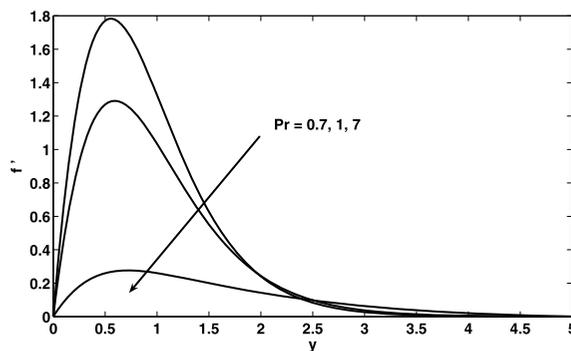
**Fig. 1** Graph of  $f''(x, 0)$  with Prandtl number  $Pr$  when  $K = 1$  and  $\gamma = 1$



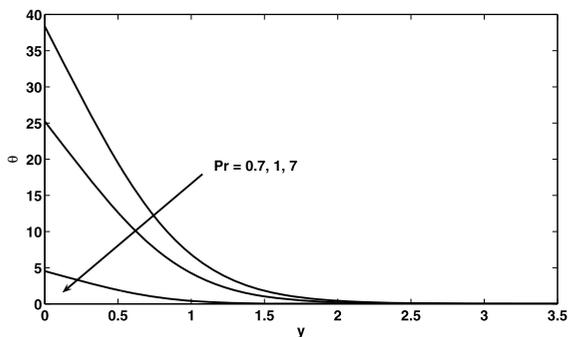
**Fig. 2** Graph of  $\theta(x, 0)$  with Prandtl number  $Pr$  when  $K = 1$  and  $\gamma = 1$



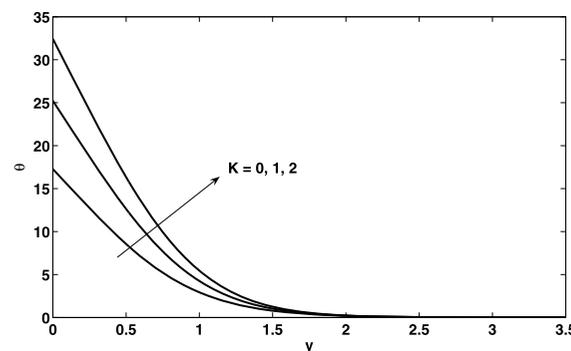
**Fig. 3** Variation of the wall temperature  $\theta(x, 0)$  with conjugate parameter  $\gamma$  when  $Pr = 7$  and  $K = 1$



**Fig. 5** Velocity profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $Pr = 0.7, 1$  and  $7, K = 1$  and  $\gamma = 1$



**Fig. 4** Temperature profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $Pr = 0.7, 1$  and  $7, K = 1$  and  $\gamma = 1$

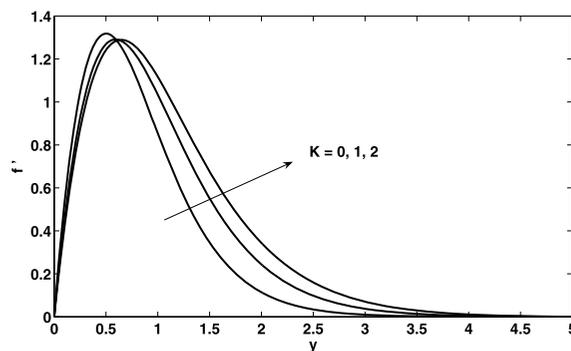


**Fig. 6** Temperature profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $K = 0, 1$  and  $2, Pr = 1$  and  $\gamma = 1$

tion,  $\gamma$  must be less than or equals to some critical value, say  $\gamma_c$ , i.e.  $\gamma \leq \gamma_c$ , depending on  $Pr$ . It can be seen from this figure that  $\theta(x, 0)$  becomes large as  $\gamma$  approaches the critical value  $\gamma_c = 3.5020$  when  $Pr = 7$  and  $K = 1$ .

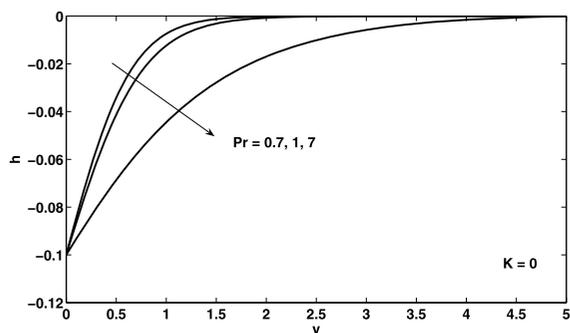
Figures 4 and 5 display the temperature and velocity profiles, respectively, near the lower stagnation point of the sphere when  $Pr = 0.7, 1$  and  $7, K = 1$  and  $\gamma = 1$ . From Fig. 4, it is found that as  $Pr$  increases, the temperature profiles decrease and also the thermal boundary layer thickness decreases. This is because for small values of the Prandtl number  $Pr (\ll 1)$ , the fluid is highly conductive. Physically, if  $Pr$  increases, the thermal diffusivity decreases and this phenomenon leads to the decreasing manner of the energy transfer ability that reduces the thermal boundary layer. On the other hand, from Fig. 5 it is shown that for fixed  $K$ , as  $Pr$  increases, the velocity profiles decrease.

Temperature and velocity profiles near the lower stagnation point of the sphere for some values of  $K$ , namely  $K = 0, 1$  and  $2$  when  $Pr = 1$  and  $\gamma = 1$  are

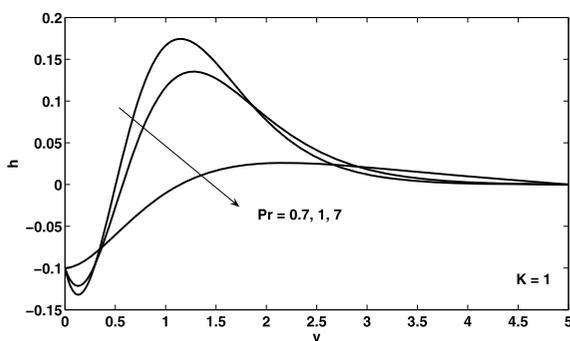


**Fig. 7** Velocity profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $K = 0, 1$  and  $2, Pr = 1$  and  $\gamma = 1$

plotted in Figs. 6 and 7, respectively. It is found that when  $Pr$  is fixed, as  $K$  increases, both the temperature and velocity profiles increase. Figures 8 and 9 display the angular velocity or microrotation profiles near the lower stagnation point of the sphere for some values of



**Fig. 8** Angular velocity profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $Pr = 0.7, 1$  and  $7$ ,  $K = 0$  and  $\gamma = 1$



**Fig. 9** Angular velocity profiles near the lower stagnation point of the sphere,  $x \approx 0$ , when  $Pr = 0.7, 1$  and  $7$ ,  $K = 1$  and  $\gamma = 1$

$Pr$ , namely  $Pr = 0.7, 1$  and  $7$  when  $K = 0$  and  $K \neq 0$  and  $\gamma = 1$ , respectively. These figures show that the angular velocity is completely negative for  $K = 0$ , while it may be positive for  $K = 1$  (or for other values of  $K \neq 0$ ). It is also noticed from these figures that as the material parameter  $K$  increases, the angular velocity profiles decrease.

## 5 Conclusions

In this paper, we have numerically studied the problem of free convection boundary layer flow on a sphere in a micropolar fluid with Newtonian heating. We are interested to see how the material parameter  $K$ , the Prandtl number  $Pr$  and conjugate parameter  $\gamma$  affect the flow and heat transfer characteristics. We can conclude that:

- when  $Pr$  and  $\gamma$  are fixed, as  $K$  increases, the temperature and velocity profiles increase, while when  $K$  and  $\gamma$  are fixed, as  $Pr$  increases, the temperature, velocity and angular velocity profiles decrease;

- when  $Pr$  and  $\gamma$  are fixed, the values of  $\theta_w$  and  $C_f$  are higher for micropolar fluids ( $K \neq 0$ ) than those for a Newtonian fluid ( $K = 0$ );
- when  $K$  and  $\gamma$  are fixed, as  $Pr$  increases, both the values of  $\theta_w$  and  $C_f$  decrease;
- to get a physically acceptable solution,  $Pr$  must be greater than  $Pr_c$  depending on  $\gamma$ , and also,  $\gamma$  must be less than  $\gamma_c$  depending on  $Pr$ .

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