

**STUDY ON THE KINETICS OF CATION  
EXCHANGE RESINS AS CATALYSTS IN  
FREE FATTY ACID (FFA) ESTERIFICATION  
OF SIMULATED USED COOKING OIL**

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## SUPERVISOR'S DECLARATION

We hereby declare that we have checked this thesis project and in our opinion, this thesis is adequate in terms of scope and quality for the award of the degree of Master of Science.

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I hereby declare that the work in this thesis is based on my original work except for quotations and citations which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at Universiti Malaysia Pahang or any other institutions.

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## LIST OF SYMBOLS

<i>TPA</i>	12-tungstophosphoric acid
<i>H<sub>3</sub>PW/ZrO<sub>2</sub></i>	12-tungstophosphoric acid supported on zirconia
<i>E<sub>a</sub></i>	Activation energy
<i>K<sub>A</sub></i>	Adsorption coefficient of FFA
<i>K<sub>B</sub></i>	Adsorption coefficient of methanol
<i>K<sub>C</sub></i>	Adsorption coefficient of esters
<i>K<sub>D</sub></i>	Adsorption coefficient of water
<i>Al</i>	Aluminium
<i>Al<sub>2</sub>O<sub>3</sub></i>	Aluminium oxide
$\text{\AA}$	Ångstrøm (0.1 nanometre)
<i>C<sub>AB</sub></i>	Bulk concentration of limiting reactant
<i>CaO</i>	Calcium oxide
<i>C</i>	Carbon
<i>CO<sub>2</sub></i>	Carbon dioxide
$\rho_b$	Catalyst density
<i>R<sub>c</sub></i>	Catalyst radius
<i>Cm</i>	Centimetre
<i>Ce</i>	Cerium
<i>Cs</i>	Caesium
<i>R<sup>2</sup></i>	Coefficient of determination
<i>M</i>	Concentration
<i>C<sub>A</sub></i>	Concentration of free fatty acid
<i>C<sub>C</sub></i>	Concentration of esters
<i>C<sub>HCl</sub></i>	Concentration of hydrochloric acid
<i>C<sub>B</sub></i>	Concentration of methanol
<i>C<sub>NaOH</sub></i>	Concentration of sodium hydroxide
<i>C<sub>V</sub></i>	Concentration of vacant sites on surface
<i>C<sub>D</sub></i>	Concentration of water
<i>C<sub>li</sub></i>	Concentration of the limiting reactant in mixture
<i>x</i>	Conversion
<i>cm<sup>3</sup></i>	Cubic centimetre

$^{\circ}C$	Degree celsius
$ID$	Diameter
$D_{eff}$	Effective diffusivity
$\Delta H$	Enthalphy
$\Delta S$	Entrophy
$K_{eq}$	Equilibrium constant
$Fe_2(SO_4)_2/C$	Ferric sulphate on carbon
$C_{NaOH\ final}$	Final concentration of sodium hydroxide
$k_f$	Forward rate constant
$R$	Gas constant
$g$	Gram
$h$	Hour/hours
$HF$	Hydrofluoric acid
$H$	Hydrogen
$H^+$	Hydrogen ion/ proton
$C_{NaOH\ initial}$	Initial concentration of sodium hydroxide
$V_{initial}$	Initial volume
$J$	Joule
$K$	Kelvin
$kJ$	Kilojoule
$kv$	Kilovolt
$La_2O_3$	Lanthanum oxide
$>$	Larger than
$<$	Less than
$L$	Litre
$MnO$	Manganese oxide
$m_c$	Mass of catalyst
$K_c$	Mass transfer coefficient
$C_M$	Mears Criterion
$Mpa$	Megapascal
$\mu m$	Micrometre
$mg$	Milligram
$ml$	Millilitre

<i>mmol</i>	Millimoles
<i>Mm</i>	Millimetre
<i>mmHg</i>	Millimetre of mercury
<i>min</i>	Minute/minutes
<i>mol</i>	Molarity
<i>Nd<sub>2</sub>O<sub>3</sub></i>	Neodymium oxide
<i>NiO</i>	Nickel (II) oxide
<i>N<sub>2</sub></i>	Nitrogen
<i>ppm</i>	Parts per million
<i>%</i>	Percent
<i>H<sub>3</sub>PO<sub>4</sub></i>	Phosphoric acid
$\pm$	Plus or minus
<i>psi</i>	Pound per square inch
<i>KOH</i>	Potassium hydroxide
<i>A/a</i>	Pre-exponential factor
<i>r<sub>AD</sub></i>	Rate of adsorption
<i>r<sub>DC</sub></i>	Rate of desorption
<i>r<sub>s</sub></i>	Rate of surface reaction
<i>r<sub>A</sub></i>	Reaction rate
<i>rpm</i>	Revolution per minute
<i>Si</i>	Silica
<i>NaOH</i>	Sodium hydroxide
<i>SiO<sub>2</sub></i>	Silicon dioxide
<i>m<sup>2</sup></i>	Square metre
<i>NH<sub>2</sub>SO<sub>3</sub>H</i>	Sulfamic acid
<i>-SO<sub>3</sub>H</i>	Sulfonic group
<i>S</i>	Sulphur
<i>H<sub>2</sub>SO<sub>4</sub></i>	Sulphuric acid
<i>SO<sub>2</sub></i>	Sulphuric oxide
<i>SO<sub>4</sub><sup>2-</sup></i>	Sulphated
<i>SO<sub>4</sub><sup>2-</sup>/SnO<sub>2</sub></i>	Sulphated tin oxide
<i>SO<sub>4</sub><sup>2-</sup>/TiO<sub>2</sub></i>	Sulphated titanium oxide
<i>SO<sub>4</sub><sup>2-</sup>/ZrO<sub>2</sub></i>	Sulphated zirconium oxide

$Fe(SO_4)_3/C$	Supported ferric sulphate on carbon
$T$	Temperature
$TCD$	Thermal conductivity detector
$TiO_2$	Titanium oxide
$C_t$	Total concentration of active sites on surface
$WO_3$	Tunsteng trioxide
$vol$	Volume
$V_{HCl}$	Volume of hydrochloric acid
$V_{NaOH}$	Volume of sodium hydroxide
$v/v$	Volume per volume
$wt.\%$	Weight percent
$w/w$	Weight per weight
$C_{wp}$	Weisz Prater Criterion
$Yb_2O_3$	Ytterbium (III) oxide
$ZnO$	Zinc oxide
$ZrO_2$	Zirconium oxide

## LIST OF ABBREVIATIONS

TPA	12-Tungstophosphoric acid
ASTM	American Society for Testing and Materials
A-SZr	Aerogel sulphated zirconia catalyst
BET	Brunauer-Emmett-Teller
CAHZ	Dealuminated HSZM-5 with citric acid
CHNS	Elemental analysis
CSTR	Continuous stirred tank reactor
DDPO	Deodorisation processes of palm oil
EDX	Energy dispersive x-ray spectroscopy
E-R	Eley-Rideal
FAME	Fatty acid methyl ester
FAU	Faujasite
FESEM	Field emission scanning electron microscopy
FFA	Free fatty acid
FS/OMC	Ferric sulfate supported on ordered mesoporous carbon
FT-IR	Fourier-Transform Infrared Spectroscopy
H	Hydrogen
HPA	Heteropolyacid
HPAs	Heteropolyacids
HZ	HZSM-5 zeolite
IM-1	Intermediate 1
IM-2	Intermediate 2
LA	Lanthanum oxide
L-M	Levenberg-Marquardt
MFI	ZSM-5
MK700	Kaolin waste
LHHW	Langmuir-Hinshelwood-Hougen-Watson
MOR	Mordenite
N	Nitrogen
OBR	Oscillatory baffled reactor
OSHA	Occupational Safety and Health Administration

OVAAT	One-variable-at-a-time
PBR	Packed bed reactor
PFR	Plug flow reactor
PMo	Molybdophosphoric acid
PSD	Particle size distribution
PSS	Polystyrene waste
P-H	Pseudo-homogeneous
R&D	Research and development
RBFA	Rice bran fatty acid
RBO	Rice bran oil
RHC	Rice husk char
S	Sulphur
SCER	Sulfonated cation exchange resins
SEM	Scanning Electron Microscopy
SiW	Tungstosilicic acid
SLO	Sulphated lanthanum oxide
ST-DVB	Styrene and divinyl benzene
SUCO	Simulated used cooking oil
SZ	Sulphated zirconia
TFR	Tubular flow reactor
TiZ	Titania zirconia
TPD	Thermal desorption spectroscopy
TW	Tungstophoric acid
UCO	Used cooking oil
USDA	United States Department of Agriculture
WZ	Tungstated zirconia
X-SZr	Xerogel sulphated zirconia catalyst

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## ABSTRAK

Minyak masak terpakai (UCO) adalah salah satu pengganti yang berpotensi sebagai bahan mentah untuk menghasilkan biodiesel kerana kosnya yang rendah. Walaupun mempunyai banyak kelebihan, UCO mengandungi asid lemak bebas yang sangat tinggi dan menyumbang kepada tindak balas saponifikasi apabila ia digunakan dalam tindak balas transesterifikasi. Resin pertukaran ion telah digunakan secara meluas dalam tindak balas esterifikasi asid lemak bebas bagi membantu mengurangkan kandungan asid lemak bebas di dalam UCO. Pemangkin ini telah menunjukkan prestasi yang sangat baik dalam masa yang singkat. Walau bagaimanapun, resin pertukaran ion konvensional mempunyai kawasan asid yang rendah, kawasan permukaan dan isipadu liang yang sederhana, dan juga ketahanan dan kestabilan yang rendah. Oleh itu, dalam kajian ini, pemangkin-pemangkin seperti RCP160M, RCP145H, PK228LH, PK216LH, PK208LH, SK104H dan SK1BH dengan tekstur dan morfologi yang berbeza telah digunakan sebagai pemangkin untuk pengesteran asid lemak bebas dalam minyak masak terpakai. Ciri-ciri fizikokimia pemangkin-pemangkin ini telah dikaji menggunakan analisis *Fourier transform-infra red spectroscopy (FT-IR)*, *nitrogen physisorption*, *scanning electron microscopy (SEM)*, *elemental analysis (CHNS)*, *titration and particle size distribution (PSD)*. Pemangkin-pemangkin ini telah disaringkan terlebih dahulu untuk menentukan pemangkin yang terbaik pada kadar kacauan 450 rpm, 5 wt. % pemangkin pemangkin, 60 °C dan 12:1 nisbah jisim metanol dan minyak. Pemangkin yang terbaik telah digunakan dalam kajian seterusnya dengan memberi tumpuan kepada kesan rintangan pemindahan jisim dan juga parameter-parameter yang berlainan seperti kesan muatan pemangkin, suhu proses dan nisbah jisim metanol dan minyak. Kajian ini telah diteruskan dengan menghasilkan tiga jenis model; Pseudo homogeneous (P-H), Langmuir-Hinshelwood-Hougen-Watson (LHHW) dan Eley-Rideal (Kes I dan Kes II) untuk menentukan kadar pemalar dan tenaga pengaktifan reaksi dengan menggunakan program POLYMAT 6.10. Keputusan kajian menunjukkan bahawa RCP160M menunjukkan prestasi yang terbaik sebagai pemangkin dalam proses pra-rawatan minyak masak terpakai bagi penghasilan biodiesel kerana ia telah berjaya mengatasi pemangkin-pemangkin lain dengan menunjukkan penukaran asid lemak bebas yang paling tinggi dalam proses pengesteran. Prestasi RCP160M yang cemerlang adalah disebabkan oleh luas permukaan pemangkin dan isi padu liang yang tinggi berbanding pemangkin-pemangkin yang lain. Sebanyak 95 % daripada asid lemak bebas telah berjaya ditukarkan pada kadar kacauan 300 rpm, 4 wt. % jumlah pemangkin, 60 °C suhu proses dan 18:1 nisbah jisim metanol dan minyak. Semasa proses kitaran semula RCP160M dalam proses pengesteran, sebanyak 5-15 % aktiviti RCP160M telah berkurang untuk satu kitaran. Pengurangan ini mungkin disebabkan oleh liang pemangkin telah tersumbat oleh minyak semasa tindak balas berlaku dan menghalang reaktan untuk memasuki kawasan aktif pemangkin. Selain itu, pengurangan kawasan yang aktif sewaktu proses mencuci juga merupakan salah satu faktor pengurangan aktiviti pemangkin. Dalam pada itu, keputusan kinetik mendapati bahawa data eksperimen bagi proses pengesteran menggunakan RCP160M telah berjaya dikaitkan dengan model E-R (II) dengan tenaga pengaktifan sebanyak 37.2 kJ/mol. Keputusan kinetik ini menunjukkan bahawa penyerapan molekul bukan polar (asid lemak bebas) adalah lebih baik daripada penyerapan molekul polar (methanol) pada permukaan pemangkin. Melalui kajian ini, pemberian prosedur untuk regenerasi RCP160M perlu diteruskan pada masa hadapan kerana pemangkin ini adalah pemangkin yang berpotensi dalam penghasilan biodiesel.

## ABSTRACT

Used cooking oil (UCO) is one of the potential substitutes for conventional biodiesel feedstock due to its low cost. In spite of its advantage, UCO has high free fatty acid (FFA) level which contributes to saponification reaction when it was directly utilised in base catalysed transesterification reaction. Ion exchange resins have been widely used in FFA esterification reaction to reduce the FFA content as this type of catalyst exhibits good catalyst performance in a short period of time. Nevertheless, conventional ion exchange resin has low acidic sites, moderate specific surface area and pore volume, poor durability and thermal stability. Therefore, in this study styrene-divinylbenzene (DVB) resins; RCP160M, RCP145H, PK228LH, PK216LH, PK208LH, SK104H and SK1BH with different textural and morphological properties were used as catalysts for the esterification of FFA in simulated used cooking oil (SUCO). These resins were characterised using Fourier transform-infrared spectroscopy (FT-IR), nitrogen physisorption, scanning electron microscopy (SEM), elemental analyser (CHNS), titration and particle size distribution (PSD) analyser to determine their physicochemical properties. These catalysts were screened to determine the best performance catalyst under reaction conditions of 300 rpm stirring speed, 5 wt. % catalyst loading, 60 °C and 12:1 methanol to oil mass ratio. The best performance catalyst was used in the subsequent studies focusing on the effect of mass transfer resistance, the effect of catalyst loading, reaction temperature, and methanol to oil mass ratio to investigate the best conditions in a batch mode system. The study proceeded with the kinetics of FFA esterification by developing three kinetic models; Pseudo homogeneous (P-H), Langmuir-Hinshelwood-Hougen-Watson (LHHW) and Eley-Rideal (Case I and Case II) to determine rate constant and activation energy of the reaction using POLYMATH 6.10 program. The results revealed that RCP160M was found to give the best catalytic performance as it outperformed the other catalysts and achieved maximum FFA conversions. This may attributed to the high specific surface area and total pore volume of RCP160M. 95 % of FFA conversion was achieved at the best reaction conditions with a stirring speed of 300 rpm, catalyst loading of 4 wt. %, a reaction temperature of 60 °C, and methanol to oil mass ratio of 18:1. During the reusability study, the catalytic activity of RCP160M decreased about 5-15 % for each cycle. The decrease of FFA conversion was due to pore blockage by oil during the reaction and simultaneously blocked the reactants from accessing the active sites. Besides, the loss of active sites during washing process might possibly occur between the reuse cycles. The kinetic results revealed that the experimental data were best-fitted to the E-R model (Case II) with the activation energy of 37.2 kJ/mol. This study showed that the reaction was limited by surface reaction where the adsorption of non-polar FFA molecules was more favourable than the adsorption of polar methanol molecules. In future, it was recommended that further work is necessary to improve the regeneration procedure of RCP160M as this catalyst can be potentially used as a catalyst for biodiesel production.

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