

Syngas from catalytic steam reforming of palm oil mill effluent: An optimization study

Yoke Wang Cheng^a, Kim Hoong Ng^b, Su Shiung Lam^c, Jun Wei Lim^d, Suwimol Wongsakulphasatch^e, Thongthai Witoon^f, Chin Kui Cheng^{a,*}

^aFaculty of Chemical & Natural Resources Engineering, Lebuhraya Tun Razak, Universiti, Malaysia Pahang, 26300, Gambang Kuantan, Pahang, Malaysia

^bChemistry & Chemical Engineering, Xiamen University Malaysia, Jalan Sunsuria, Bandar Sunsuria, 43900, Sepang, Selangor, Malaysia

^cEastern Corridor Renewable Energy Group (ECRE), School of Ocean Engineering, Universiti Malaysia Terengganu, 21030, Kuala Terengganu, Terengganu, Malaysia

^dDepartment of Fundamental and Applied Sciences, Universiti Teknologi PETRONAS, 32610, Seri Iskandar, Perak, Malaysia

^eCenter of Ecomaterials and Cleaner Technology, Department of Chemical Engineering, Faculty of Engineering, King Mongkut's University of Technology North Bangkok, Bangkok 10800, Thailand

^fCenter of Excellence on Petrochemical and Materials Technology, Department of Chemical Engineering, Faculty of Engineering, Kasetsart University, Bangkok 10900, Thailand

ABSTRACT

In this work, the syngas production rate (F_{Syngas}) of LaNiO₃-catalysed steam reforming of palm oil mill effluent (POME) was optimized with respect to POME flow rate ($_VPOME$), catalyst weight (W_{cat}), and particle size (d_{cat}). With a net acidity, the synthesized LaNiO₃ catalysed POME steam reforming by cracking the bulky compounds and valorising simpler intermediates into syngas. The degradation efficiencies (XP) were also evaluated by assessing wastewater parameters, viz. pH, chemical oxygen demand (COD), biochemical oxygen demand (BOD₅), total suspended solids (TSS), and colour intensity (A). After steam reforming at 873 K, the liquid condensate has neutral pH and zero TSS. The parallel trend of F_{Syngas} and XP verified syngas generation from degradation of POME's organics. At higher $_VPOME$ (0.05e0.09 mL/min), greater POME partial pressure promoted its steam reforming and water gas shift, which enhanced catalytic performance. Beyond optimum $_VPOME$ (0.09 mL/min), coke-forming Boudouard reaction deteriorated catalytic activity. Catalytic performance was boosted for a longer residence time at higher W_{cat} (0.1e0.3 g); nonetheless, it was reduced by agglomerated catalyst when $W_{\text{cat}} > 0.3$ g. Finer LaNiO₃ ($d_{\text{cat}} > 74$ nm) with greater surface area to volume ratio exhibited better performance; however, ultrafine LaNiO₃ ($d_{\text{cat}} < 74$ nm) had poor performance because of occluded pores. Remarkably, optimized POME steam reforming over LaNiO₃ ($T = 873$ K, $_VPOME = 0.09$ mL/min, $W_{\text{cat}} = 0.3$ g, $d_{\text{cat}} = 74$ nm) has generated 132.47 mmol/min of H₂-rich syngas, whilst achieved 99.53% XCOD, 99.88% XA, 99.75% XBOD₅, and 100% XTSS.

KEYWORDS: Palm oil mill effluent; Wastewater remediation; Steam reforming; Syngas production