

## Effect of non-solvent additives on the structure and performance of PVDF hollow fiber membrane contactor for CO<sub>2</sub> stripping

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### ABSTRACT

Microporous polyvinylidene fluoride (PVDF) hollow fiber membranes with various non-solvent additives, i.e. lithium chloride, glycerol, polyethylene glycol (PEG-400), methanol and phosphoric acid, were fabricated for CO<sub>2</sub> stripping via membrane contactors. The membranes were characterized in terms of liquid entry pressure, contact angle, gas permeation and morphology analysis. CO<sub>2</sub> stripping performance was investigated by using an in-house made stainless steel module with CO<sub>2</sub>-preloaded aqueous diethanolamine as the liquid absorbent. Hydrophobicity and gas permeability of the membranes reduced with the addition of a non-solvent additive in the polymer dope but increase in liquid entry pressure was observed as more sponge-like structures developed in the inner layer of the fibers. It was found that PVDF/PEG-400 membrane produced the highest stripping flux of  $4.03 \times 10^{-2} \text{ mol m}^{-2} \text{ s}^{-1}$  which can be correlated to its high gas permeation and high effective surface porosity. The result of long-term stripping operation indicated an approximately 80% stripping flux reduction which can be related to the interaction of polymer membrane and amine solution at high temperature.

### KEYWORDS:

PVDF hollow fiber membrane; Non-solvent additive; CO<sub>2</sub> stripping; Membrane contactor

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## REFERENCES

1. G.K. Agrahari, N. Verma, P.K. Bhattacharya, Application of hollow fiber membrane contactor for the removal of carbon dioxide from water under liquid–liquid extraction mode, *J. Membr. Sci.* 375 (2011) 323–333.
2. Brian Miller, Jorge Munoz, Fred Wiesler, Boiler Feed Water Degasification Using Membrane Contactors—New Methods for Optimized Performance, *Membrana-Industrial Separations*, Charlotte, NC. IWC-05-79 (2005) (Presented at the International Water Conference)
3. J. Shao, H. Liu, Y. He, Boiler feed water deoxygenation using hollow fiber membrane contactor, *Desalination* 234 (2008) 370–377.
4. S. Bamperng, T. Suwannachart, S. Atchariyawut, R. Jiratananon, Ozonation of dye wastewater by membrane contactor using PVDF and PTFE membranes, *Sep. Purif. Technol.* 72 (2010) 186–193.
5. V.V. Usachov, V.V. Teplyakov, A.Yu. Okunev, N.I. Laguntsov, Membrane contactor air conditioning system: experience and prospects, *Sep. Purif. Technol.* 57 (2007) 502–506