

Enhanced syngas production from glycerol dry reforming over Ru promoted -Ni catalyst supported on extracted Al₂O₃

Nurul Asmawati Roslan^a, Sumaiya Zainal Abidin^{b,c}, Osarieme Uyi Osazuwa^{b,d}, Sim Yee Chin^{a,b},
Y. H. Taufiq-Yap^{e,f}

^a Department of Chemical Engineering, College of Engineering, Universiti Malaysia Pahang, Lebuhraya Tun Razak, 26300, Gambang, Kuantan, Pahang, Malaysia

^b Centre for Research in Advanced Fluid & Processes (FLUID CENTRE), Universiti Malaysia Pahang, 26300 Gambang, Kuantan, Pahang, Malaysia

^c Faculty of Chemical Engineering, Industrial University of Ho Chi Minh City, 12 Nguyen Van Bao St, Go Vap, Ho Chi Minh City 7000, Vietnam

^d Department of Chemical Engineering, University of Benin, PMB 1154, Benin City, Edo State, Nigeria

^e Catalysis Science and Technology Research Centre (PutraCAT), Faculty of Science, Universiti Putra Malaysia, 43400, UPM, Serdang, Selangor, Malaysia

^f Chancellery Office, Universiti Malaysia Sabah, 88400, Kota Kinabalu, Sabah, Malaysia

ABSTRACT

Crude glycerol, a by-product of biodiesel production, has drawn considerable attention to the importance of glycerol valorization through dry reforming reaction to obtain syngas. The selection of suitable catalysts is significantly important to enhance the catalytic activity in glycerol dry reforming (GDR) reactions. Hence, Ru with different loadings (i.e. 1%, 2%, 3%, 4%, 5%) doped in 15% Ni-extracted Al₂O₃(EA) was evaluated as catalyst via GDR process in this study. The catalyst prepared by ultrasonic-impregnation assisted technique was subjected to 8 h of CO₂ reforming of glycerol. The reactant conversions and products yield was in the order of 3%Ru-15%Ni/EA > 5%Ru-15%Ni/EA > 4%Ru-15%Ni/EA > 2%Ru-15%Ni/EA > 1%Ru-15%Ni/EA > 15%Ni/EA, while the quantity of carbon deposited was in the order 15%Ni/EA > 1%Ru-15%Ni/EA > 2%Ru-15%Ni/EA > 4%Ru-15%Ni/EA > 5%Ru-15%Ni/EA > 3%Ru-15%Ni/EA. 3%Ru-15%Ni/EA attained the greatest glycerol conversions of 90%, H₂ yield of 80% and CO yield of 72% with the lowest carbon deposition of 7.38%. The dispersion of Ni particles on EA support evidently improved after the promotion step with Ru, which minimized the agglomeration of Ni and smaller crystallite size. In addition, the introduction of Ru increased the oxygen storage capacity which significantly reduced the formation of carbon during the reaction. GDR's optimal reaction temperature obtained over 3%Ru-15%Ni/EA catalysts was at 1073 K (i.e. 93% glycerol conversion; 87% H₂ yield; 79% CO yield). Over a 72 h time on stream at 1073 K, 3%Ru-15%Ni/EA catalyst had superior catalytic activity and stability. Overall, 3%Ru-15%Ni/EA catalyst was more coke-resistant than other promoted catalysts due to its accessible structure, higher oxygen storage capacity, moderate basicity, uniformly dispersed Ni phase and stronger Ru/Ni-EA interaction.

KEYWORDS

Glycerol; Dry reforming; Syngas; Hydrogen; Ni-based catalyst; Nobel-metal promoter

ACKNOWLEDGEMENTS

The authors would like to acknowledge the Ministry of Higher Education, Malaysia for awarding the FRGS research grant vote RDU190197 (FRGS/1/2018/TK02/UMP/02/12) and Universiti Malaysia Pahang (RDU1803118 and PGRS1903121) for financial support.