

THE EVALUATION OF PREMIXED  
BIOGAS/AIR EXPLOSION  
CHARACTERISTICS IN A 20 L CLOSED  
VESSEL

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## **SUPERVISOR'S DECLARATION**

We hereby declare that we have checked this thesis and in our opinion, this thesis is adequate in terms of scope and quality for the award of the degree of Master of Science.

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I hereby declare that the work in this thesis is based on my original work except for quotations and citations, which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at Universiti Malaysia Pahang or any other institutions.

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CHARACTERISTICS IN A 20 L CLOSED VESSEL

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## ABSTRAK

Letupan gas yang melibatkan biogas adalah fenomena yang serius akibat dari pembakaran pracampuran awan gas. Bagi mengkaji faktor-faktor yang menyumbang kepada kejadian letupan, kajian terperinci dan menyeluruh terhadap kepekatan bahan api, tekanan mula dan suhu, dan pencairan karbon dioksida ( $\text{CO}_2$ ) telah dijalankan. Namun, kajian-kajian yang dijalankan ini hanya melibatkan campuran bahan api selain daripada biogas. Biogas merupakan gas yang mudah terbakar memandangkan komposisinya terdiri daripada 50 hingga 70% metana ( $\text{CH}_4$ ), 30 hingga 50%  $\text{CO}_2$  dan beberapa gas yang lain. Oleh itu, kekurangan data mengenai ciri-ciri asas pembakaran dan letupan biogas akan membawa kepada pertambahan potensi bahaya letupan terutamanya dalam industri. Dalam kajian ini, letupan gas di ruang terbatas telah dijalankan. Pendekatan eksperimen menggunakan bekas sfera tertutup yang mempunyai isipadu 20 L telah dipilih bagi mengkaji ciri-ciri letupan pracampur campuran biogas/udara. Faktor-faktor seperti nisbah kesetaraan (ER), kepekatan  $\text{CO}_2$  dan tekanan mula yang menyumbang kepada ciri-ciri letupan pracampur campuran biogas/udara telah dikaji dan dianalisis melalui tekanan lebih letupan ( $P_{ex}$ ), tekanan lebih letupan maksimum ( $P_{max}$ ), kadar maksimum kenaikan tekanan ( $(dP/dt)_{max}$ ) dan indeks deflagrasi gas ( $K_G$ ). Berdasarkan penilaian yang dilakukan, pracampur campuran biogas/udara yang mempunyai 40% vol/vol  $\text{CO}_2$  pada nisbah kesetaraan yang agak tinggi (ER = 1.2) adalah yang paling serius apabila meletup dengan  $P_{ex}$ ,  $P_{max}$  dan  $(dP/dt)_{max}$  masing-masing bernilai 8.50 bar, 9.08 bar dan 120.00 bar/ms. Selain itu, berdasarkan penilaian kepekatan  $\text{CO}_2$ , pracampur campuran biogas/udara yang mempunyai 45% vol/vol  $\text{CO}_2$  pada ER 1.2 didapati paling tidak serius apabila meletup dengan  $P_{ex}$ ,  $P_{max}$  dan  $(dP/dt)_{max}$  masing-masing bernilai 7.60 bar, 8.05 bar dan 82.25 bar/ms. Ini adalah disebabkan oleh kesan fizikal  $\text{CO}_2$  dan ketidakstabilan kemeresapan-haba. Malah, pracampur campuran biogas/udara pada tekanan mula 1.1 bar juga didapati paling serius apabila meletup dengan  $P_{ex}$ ,  $P_{max}$  dan  $(dP/dt)_{max}$  masing-masing bernilai 9.90 bar, 10.90 bar dan 1922.50 bar/ms. Ini adalah disebabkan oleh batasan ruang yang wujud di antara molekul, kadar tindak balas kimia yang cepat serta peranan ketidakstabilan kemeresapan-haba. Kajian ini juga menunjukkan bahawa pracampur campuran biogas/udara pada ER antara 0.8 hingga 1.5 tergolong dalam kategori kelas bahaya St-3, yakni merujuk kepada letupan yang sangat serius. Data  $P_{max}$  yang diperoleh daripada eksperimen juga telah di sahkan dengan menggunakan perisian FLame ACcelaration Simulator (FLACs). Keputusan yang diperoleh menunjukkan bahawa  $P_{max}$  yang diperoleh daripada eksperimen berada dalam lingkungan had kelainan  $\pm 30\%$  dan yang dianggap memuaskan. Malah, perbandingan  $P_{max}$  yang diperoleh daripada eksperimen dan data yang diterbitkan daripada kajian-kajian terdahulu juga menunjukkan trend yang setanding. Kesimpulannya, ER, kepekatan  $\text{CO}_2$  dan tekanan awal pracampur campuran biogas/udara mempunyai kesan yang signifikan terhadap ciri-ciri letupan dan boleh membawa kepada bencana yang melibatkan letupan.

## ABSTRACT

A gas explosion involving biogas is a severe phenomenon that results from the combustion of a premixed gas cloud. As of today, several explosion accidents involving biogas have been reported worldwide. Extensive and comprehensive studies have been done to investigate the factors contributing to the explosion (i.e. the fuel concentration, initial pressure and temperature, and carbon dioxide (CO<sub>2</sub>) dilution). However, these studies have only been done involving fuel/air mixtures other than biogas. Since biogas is composed of 50 to 70% methane (CH<sub>4</sub>), 30 to 50% CO<sub>2</sub> and traces of other gases, it is highly combustible. Lacked in its fundamental combustion and explosion characteristics will lead to a higher potential of explosion hazard especially in industries. In this study, a gas explosion in a confined space is considered. An experimental approach using the 20 L closed spherical vessel is adopted to investigate the explosion characteristics of the premixed biogas/air mixtures. The factors (i.e. equivalence ratio (ER), CO<sub>2</sub> concentration and initial pressure) contributed to the premixed biogas/air explosion characteristics (i.e. the explosion overpressure (P<sub>ex</sub>), maximum explosion overpressure (P<sub>max</sub>), the maximum rate of pressure rise ((dP/dt)<sub>max</sub>) and gas deflagration index (K<sub>G</sub>) was evaluated. From the results, it was found that the premixed biogas/air having 40% vol/vol CO<sub>2</sub> was the most severe when exploded at a slightly rich concentration (ER = 1.2) with P<sub>ex</sub>, P<sub>max</sub> and (dP/dt)<sub>max</sub> of 8.50 bar, 9.08 bar and 120.00 bar/ms respectively. Besides, the evaluation of CO<sub>2</sub> concentration in the premixed biogas/air mixture also showed that the mixture having 45% vol/vol CO<sub>2</sub> at ER of 1.2 was found to be the least severe when exploded with P<sub>ex</sub>, P<sub>max</sub> and (dP/dt)<sub>max</sub> of 7.60 bar, 8.05 bar and 82.25 bar/ms respectively. This was due to the physical effect of CO<sub>2</sub> and thermal-diffusive instability. Further, the premixed biogas/air mixture was also found to be the most severe when exploded at an initial pressure of 1.1 bar with P<sub>ex</sub>, P<sub>max</sub> and (dP/dt)<sub>max</sub> of 9.90 bar, 10.90 bar and 1922.50 bar/ms respectively. This was due to the fewer spaces between molecules, higher reaction rate as well as due to the role of thermal-diffusive instability. This study also shows that the premixed biogas/air mixture at ER ranging from 0.8 to 1.5 to fall into St-3 hazard class that was the most severe when exploded. Verification of the P<sub>max</sub> obtained from the experimental results was also conducted using the FLame ACceleration Simulator (FLACs) software. Results showed that the P<sub>max</sub> was found to be within the ± 30% limit of discrepancy and is considered satisfactory. The compared P<sub>max</sub> from this study with published data from literature also shows a comparable trend. As a conclusion, it shows that the ER, CO<sub>2</sub> concentration and the initial pressure of the premixed biogas/air mixture has a significant impact on its explosion characteristics, which can lead to a catastrophic explosion.

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## LIST OF SYMBOLS

-	Negative
%	Percent
$(dP/dt)_m$	Rate of pressure rise
$(dP/dt)_{max}$	Maximum rate of pressure rise
~	Approximately
<	Less than
=	Equal
>	More than
$c_p$	Specific heat capacity
D	Mass diffusivity
$dm^3$	Cubic decimetre
$ft^3$	Cubic foot
g	Gram
g	Gravitational acceleration
h	Heat transfer coefficient
hr	Hour
K	Kelvin
k	Thermal conductivity
k	Turbulent kinetic energy
kg	Kilogram
kJ	Kilojoules
kPa	Kilopascal
L	Litre
$l_T$	Length scale
m	Meter
$\dot{m}$	Mass rate
$m^3$	Cubic meter
mA	Milliampere
mbar	Millibar
MJ	Megajoule
mm	Millimetre

mPa	MilliPascal
ms	Millisecond
°C	Degree Celsius
p	Absolute pressure
P	Pressure
P <sub>0</sub>	Initial pressure
P <sub>Air</sub>	Air pressure
P <sub>d</sub>	Expansion pressure
P <sub>ex</sub>	Explosion overpressure
P <sub>Fuel</sub>	Fuel pressure
P <sub>k</sub>	Production of turbulent kinetic energy
P <sub>m</sub>	Corrected explosion overpressure
P <sub>max</sub>	Maximum explosion overpressure
psi	Pounds per square inch
P <sub>Total</sub>	Total pressure
P <sub>ε</sub>	Production of dissipation
R	Universal gas constant
R <sub>burned</sub>	Radius of the burned gas mixture
Re <sub>T</sub>	Turbulent Reynolds number
R <sub>flame</sub>	Radius of the flame
R <sub>fuel</sub>	Fuel reaction rate
R <sub>o,i</sub>	Flow resistance due to sub-grid obstructions
R <sub>w,i</sub>	Flow resistance due to the walls
R <sub>wall</sub>	Radius of the vessel
s	Second
S <sub>L</sub>	Laminar burning velocity
S <sub>QL</sub>	Turbulent burning velocity in the quasi-laminar regime
t	Time
T <sub>b</sub>	Maximum flame temperature
T <sub>burned</sub>	Temperature of the burned gas mixture
T <sub>o</sub>	Initial flame temperature
T <sub>unburned</sub>	Temperature of the unburned gas mixture
u'	Turbulent flow



$V$	Volt
$V$	Volume
$W$	Molar mass
$W$	Watt
$W_p$	Inflection point
$x$	Length coordinate
$Y_{\text{fuel}}$	Mass fraction
$\beta$	Volume porosity
$\beta$	Volume porosity
$\beta_j$	Area porosity
$\gamma_P$	Fuel dependent parameter
$\varepsilon$	Dissipation of turbulent kinetic energy
$\varepsilon$	Rate of decay
$\mu$	Mean velocity
$\mu_{\text{eff}}$	Effective viscosity
$\xi$	Mixture fraction
$\rho$	Density
$\rho_u$	Unburned gas density
$\sigma_{ij}$	Stress Tensor
$\tau_c$	Chemical time scales
$\tau_K$	Kolmogorov time scale of turbulence
$\tau_t$	Turbulent time scales
$\Omega$	Resistance
$\Phi$	Equivalence ratio
$Q$	Heat rate

## LIST OF ABBREVIATIONS

1D	One-dimensional
3D	Three-dimensional
A	Ampere
AD	Anaerobic digestion
Apr.	April
atm	Atmospheric
Aug.	August
BTU	British thermal unit
CDM	Clean Development Mechanism
CFD	Computational Fluid Dynamics
CH <sub>4</sub>	Methane
CO	Carbon monoxide
CO <sub>2</sub>	Carbon dioxide
CPO	Crude palm oil
Da	Damköhler number
Dec.	December
ER	Equivalence ratio
Feb.	February
FLACs	FLame ACceleration Simulator
FS	Full scale
GHG	Greenhouse gases
GW	Gigawatts
H <sub>2</sub>	Hydrogen
H <sub>2</sub> O	Water vapor
H <sub>2</sub> S	Hydrogen sulfide
H <sub>2</sub> SO <sub>4</sub>	Sulphuric acid
He	Helium
Jan.	January
Ka	Karlovitz number
Ka <sub>δ</sub>	Klimov-Williams line
K <sub>G</sub>	Deflagration index

L	Markstein length
L-D	Landau-Darrieus
Le	Lewis number
LFL	Lower flammability limit
LHV	Lower heating value
Ma	Markstein number
Mar.	March
MoSTI	Minister of Science, Technology and Innovation
N <sub>2</sub>	Nitrogen
N <sub>2</sub> O	Nitrous oxide
NG	Natural gas
NH <sub>3</sub>	Ammonia
Nov.	November
O <sub>2</sub>	Oxygen
Oct.	October
POME	Palm oil mill effluent
ppm	Parts per million
Re	Reynolds number
Sep.	September
SO <sub>2</sub>	Sulfur dioxide
T	Temperature
UFL	Upper flammability limit
vol	Volume

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