

Preliminary Study on Pelletization of Oil Palm Empty Fruit Bunches (EFB)/Spent Activated Carbon (AC): Effect of Mixing and Adhesive Ratio

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ABSTRACT – Non-renewable resources such as fossil fuels could be combusted for energy and electricity to human kind. The demand of fossil fuel energy had reached an exponential growth which caused disasters and catastrophic damages on the environment; thus, renewable resources should be implemented to protect the environment. One of the natural resources was biomass waste. In this study, spent activated carbon (AC) was co-pelletized with biomass waste, oil palm empty fruit bunches (EFB). The effect of EFB, AC and adhesive (tapioca) mixing ratio in the pellet was evaluate through physical and thermal properties. The raw materials were grinded and mixed together at different AC/EFB/tapioca ratio. The mixed raw materials were compressed at 130°C and 7 MPa for 10 minutes. The densified products were characterized by using Thermogravimetric Analysis (TGA). For the thermal characteristics, sample with 0% waste AC, 90% EFB and 10% starch had the highest mass loss rate (570 µg/min) followed by sample with 10% of waste AC, 60% of EFB and 30% of starch which was 420 µg/min. Besides, sample with 0% waste AC, 90% EFB and 10% had the highest burn out temperature (802.6 °C) followed by sample with 30% of waste AC, 60% of EFB and 10% of starch which was 792.85 °C. In conclusion, sample with 0% waste AC, 90% EFB and 10% starch had an easiest ignition and longest combustion period since it had the highest mass loss rate and burn out temperature.

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INTRODUCTION

Biomass energy is the solar energy that is stored in plants and animals or in the wastes that are produced. This energy can be recovered by burning biomass as fuel [1]. The average majority of biomass energy is produced from wood and wood wastes (64%), followed by solid waste (24%), agricultural waste (5%), and landfill gases (5%) [2]. One of the agricultural wastes is oil palm empty fruit bunches (EFB). EFB is the waste generated from the palm oil extracting process. Due to its availability in Malaysia, oil palm waste is the best to be used as biomass waste. In 2019, Malaysia was one of the producers of palm oil, producing 17.73 million tonnes, or 29.5% of the world total production.

Previous research and commercialization activities have indicated that EFB has been subjected to produce numerous products such as bio-syngas, bio-oil, bio-hydrogen, briquette and pellet fuels, bio-ethanol, and activated carbon [3, 4]. Moreover, these EFBs are also used as fuels to generate energy. EFB generates the most power among the other by-products from the palm oil mill industry. According to Sarawak Energy, EFB has generated a total of 125 MW of electricity which is higher than fiber (112 MW), shell (98 MW), and palm oil mill effluent (POME) (40 MW).

Activated carbons (AC) are the most versatile and commonly used adsorbents because of their extremely high surface areas micropore volumes, large adsorption capacities, fast adsorption kinetics and relatively ease of regeneration. In the pharmaceutical area, the chemical activated carbon with iron (III) chloride is used to adsorb antipyrine from wastewater treatment plants [5]. Besides, in the biogas production area, bio-methane is adsorbed from anaerobic digestion by using AC [6]. Furthermore, in the mining field, AC is also useful in the adsorptive removal of sulfate from acid mine drainage. However, once contaminants concentrate on the active bonding sites and the AC becomes saturated, it is replaced with fresh activated carbon, and spent AC is usually incinerated.

Restoring the adsorption capacity, referred to as AC regeneration, might involve heating in steam or nitrogen (N₂) at a given temperature for an adequate length of time or the use of stirring electrochemical reactors. Depending on the substances adsorbed that need to be removed, some solvents, acids, and alkalis might be employed. Regeneration is therefore an energy-intensive and relatively expensive option. Regeneration efficiency, however, decreases after some cycles and deterioration of the regenerated adsorbent's porosity and serious carbon weight losses [7].

According to Isla-Cabaraban [8], spent AC or waste AC could be used in cofiring with coal which is an economical method for waste disposal while recovering energy from the heat of combustion. From the study of [9], sewage sludge was co-pelletized with biomass and the pellet showed its potential in power generation. Hence, in this study, EFB (biomass) and waste AC will be co-pelletized due to their potential in generating energy.

Pelletization is referred to an agglomeration process that compresses fine powder or granules of dried biomass into small, spherical, or semi-spherical pellets under high pressure. According to the study of Jiang et.al, the density of pellet was increased when the pressure was increased since the solid particles became closer. In view of the effect of material ratio, when the ratio of material that adds to the biomass increased, the density of pellet increased. This is proved in the study of Jiang and co-workers, when the ratio of sludge is increased, the density of co-pelletized pellet increased. In terms of temperature, as reported by Gilbert et al., the densified pellet density was increased from 50 °C to 110 °C. However, attention should be paid to a slight decrease in pellet density when the temperature at 125 °C. The appropriate moisture content for co-pelleting is 10-15% and peaked at 15%. On the other hand, when the biomass size is decreased, the pellet density is increased [10].

The main objective of this paper was to determine the effect of the AC/EFB/Tapioca ratio in pellet physical properties with different material and adhesive ratios. The thermal properties of EFB and pelletized samples were analyzed by thermogravimetric analysis (TGA) [11].

MATERIALS AND METHODS

Raw Materials Collection

The spent activated carbon was collected at an industry in Kerteh, Terengganu while the EFB was collected at Lepar. Both samples were dried prior for experimental use. For the adhesive, commercial tapioca flour was chosen and prepared.

Sample Preparation

EFB was ground by SIMA FG 400 X 200 Grinder with a mesh size of 2 mm. The size of ground EFB was lower than 2 mm. Ground EFB was placed in a stack of sieves arranged from the largest to the smallest openings. The sieve sizes used were 800, 630, 500, 355, 250, and 106 microns. The set of sieves were placed on the Retsch AR 200 sieve shaker. The duration of the sieving process was 10 min and the amplitude was 3.0 m/mg. The particle size of EFB that below 106 microns was chosen for material mixing.

Mixing of Co-Pelletization Sample

The samples for the co-pelletization process were prepared as in Table 1. The raw materials were mixed according to the ratios by blending. The estimated density of the pellet is 700 kg/m³, with the volume of the pellet is 7.85 cm³ obtained from the mold design. The raw material mixture was sprayed with 25 times of water using a spray bottle during the mixing process.

Table 1. Sample ratio for each pellet sample

Sample	AC/EFB Ratio		
	Waste AC	Ratio (%)	
		EFB	Tapioca
1	0	90	10
2	10	80	10
3	20	70	10
4	30	60	10
	EFB/Adhesive Ratio		
1	10	90	0
2	10	80	10
3	10	70	20
4	10	60	30

The blended raw mixture was inserted and pre-compressed manually into mould. The pre-compressed raw mixture in mould was compressed at a temperature of 130 °C and pressure of 7 MPa for 10 minutes using Lotus Scientific LS-22025 25 Ton Hot and Cold Moulding Press. After the compression process was completed, the densified mixture was cooled under room temperature [12].

Characterization of Raw Materials and Pelletized Sample

Thermogravimetric analysis was performed to determine the thermal properties of the raw EFB and pelletized sample. The thermal stability data were collected on a Hitachi STA 7000 thermogravimetric analyzer under linear temperature conditions. The temperature was swept from 50°C to 800°C for samples of 10-15 mg placed in an aluminium pan at a heating rate of 10°C/min under nitrogen atmosphere [11].

The actual density of the pellet was determined after the pellet was dried by using Equation 1. The W_c was referred to the mass of dried sample and crucible while W_a was referred to the mass of crucible.

$$\text{Actual density} \left(\frac{\text{kg}}{\text{m}^3} \right) = \frac{W_c - W_a}{1000 \times \text{Volume pellet}} \quad (1)$$

EXPERIMENTAL RESULTS

Physical Appearance of the Pelletized Sample

The physical appearance of pelletized samples was illustrated in Figure 1. The mixtures of different ratios were able to produce a compact and maintain in shape of pellet. This indicate that the optimum amount of moisture and pressure supplied during the pressing process. In addition, an optimum moisture content in pellets improves densification characteristics by increasing bonding via van der Waal's forces.

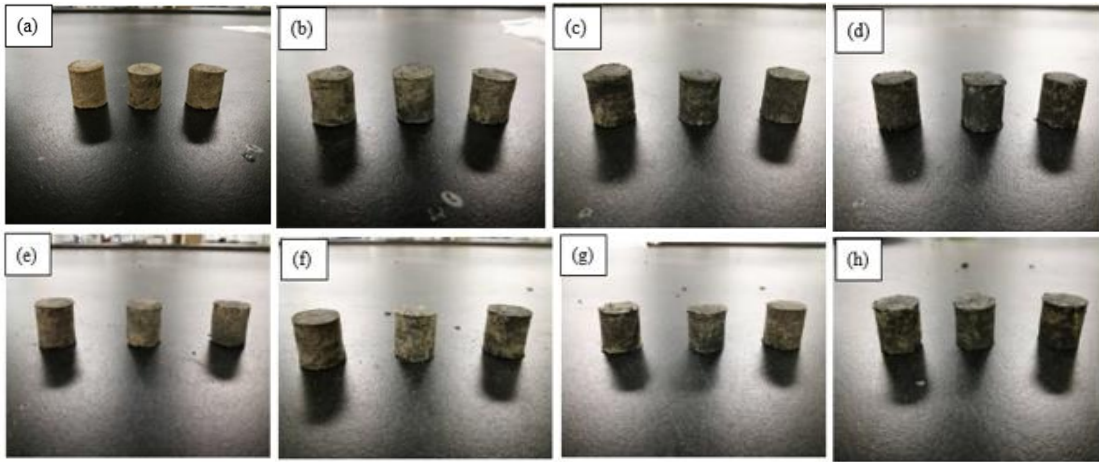


Figure 1. Pelletized samples noted by waste AC: EFB: Tapioca (a) 0%: 90%: 10% (b) 10%: 80%: 10% (c) 20%: 70%: 10% (d) 30%: 60%: 10% (e) 10%: 90%: 0% (f) 10%: 80%: 10% (g) 10%: 70%: 20% (h) 10%: 60%: 30%.

Actual Pellet Density

Figure 2 shows that as the mass ratio of EFB for both AC/EFB and EFB/Adhesive ratios factors increased, the pellet density decreased and agreed well with the previous reported work [13]. The pellets made from lower particle size exhibited higher density for all biomass. In this study, the lower ratio of EFB in the pellet would result in a higher pellet density. This probably due to the lower ratio of EFB in the pellet will lower the average particle size of biomass in the pellet. The smaller average particle size of biomass could yield a high surface area of contact to form bonds or solid bridges during the compaction process and finally produce higher density pellets [14]. Although the mass ratio of starch is increasing in the EFB/Adhesive ratio factor, there is no noticeable effect of starch content on the individual pellet density [15].

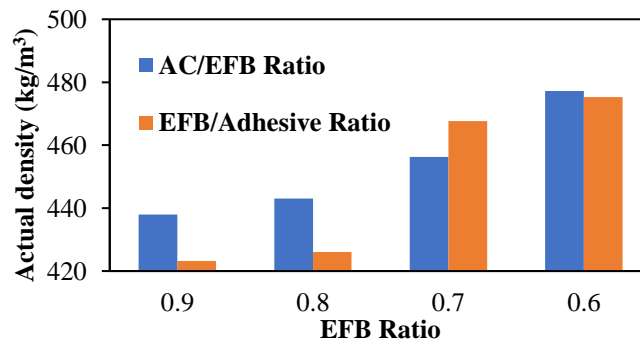


Figure 2. Effect of EFB ratio on the actual pellet density.

Thermal Properties of PHA/NCF Composite

Thermogravimetric analysis is an important method to understand the thermal stability and combustibility of fuels for subsequent application in combustion facilities. TG and DTG profiles of densified pellets with different material and adhesive ratios were shown in Figures 3 and 4.

From TG curves in Figure3, the first stage corresponds to moisture and very light volatile matter content in the samples is eliminated at a temperature ranging from ambient temperature to 250 °C. At this stage, there were identical among samples from raw EFB and different AC/EFB and EFB/Adhesive ratios. The second stage was indicated by a rapid weight loss beginning at 250 °C to 350 °C which occurred from the decomposition of hemicellulose common content of lignocellulosic biomass components. The third stage was observed from the change of a rate of mass loss at a temperature

around 350 °C to 795 °C for all samples except for samples with 0% of waste AC, 90% of EFB, and 10% of starch, until 800 °C. After that, the rate of mass loss would remain constant at the fourth stage, where the carbon content has burnt out [16].

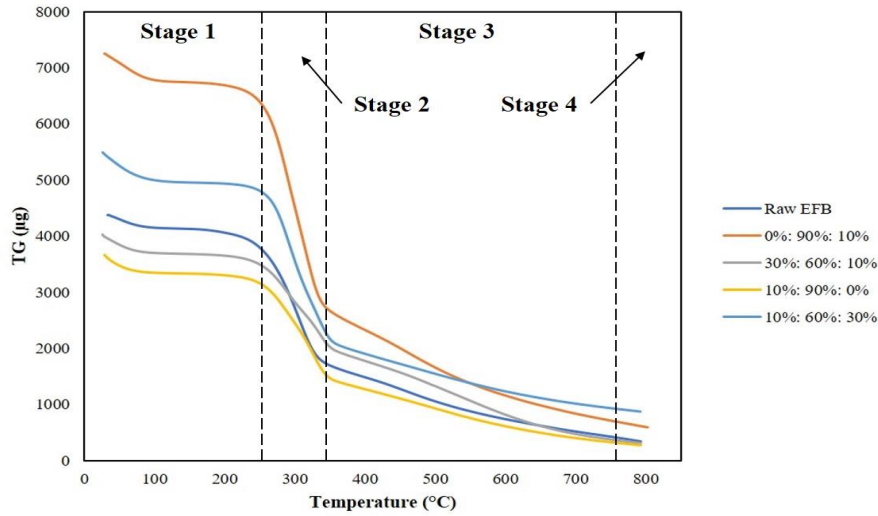


Figure 3. TG curves of raw EFB and pelletized samples of different material and adhesive ratio noted as waste AC: EFB: tapioca

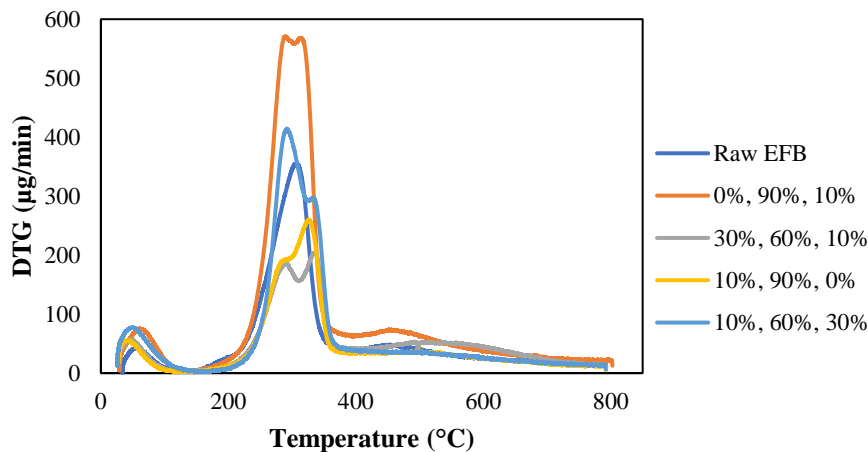


Figure 4. DTG curves of raw EFB and pelletized samples of different material and adhesive ratio waste; AC: EFB: tapioca

On the DTG curves shown in Figure 4, the temperatures at which the maximum rate of weight loss occurred are indicated by the position of peaks in the curve. The four distinct peaks were observed which corresponds to four different changes in the slope of TG curves. The characteristics of three peaks during the combustion process of each material and adhesive ratios were summarized and shown in Table 2. The highest mass loss rate was obtained from a sample with 0% of waste AC, 90% of EFB, and 10% of starch which provide an easier ignition.

The burnout temperature, T_b which is shown in Table 2 is the temperature where the rate of weight lost consistently decrease to less than 1% per min or when 99% of the combustible materials have been burnt out [17]. Sample with 0% of waste AC, 90% of EFB, and 10% of starch was provided the highest burnout temperature which was 802.6 °C. The higher burnout temperature indicating the longer the combustion period requires.

Table 2. Thermal characteristics of raw EFB and pelletized sample at different AC/EFB/Tapioca ratios

Sample	T_{p1} (°C)/ max rate (µg/min)	T_{p2} (°C)/ max rate (µg/min)	T_{p3} (°C)/ max rate (µg/min)	T_b (°C)/
Raw EFB	55.32/43.48	357.45/360	458.57/52.17	792.73
0:90:10	68.09/76.52	314.89/570	462.86/78.26	802.58
30:60:10	42.55/69.57	340.43/205.71	557.14/56.52	792.85
10:90:0	42.55/69.57	327.66/270	540/39.13	792.63
10:60:30	51.06/78.26	293.62/420	531.43/39.13	792.16

CONCLUSION

In conclusion, the higher EFB ratio or content in the pellet was increased, the actual pellet density would decrease. This was because the higher amount of EFB would increase the average particle size of the pellet and reduced the pellet density. Furthermore, the sample with 0% of waste AC, 90% of EFB, and 10% of starch had the longest combustion period since it had the highest burn out temperature which was 802.6 °C. Besides, a sample with 10% of waste AC, 60% of EFB, and 30% of starch were the second easiest of ignition because it had the second-highest of mass loss rate which was 420 µg/min, while the sample with 30% of waste AC, 60% of EFB and 10% of starch was the second-longest of combustion period because it had the second-highest of burn out temperature which was 792.85 °C. The study shows that the addition of AC has not given a significant impact to the burnout temperature as the value is just about similar to the raw EFB.

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