



## Numerical Solutions on Reiner–Philippoff (RP) Fluid Model with Velocity and Thermal Slip Boundary Condition

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### ABSTRACT

Non-Newtonian fluid model was created against the Newton's Law of viscosity where the viscosity is no more constant and dependent on the shear rate. The existing such fluid can be found in many industrial claims especially in food manufacturing, lubrication, biomedical flows and oil and gas. Besides, the used of non-Newtonian fluid occurs in mining industry where the slurries and muds are often handled. There are many models on non-Newtonian fluid available in literature where some of them capture the specific properties. The Reiner–Philippoff (RP) fluid model is considered in this endeavour due to the capabilities of the model which can be acted in three different family of fluid which are viscous, shear thickening and the shear-thinning. Mathematical model is constructed using continuity, momentum and energy equations where in form of partial differential equations (PDEs). The complexity of the proposed model is abridged by deduced the equations into ordinary differential equations (ODEs) by adopting similarity variables before the computation is done by `bvp4c` function drive in MATLAB software. To ratify the validity of the proposed model as well as numerical outputs, the comparative study is performed and it found to be in very strong agreement under limiting case where the present model is condensed to be identical with the reported model previously. The consequences of pertinent parameters on fluid's characteristics are analyzed in details through the plotted graphic visuals and tabular form.

## 1. Introduction

Non-Newtonian fluid encounter in many industrial applications such as food processing, biomedical, manufacturing and also including oil and gas industries. A thorough understanding on

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the properties and behaviour of this fluid is crucial to the mentioned applications. The evolution on the growth in mathematical model concentrating on non-Newtonian fluid has been in high interest for the past few decades due to cost effectiveness in examine the properties of non-Newtonian fluid. The fact that characteristic of particular fluid does not follow the Newton's law of viscosity where the constant viscosity is independent to the stress, many existing real fluids suit its characteristics. The main characteristic in non-Newtonian fluids is the viscosity can vary when under force to either more liquid or more solid [1]. The close example for this type of liquids is honey, ketchup, toothpaste and many others.

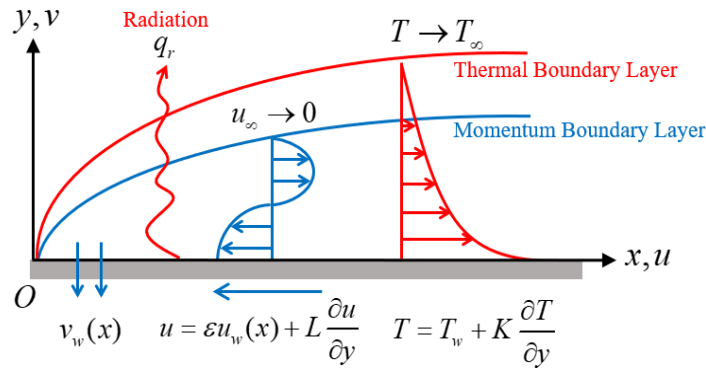
Disparate to the fluid model which have linearly relationship on strain and the stress tensors, the fluid under non-Newtonian models is perceived established on the behaviour of dilatant otherwise pseudo-plasticity. Over the last few decades, mathematicians as well as scientist introduced few mathematical models under non-Newtonian fluid type where certain model representing the special characteristics of fluid. The model that exists in literature are Casson, Jeffrey, Williamson, Eyring Powell Fluid, Reiner–Philippoff, micropolar, dusty fluid, viscoelastic, Brinkman, ferrofluid, nanofluid and several others [2-36].

Among the mentioned model, the RP fluid model is interesting to explore since the respective model able to be reduced to viscous fluid and being non-viscous in certain situation. Thus, due to the nature of properties, RP fluid offered many usages in the field of engineering, sciences and also to other technologies. The RP fluid model behave like Newtonian type when shear stress disappears or huge whereas at other condition, this fluid can work like the non-Newtonian characteristics. Many works have been reported on this fluid and the contributions are highlighted on the external effect considered to the flow and also the assumption of the flow of fluid moving too [37-40]. A fascinating study has been performed by Ahmad *et al.*, [41] where the flow of RP fluids flow prompted by the nonlinearly stretched surface and variable thickness effects. They recognized the sheer stress in term of skin friction changes by the different behaviour of fluid characteristics. Other reported study on RP fluid flow has been conducted by Reddy *et al.*, [42] where the investigation focussed on the flow toward the Darcy–Forchheimer porous medium. They exposed that the RP fluid parameter contributed major impact on temperature distribution. The reported outputs were in line with findings by Kumar *et al.*, [17]. Supplementary documents that discussed on RP fluid can be found in Ahmad [43], Reddy *et al.*, [44] and Sajid *et al.*, [45].

Motivated to the above-mentioned studies, this report is aimed to present the output of computational investigation on radiative non-Newtonian RP fluid flow past a stretching sheet in the presence of velocity slip and temperature jump effects. Appropriate similarity transformations are adopted to the governing PDEs to obtained similarity equations. To confirm on the validity of the proposed model and its results, the comparative analysis is done for the case where the present model is reduced to be identical with the reported model previously. The numerical computations are attained by applying bvp4c technique.

## 2. Methodology

The non-Newtonian RP fluid pass over a shrinking sheet was considered and its configuration as presented in Figure 1. By considering the velocity slip boundary condition, the surface velocity defined as  $u_w(x) = ax^{1/3}$  and hold the  $a > 0$ . The mass flux velocity on the other hand presenting the surface permeability with  $v_w(x)$ . The surface temperature is defined as  $T_w(x)$  since thermal slip boundary condition is considered with the ambient temperature  $T_\infty$  is constant. Furthermore, the radiative heat flux is taking as  $q_r = -(4\sigma^*/3k^*)(\partial T^4/\partial y)$ .



**Fig. 1.** Schematic configuration of flow

Therefore, the system of equation presenting this fluid system is written as

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$\frac{\partial u}{\partial y} = \frac{\tau}{\mu_\infty + \frac{\mu_0 - \mu_\infty}{1 + \left(\frac{\tau}{\tau_s}\right)^2}}, \quad (2)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{1}{\rho} \frac{\partial \tau}{\partial y}, \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \left( \frac{k}{\rho C_p} + \frac{16\sigma^* T_\infty^3}{3(\rho C_p)k^*} \right) \frac{\partial^2 T}{\partial y^2}, \quad (4)$$

subject to

$$u = \epsilon u_w(x) + L \frac{\partial u}{\partial y}, \quad v = v_w(x), \quad T = T_w + K \frac{\partial T}{\partial y} \quad \text{for } y=0; \quad (5)$$

$$u \rightarrow 0, \quad T \rightarrow T_\infty \quad \text{as } \eta \rightarrow \infty$$

The terms arise are summarized as

$\rho$  = fluid density

$\rho C_p$  = heat capacity

$k$  = thermal conductivity

$T$  = the temperature

$L$  = velocity slip factor

$K$  = thermal slip factor

$(u, v)$  = velocity components in the  $(x, y)$  direction

$\tau$  = shear stress

$\tau_s$  = reference shear stress

$\mu_\infty$  = dynamic viscosity

$\mu_0$  = zero-shear dynamic viscosity

Moreover, the value  $\varepsilon=0$ ,  $\varepsilon>0$  and  $\varepsilon<0$  signify static, stretching and shrinking sheet, respectively. The similarity transformation (6) is employed to (1) to (5) in order to obtain the similarity equations.

$$\psi = \sqrt{av}x^{2/3}f(\eta), \quad \tau = \rho\sqrt{a^3v}g(\eta), \quad \theta(\eta) = \frac{T-T_\infty}{T_w-T_\infty}, \quad \eta = \frac{y}{x^{1/3}}\sqrt{\frac{a}{v}} \tag{6}$$

The  $\psi$  is denoted as stream function and the definition is  $u = \partial\psi/\partial y$  and  $v = -\partial\psi/\partial x$ . Then:

$$u = ax^{1/3}f'(\eta), \quad v = -\sqrt{av}x^{-1/3}\left(\frac{2}{3}f(\eta) - \frac{1}{3}\eta f'(\eta)\right). \tag{7}$$

At  $\eta=0$ , the wall mass flux velocity turns out to be:

$$v_w(x) = -\frac{2}{3}\sqrt{av}x^{-1/3}S, \tag{8}$$

The expression  $f(0)=S$  mean the constant mass flux parameter at which  $S<0$  is the injection situation and  $S>0$  is suction situation. For  $S=0$ , the surface is considered as impermeable. The term  $\nu = \mu_\infty/\rho$  implies the kinematic viscosity of the respective fluid. Adopting Eq. (6) and Eq. (7) yield

$$g' + \frac{2}{3}ff'' - \frac{1}{3}f'^2 = 0, \tag{9}$$

$$g = f''\left(\frac{\lambda\gamma^2 + g^2}{\gamma^2 + g^2}\right), \tag{10}$$

$$\frac{1}{Pr}\left(1 + \frac{4}{3}R\right)\theta'' + \frac{2}{3}f\theta' = 0. \tag{11}$$

The boundary condition (5) was transformed to

$$f(0) = S, \quad f'(0) = \varepsilon + Af''(0), \quad \theta(0) = 1 + B\theta'(0); \\ f'(\eta) \rightarrow 0, \quad \theta(\eta) \rightarrow 0 \quad \text{as } \eta \rightarrow \infty \tag{12}$$

with the following parameter

$$\lambda = \frac{\mu_0}{\mu_\infty} \text{ (RP fluid parameter)}, \quad \gamma = \frac{\tau_s}{\rho\sqrt{a^3v}} \text{ (Bingham number)}, \\ Pr = \frac{\mu C_p}{k} \text{ (Prandtl number)}, \quad R = \frac{4\sigma^* T_\infty^3}{kk^*} \text{ (thermal radiation parameter)}, \\ A = L\sqrt{\frac{a}{v}} \text{ (velocity slip parameter)}, \quad B = K\sqrt{\frac{a}{v}} \text{ (thermal slip parameter)}. \tag{13}$$

It is worth to mention, the  $\lambda=1$  represent Newtonian fluid. In addition, for  $\lambda < 1$  and  $\lambda > 1$  signify shear thickening and the shear-thinning fluid cases respectively. The skin friction  $C_f$  and the local Nusselt number  $Nu_x$  are known as:

$$C_f = \frac{\tau_w}{\rho u_w^2}, \quad Nu_x = \frac{xq_w}{k(T_w - T_\infty)}, \quad (14)$$

where

$$\tau_w = \rho \sqrt{a^3 \nu} (g(\eta))_{y=0}, \quad q_w = -k \left( \frac{\partial T}{\partial y} \right)_{y=0} + (q_r)_{y=0}. \quad (15)$$

The term  $\tau_w$  symbolizes the quantity of  $\tau$  at  $y=0$  while the  $q_w$  is heat flux of the surface. Applying Eq. (14) and Eq. (15), obtained

$$Re_x^{1/2} C_f = g(0), \quad Re_x^{-1/2} Nu_x = -\left(1 + \frac{4}{3}R\right) \theta'(0), \quad (16)$$

which  $Re_x = u_w(x)x/\nu$  presenting the local Reynolds number.

### 3. Results and Discussions

In this section, the details discussion on the outputs from computational of Eq. (9) to Eq. (11) with respected to boundary conditions (12) using `bvp4c` solver embedded in MATLAB language. The procedures on the proposed method are explained in the studies by Shampine *et al.*, [46,47]. Further, the outputs are summarizing in the tabular and graphical forms.

To ensure the computation on the present model is acceptable, the validation procedures are carried out by direct comparison on the present results with the established output for the case where the equations and its boundary conditions are identical. It is worth to mention that, the current equations can be reduced to the equations by Cortell [48], Ferdows *et al.*, [49], Waini *et al.*, [50] and Sajid *et al.*, [45] in certain conditions. The comparative's results present a very strong agreement where it can be concluded the present results are satisfactory. The details fallouts can be found in Table 1, Table 2 and Table 3. It is highlighted from Table 1 and Table 2, for the fixed value  $\varepsilon = \lambda = \gamma = 1$  and  $Pr = 2$  the values of  $f''(0)$  significantly reduced and the quantity of  $-\theta'(0)$  improved in the increment of  $s$ . It is obvious, the situation happened due to the forces built by the activities of suction/injection. Meanwhile, the presence of strong quantity of radiation led to reduce the performance of  $-\theta'(0)$ . The output in Table 3 was strengthening the reliability of the present results as the value of  $g(0)$  concurs well with those reported by Sajid *et al.*, [45]. The results reported that, the strong value of Bingham number  $\gamma$  and RP fluid parameter  $\lambda$  enriched and decelerated the  $g(0)$  respectively.

**Table 1**  
 Quantity of  $f''(0)$  at  $\varepsilon = \lambda = \gamma = 1, Pr = 2$  for several  $S$

$S$	Cortell [48]	Ferdows <i>et al.</i> , [49]	Waini <i>et al.</i> , [50]	Present Result
-0.5	-0.518869	-0.518869	-0.518869	-0.518869426
0	-0.677647	-0.677648	-0.677648	-0.677647984
0.5	-0.873627	-0.873643	-0.873643	-0.873642862

**Table 2**  
 Quantity of  $-\theta'(0)$  when  $\varepsilon = \lambda = \gamma = 1, Pr = 2$  for several  $R$  and  $S$

$R$	$S$	Cortell [48]	Ferdows <i>et al.</i> , [49]	Waini <i>et al.</i> , [50]	Present Result
0	-0.5	0.3989462	0.398951	0.399100	0.399099808
	0	0.7643554	0.764374	0.764357	0.764356557
	0.5	1.2307661	1.230952	1.230792	1.230791767
1	-0.5	0.2873762	0.287483	0.287485	0.287483696
	0	0.4430879	0.443323	0.443323	0.443323143
	0.5	0.6322154	0.632199	0.632200	0.632199696

**Table 3**  
 Quantity of  $g(0)$  at  $S = 0$  and  $\varepsilon = 1$  for several value of  $\gamma$  and  $\lambda$

$\gamma$	$\lambda$	Sajid <i>et al.</i> , [45]	Present Result
0.1	0.1	-0.660273	-0.660275191
0.5	0.1	-0.380604	-0.380603982
1.0	0.1	-0.246415	-0.246414994
0.1	0.3	-0.664497	-0.664497828
0.1	0.5	-0.668484	-0.668486423
0.1	0.7	-0.672282	-0.672276683

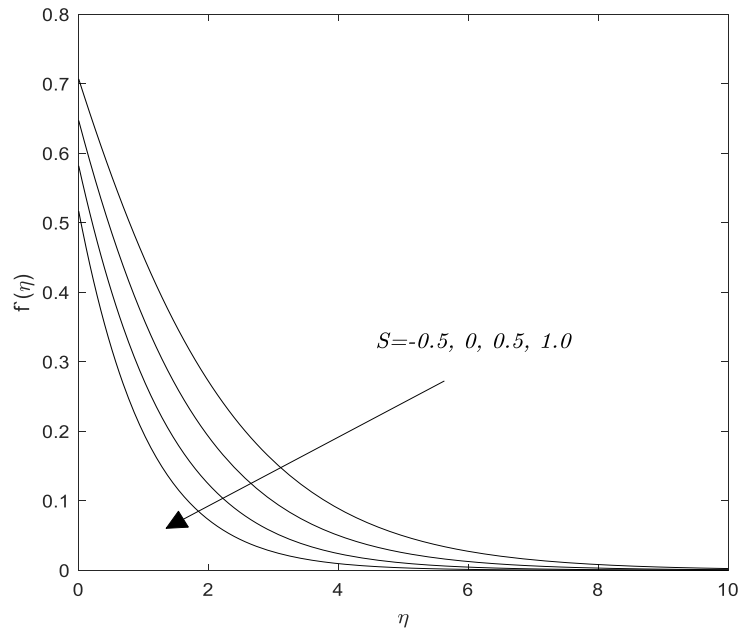
Table 4 delivers the values of  $Re_x^{1/2} C_f$  and  $Re_x^{-1/2} Nu_x$  for numerous physical parameters. The investigation is done at fixed values of  $\varepsilon = -1, S = 2.4, \lambda = 1.5, \gamma = 0.1, A = 3, B = 1, R = 3$  and  $Pr = 10$  against the inspected parameter. For increment values of  $\varepsilon$ , it is shown that the values of  $Re_x^{1/2} C_f$  are declined significantly, and the quantity of  $Re_x^{-1/2} Nu_x$  are intensified. It is logic since in the shrinking environment ( $\varepsilon < 0$ ), the interaction established to both fluid and the surface which controlled the skin friction. Meanwhile, the stretching case ( $\varepsilon > 0$ ) contributed in lessen the contact between fluid and surface. This indication in line with the output of  $Re_x^{-1/2} Nu_x$  in which the high vorticity take place in the shrinking environment which later affecting the degree of heat transfer. Also, it is observed the quantity of  $Re_x^{1/2} C_f$  and  $Re_x^{-1/2} Nu_x$  are amplified in intensifying the values of  $S$ . It happened due to the forces which led to augmenting the friction restored extra energy. In addition, the quantity of  $Re_x^{1/2} C_f$  and  $Re_x^{-1/2} Nu_x$  are deteriorating as  $\lambda$  and  $\gamma$  increasing. The growing on  $\lambda$  and  $\gamma$  under at  $\varepsilon = -1$  overwhelms the drag force enforcing the reduction on  $Re_x^{1/2} C_f$  and subsequently control the  $Re_x^{-1/2} Nu_x$ . The existing of velocity slip,  $A$ , in the shrinking case, condensing the  $Re_x^{1/2} C_f$  while boosting the  $Re_x^{-1/2} Nu_x$  due to the presence of difference phases on the flow field.

**Table 4**  
 Values of  $Re_x^{1/2}C_f$  and  $Re_x^{-1/2}Nu_x$  on studied parameters

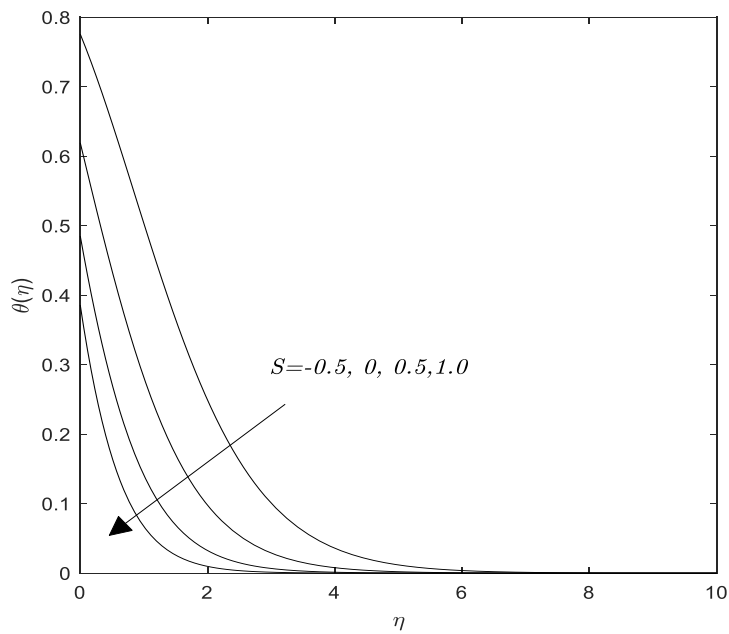
$\varepsilon$	$S$	$\lambda$	$\gamma$	$A$	$B$	$R$	$P$	$C_{fy}$	$Nu$
-1	2.4	1.5	0.1	1	1	3	10	0.591775617	3.773411221
-0.5								0.302085764	3.792674212
1								-0.631229651	3.836644918
-1	2.33							0.582038756	3.742197084
	2.36							0.586296266	3.755800954
	2.38							0.589063025	3.764679498
	2.4	0.5						0.594820740	3.774745113
		1						0.593346223	3.774057265
		2						0.590092566	3.772781463
		1.5	0.12					0.591303868	3.773199222
			0.15					0.590564716	3.772860858
			0.18					0.589809224	3.772510160
			0.1	0				1.102979762	3.696289899
				0.1				1.072489670	3.715272360
				0.5				0.813517063	3.754153222
				1	0			0.591775617	15.381728892
					0.1			0.591775617	11.763017861
					0.5			0.591775617	6.060158063
					1	0		0.591775617	0.940621426
						1		0.591775617	2.030762205
						2		0.591775617	2.965566520
						3	3	0.591775618	2.348890636
							5	0.591775617	3.003128795
							7	0.591775617	3.402479926

The changes in  $Pr$ ,  $B$ , and  $R$  do not affect the  $Re_x^{1/2}C_f$  because the mentioned parameters are treated independently. Conversely, the rate of  $Re_x^{-1/2}Nu_x$  were heightened under increasing in  $Pr$  and  $R$ . On the other hand, the deterioration behaviour is noticed at larger  $B$ . the fact of higher  $Pr$  diminish the thermal diffusivity which led to decay the thickness of the thermal boundary layer. Consequently, the temperature gradient and boosts the heat transfer rate. The affluence of thermal radiation over conduction is determine in higher  $R$ . Thus, more radiative heat energy is drove to the flow field. In this situation the temperature is upsurge and heat transfer is weakened.

The analysis conducted in this study are presented graphically in term of profiles and physical quantities subjected to effect considered. Figure 2 and Figure 3 presented the analysis in term of velocity and temperature profile respectively with suction and injection effect are considered. Both figures satisfied the boundary condition with each of them asymptotically approaching zero as the  $\eta$  value increase. From Figure 2, the velocity profile for the suction cases was found higher than injection cases with the velocity profile keep decreasing as  $S$  values increase. The same behaviour was also noticed on the temperature profile with the temperature profile values decreases as the  $S$  value increased.



**Fig. 2.**  $f'(\eta)$  vs  $\eta$  and various values of  $S$

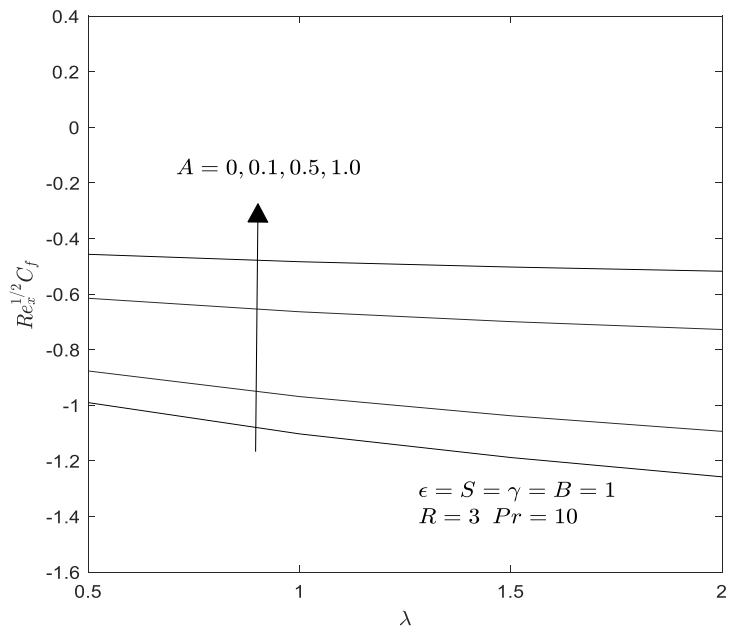


**Fig. 3.**  $\theta(\eta)$  vs  $\eta$  and various values of  $S$

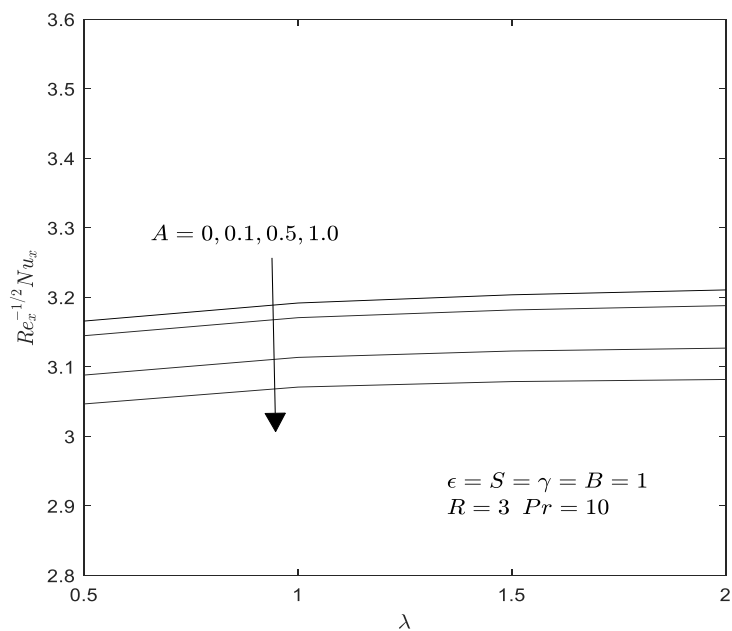
Figure 4 and Figure 5 show the impact of  $\lambda$  and  $A$  on the variations of  $Re_x^{1/2}C_f$  and  $Re_x^{-1/2}Nu_x$  when  $\varepsilon=1$ ,  $S=1$ ,  $\gamma=1$ ,  $B=1$ ,  $R=3$  and  $Pr=10$ . The increases of  $\lambda$  shows a decreasing behaviour for  $Re_x^{1/2}C_f$  but increase in term of  $Re_x^{-1/2}Nu_x$ . On the other hand, a contradict behaviour was noticed on  $Re_x^{1/2}C_f$  and  $Re_x^{-1/2}Nu_x$  for parameter  $A$  with the increases of parameter  $A$  increase the  $Re_x^{1/2}C_f$  but decrease in term of  $Re_x^{-1/2}Nu_x$ . The analysis on  $Re_x^{1/2}Nu_x$  was also conducted in Figure 6 subjected to parameter  $B$  with constant value of  $\varepsilon=1$ ,  $S=1$ ,  $\gamma=1$ ,  $A=1$ ,  $R=3$  and  $Pr=10$  were used. From Figure 6, the increases of parameter  $B$  increase the  $Re_x^{1/2}Nu_x$  values significantly. The analysis on the parameters  $Pr$  and  $R$  are presented in Figure 7 on  $Re_x^{1/2}Nu_x$  quantities with  $\varepsilon=1$ ,  $\lambda=1$ ,  $\gamma=1$ ,



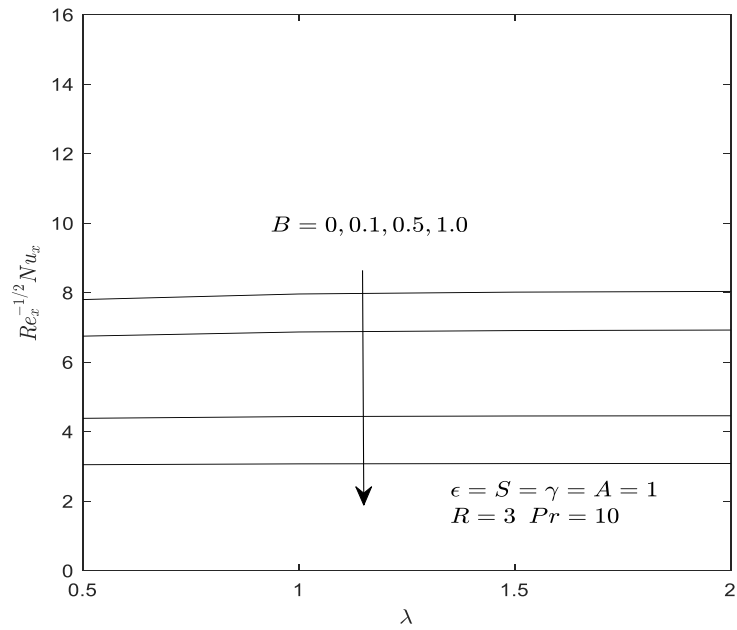
$A = 1$ , and  $B = 1$ . Based on the graphical analysis presented in Figure 7, both parameters  $Pr$  and  $R$  increase the thermal characteristic of  $Re_x^{1/2} Nu_x$ . Figure 8 and Figure 9 show the variation of  $Re_x^{1/2} C_f$  and  $Re_x^{1/2} Nu_x$  with the influence of  $S$  and  $\lambda$  at constant values of  $\epsilon = 1, \gamma = 1, A = 1, B = 1, R = 3$  and  $Pr = 10$ . From Figure 8, the increases of both parameters  $S$  and  $\lambda$  decrease the  $Re_x^{1/2} C_f$  while contradict behaviour noticed on  $Re_x^{1/2} Nu_x$  for the same parameter values induced as shown in Figure 9.



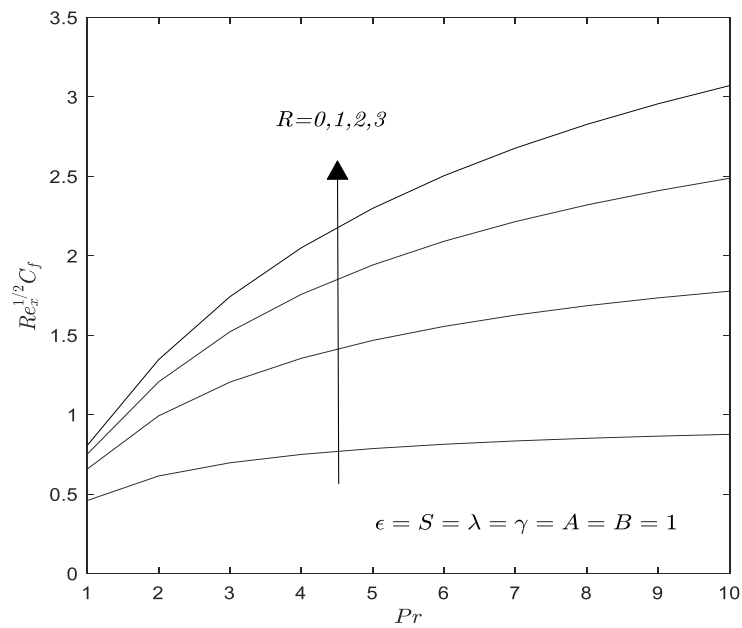
**Fig. 4.** Skin friction variation  $Re_x^{1/2} C_f$  vs  $\lambda$  for numerous values of  $A$



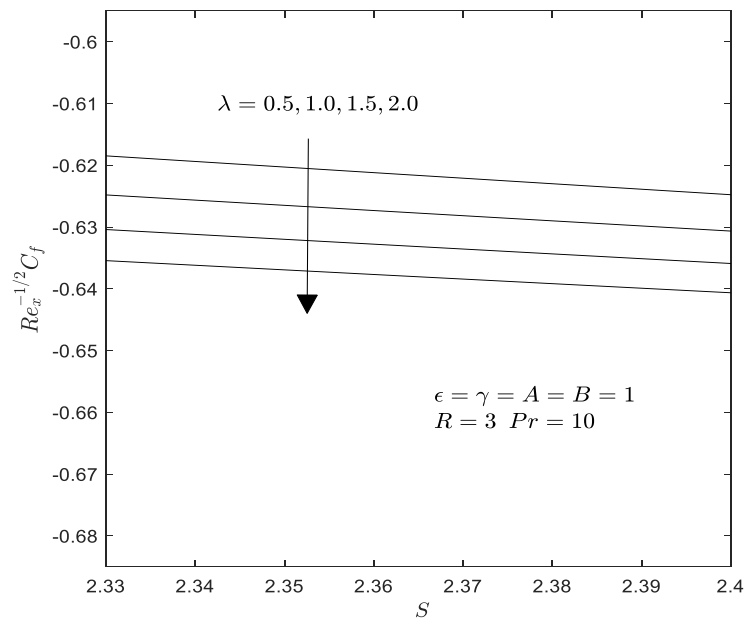
**Fig. 5.** Local Nusselt number  $Re_x^{-1/2} Nu_x$  vs  $\lambda$  for numerous values of  $A$



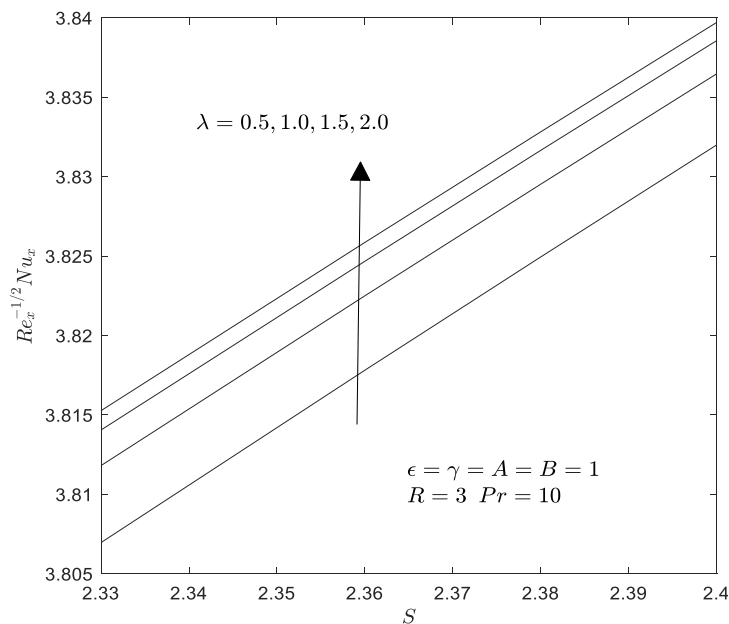
**Fig. 6.** Local Nusselt number  $Re_x^{-1/2} Nu_x$  vs  $\lambda$  for numerous values of  $B$



**Fig. 7.** Local Nusselt number  $Re_x^{-1/2} C_f$  vs  $Pr$  for numerous values of  $R$



**Fig. 8.** Skin friction variation  $Re_x^{-1/2} C_f$  vs  $S$  for numerous values of  $\lambda$



**Fig. 9.** Local Nusselt number  $Re_x^{-1/2} Nu_x$  vs  $S$  for numerous values of  $\lambda$

#### 4. Conclusions

The RP fluid flow through a sheet that have ability to shrink is mathematically analysed under influence of thermal radiation together with condition of slip in velocity and thermal. The suction parameter has been shown to influence the thickness of the boundary layer in velocity and temperature distribution. Both velocity and thermal slip parameter decrease in term of local Nusselt number. On the other hand, the increases of radiation parameter, Prandtl number, RP fluid parameter and injection parameter increase the local Nusselt number. The increases of velocity slip

parameter increase the skin friction coefficient while RP fluid parameter and injection parameter decrease the skin friction coefficient.

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